

Table with 6 columns: English Unit, SI Unit, Symbol, and Greek Unit. Includes units for Mass (kg, g, mg, μg), Length (m, cm, mm), Area (m², cm², mm²), Volume (m³, cm³, mm³), Time (s, min, h, day), Temperature (K, °C, °F), and Energy (J, cal, Btu, kWh).

Table with 6 columns: English Unit, SI Unit, Symbol, and Greek Unit. Includes units for Force (N, dyne, lbf, kip), Pressure (Pa, bar, psi, atm), Power (W, hp, Btu/h, kcal/h), Heat Flow (W/m², Btu/ft²), and Heat Transfer Coefficient (W/m²K).

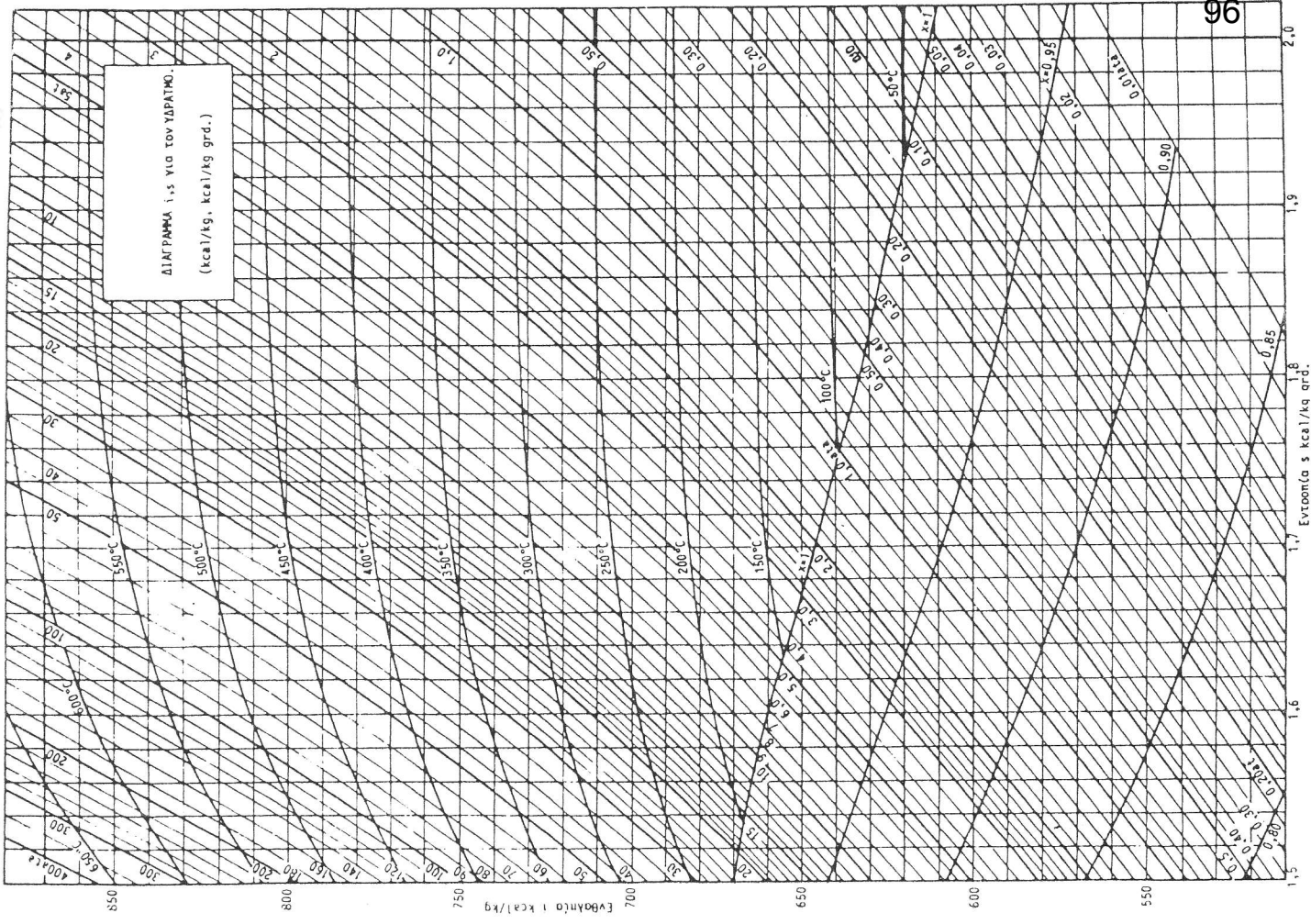
Table with 6 columns: English Unit, SI Unit, Symbol, and Greek Unit. Includes units for Viscosity (Pa·s, poise, centipoise), Thermal Conductivity (W/mK, kcal/mK), Thermal Expansion (1/K, 1/°C, 1/°F), and Thermal Diffusivity (m²/s, ft²/h).

1.5. ΣχΆσεις μεταφύ των παραγκων μονΆδων και των βασικων
1 mm = 60 s
1 h = 60 min = 3600 s
1 d = 24 h = 1440 min = 86400 s
1 hz = 1/s
1 N = 1 kg m/s²
1 Pa = 1 N/m² = 1 kg/m s² = 1 kg/m s²
1 bar = 10⁵ N/m² = 10⁵ kg/m s² = 10⁵ kg/m s²
1 Pa = 1 N/m² = 1 kg/m s² = 1 kg/m s²
1 J = 1 W s = 1 Nm = 1 kg m²/s² = 1 kg m²/s²
1 W = 1 J/s = 1 Nm/s = 1 kg m²/s³ = 1 kg m²/s³
1 Pa = 1 W/A = 1 J/(A s) = 1 Nm/(A s) = 1 kg m/s²A = 1 kg m/s²A
1 Ω = 1 V/A = 1 W/A² = 1 J/(A² s) = 1 Nm/(A² s) = 1 kg m/(A² s) = 1 kg m/A² s
1 S = 1/Ω = 1 A/V = 1 A/(Nm/A s) = 1 kg m/A² s = 1 kg m/A² s
1 C = 1 A s

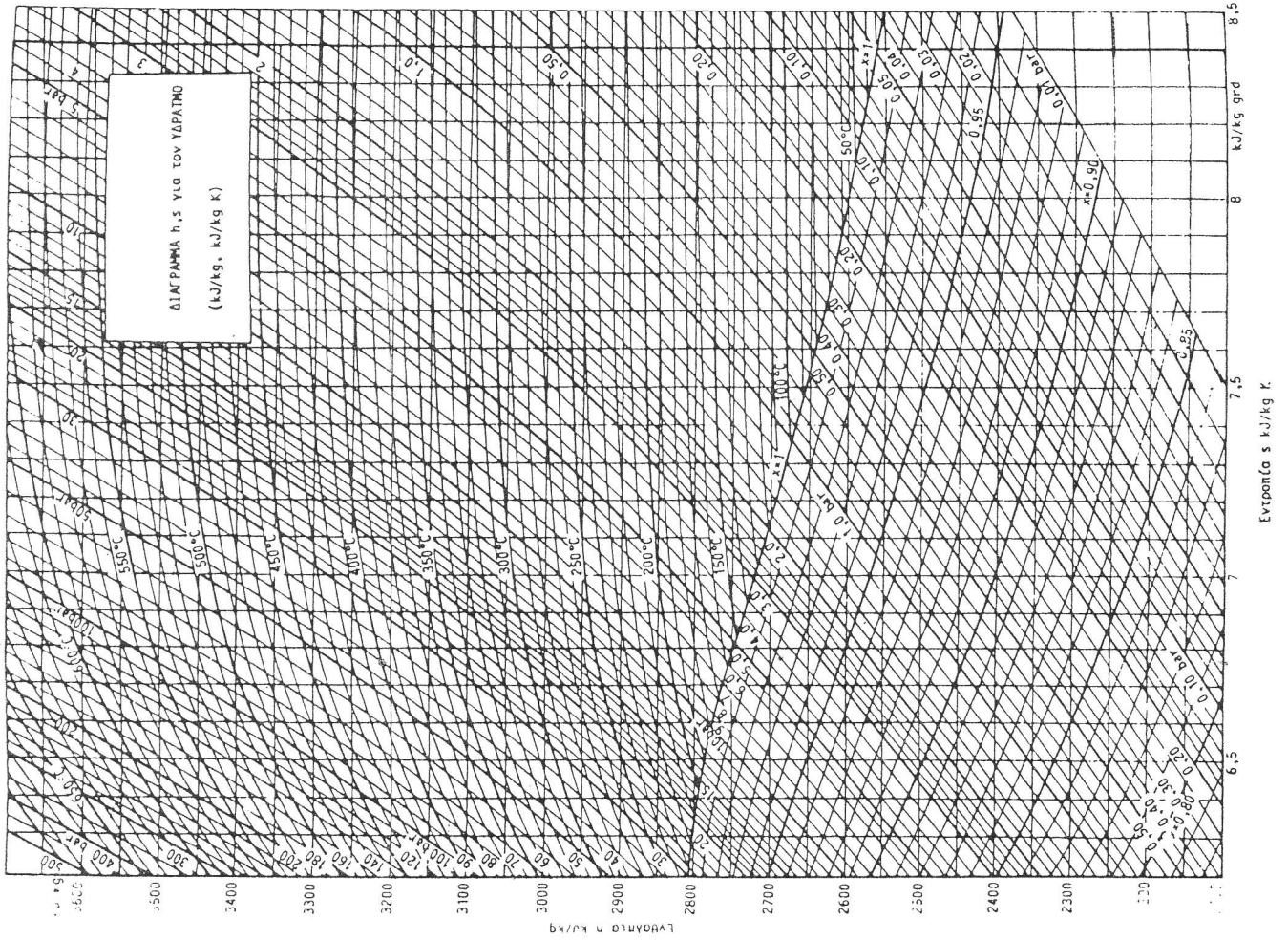
Ββ 2	Μονάδες και σχέσεις μονάδων	VDI-Wärmeatlas 2. Auflage 1974
2. ΜΕΤΑΤΡΟΠΗ ΔΙΑΦΟΡΩΝ ΜΟΝΑΔΩΝ ΕΙΣ ΤΟ ΣΥΣΤΗΜΑ SI	Μονάδες και σχέσεις μονάδων	VDI-Wärmeatlas 2. Auflage 1974
"Εργον, Ενέργεια, Θερμότητα 1 Nm 1 W s 1 dyn cm 1 erg 1 Dyn m 1 kpm 1 kcal 1 kWh 1 PSh 1 Btu 1 Chu 1 ft pdl 1 ft lbf 1 hp hr (britisch) 1 therm	"Ενέργεια, Έργον "Ενθαλπία, Έργον Είδωλη "Ενθαλπία 1 kcal/kg 1 Btu/lb 1 Chu/lb "Εντροπία - είδωλη Θερμότητα "Επιπόνοια 1 in ² 1 ft ² 1 yd ² 1 acre 1 mile ² Παχύτητα 1 ft/hr 1 ft/min 1 ft/s 1 mile/hr "Αρτίον Θερμότητας - επίσημοις - πυκνότητες οφεις Θερμότητας Θερμική μεγέθη βασιζόμενα εις τον όγκον 1 kcal/m ³ 1 Btu/ft ³ 1 Chu/ft ³ 1 therm/ft ³ Δυναμεις 1 kp 1 dyn 1 Dyn 1 pdl 1 lbf 1 tonf "Ήλικος 1 A 1 μ (micron) 1 in 1 ft = 12 in 1 yd = 3 ft = 36 in 1 thou 1 mile (statute) 1 mile (nautical) 1 rod = 1 perch = 5,5 yd 1 chain 1 furlong	9,8065 J = 1 Nm = 1,0000 J = 1 W s = 1,0000 · 10 ⁻⁷ J = 1 dyn cm = 1,0000 · 10 ⁻⁷ J = 1 erg = 1,0000 · 10 ⁻² J = 1 Dyn m = 9,8067 J = 1 kpm = 4,1868 · 10 ³ J = 1 kcal = 3,6000 · 10 ⁶ J = 1 kWh = 2,6478 · 10 ⁶ J = 1 PSh = 1,0551 · 10 ³ J = 1 Btu = 4,3991 · 10 ³ J = 1 Chu = 4,2139 · 10 ⁻² J = 1 ft pdl = 1,3558 J = 1 ft lbf = 2,6845 · 10 ⁶ J = 1 hp hr (britisch) = 1,0551 · 10 ⁸ J = 1 therm
"Εκτατικός συντελεστής (όγκομετρικός) 1 g/cm ³ °C 1 lb/ft ³ °C 1 lb/ft ³ °F	Εξοχή, Θερμότητα 1 mikp/s 1 kcal/h 1 erg/s 1 PS 1 m ³ atm/h 1 ft lbf/min 1 ft lbf/s 1 ft pdl/s 1 Btu/hr 1 Chu/hr 1 hp (britisch) 1 ton refrigeration 1 therm/hr	9,8065 W = 1 mikp/s = 1,1630 W = 1 kcal/h = 1,0000 · 10 ⁻⁷ W = 1 erg/s = 7,3548 · 10 ² W = 1 PS = 2,8150 · 10 W = 1 m ³ atm/h = 2,2597 · 10 ⁻² W = 1 ft lbf/min = 1,3558 W = 1 ft lbf/s = 4,2139 · 10 ⁻² W = 1 ft pdl/s = 2,9308 · 10 ⁻¹ W = 1 Btu/hr = 5,2754 · 10 ⁻¹ W = 1 Chu/hr = 7,4570 · 10 ² W = 1 hp (britisch) = 3,5169 · 10 ³ W = 1 ton refrigeration = 2,9308 · 10 ⁴ W = 1 therm/hr
"Επιτόχιος 1 ft/s ² 1 grain 1 lb 1 ton (short) = 20 cwt brit. 1 ton (long) = 20 cwt UK Ροή μάζης 1 lb/hr 1 ton/day (short) 1 ton/day (long) 1 ton/hr (short) 1 ton/hr (long) Πυκνότητες ροής μάζης 1 lb/hr ft ² 1 kg/hr ft ² 1 lb/s ft ² Τάσις μηχανική + πίεσις Θερμικρασία (είδε πίνακα κερ. Bb) θ °C θ °F (Fahrenheit) 1 °R (Rankine) Σχέσεις θερμοκρασιών 1 °C 1 °F 1 °R	Μονάδες και σχέσεις μονάδων	9,8065 Pas = 1 kps/m ² = 3,532 · 10 ⁻⁴ Pas = 1 kplb/m ² = 1,0000 · 10 ⁻¹ Pas = 1 Poise = 1 g/cm s = 4,1338 · 10 ⁻⁴ Pas = 1 lb/ft hr = 9,1134 · 10 ⁻⁴ Pas = 1 kg/ft hr = 1,4882 Pas = 1 lb/fts
1 ft/s ² 1 grain 1 lb 1 ton (short) = 20 cwt brit. 1 ton (long) = 20 cwt UK Ροή μάζης 1 lb/hr 1 ton/day (short) 1 ton/day (long) 1 ton/hr (short) 1 ton/hr (long) Πυκνότητες ροής μάζης 1 lb/hr ft ² 1 kg/hr ft ² 1 lb/s ft ² Τάσις μηχανική + πίεσις Θερμικρασία (είδε πίνακα κερ. Bb) θ °C θ °F (Fahrenheit) 1 °R (Rankine) Σχέσεις θερμοκρασιών 1 °C 1 °F 1 °R	Μονάδες και σχέσεις μονάδων	9,8065 Pas = 1 kps/m ² = 3,532 · 10 ⁻⁴ Pas = 1 kplb/m ² = 1,0000 · 10 ⁻¹ Pas = 1 Poise = 1 g/cm s = 4,1338 · 10 ⁻⁴ Pas = 1 lb/ft hr = 9,1134 · 10 ⁻⁴ Pas = 1 kg/ft hr = 1,4882 Pas = 1 lb/fts
1 ft/s ² 1 grain 1 lb 1 ton (short) = 20 cwt brit. 1 ton (long) = 20 cwt UK Ροή μάζης 1 lb/hr 1 ton/day (short) 1 ton/day (long) 1 ton/hr (short) 1 ton/hr (long) Πυκνότητες ροής μάζης 1 lb/hr ft ² 1 kg/hr ft ² 1 lb/s ft ² Τάσις μηχανική + πίεσις Θερμικρασία (είδε πίνακα κερ. Bb) θ °C θ °F (Fahrenheit) 1 °R (Rankine) Σχέσεις θερμοκρασιών 1 °C 1 °F 1 °R	Μονάδες και σχέσεις μονάδων	9,8065 Pas = 1 kps/m ² = 3,532 · 10 ⁻⁴ Pas = 1 kplb/m ² = 1,0000 · 10 ⁻¹ Pas = 1 Poise = 1 g/cm s = 4,1338 · 10 ⁻⁴ Pas = 1 lb/ft hr = 9,1134 · 10 ⁻⁴ Pas = 1 kg/ft hr = 1,4882 Pas = 1 lb/fts

Ββ 3	Μονάδες και σχέσεις μονάδων	VDI-Wärmeatlas 2. Auflage 1974
1 ft/s ² 1 grain 1 lb 1 ton (short) = 20 cwt brit. 1 ton (long) = 20 cwt UK Ροή μάζης 1 lb/hr 1 ton/day (short) 1 ton/day (long) 1 ton/hr (short) 1 ton/hr (long) Πυκνότητες ροής μάζης 1 lb/hr ft ² 1 kg/hr ft ² 1 lb/s ft ² Τάσις μηχανική + πίεσις Θερμικρασία (είδε πίνακα κερ. Bb) θ °C θ °F (Fahrenheit) 1 °R (Rankine) Σχέσεις θερμοκρασιών 1 °C 1 °F 1 °R	Μονάδες και σχέσεις μονάδων	9,8065 Pas = 1 kps/m ² = 3,532 · 10 ⁻⁴ Pas = 1 kplb/m ² = 1,0000 · 10 ⁻¹ Pas = 1 Poise = 1 g/cm s = 4,1338 · 10 ⁻⁴ Pas = 1 lb/ft hr = 9,1134 · 10 ⁻⁴ Pas = 1 kg/ft hr = 1,4882 Pas = 1 lb/fts
1 ft/s ² 1 grain 1 lb 1 ton (short) = 20 cwt brit. 1 ton (long) = 20 cwt UK Ροή μάζης 1 lb/hr 1 ton/day (short) 1 ton/day (long) 1 ton/hr (short) 1 ton/hr (long) Πυκνότητες ροής μάζης 1 lb/hr ft ² 1 kg/hr ft ² 1 lb/s ft ² Τάσις μηχανική + πίεσις Θερμικρασία (είδε πίνακα κερ. Bb) θ °C θ °F (Fahrenheit) 1 °R (Rankine) Σχέσεις θερμοκρασιών 1 °C 1 °F 1 °R	Μονάδες και σχέσεις μονάδων	9,8065 Pas = 1 kps/m ² = 3,532 · 10 ⁻⁴ Pas = 1 kplb/m ² = 1,0000 · 10 ⁻¹ Pas = 1 Poise = 1 g/cm s = 4,1338 · 10 ⁻⁴ Pas = 1 lb/ft hr = 9,1134 · 10 ⁻⁴ Pas = 1 kg/ft hr = 1,4882 Pas = 1 lb/fts

Διάγραμμα i, s γυν υδρατμό (kcal/kg, kcal/kggrd)

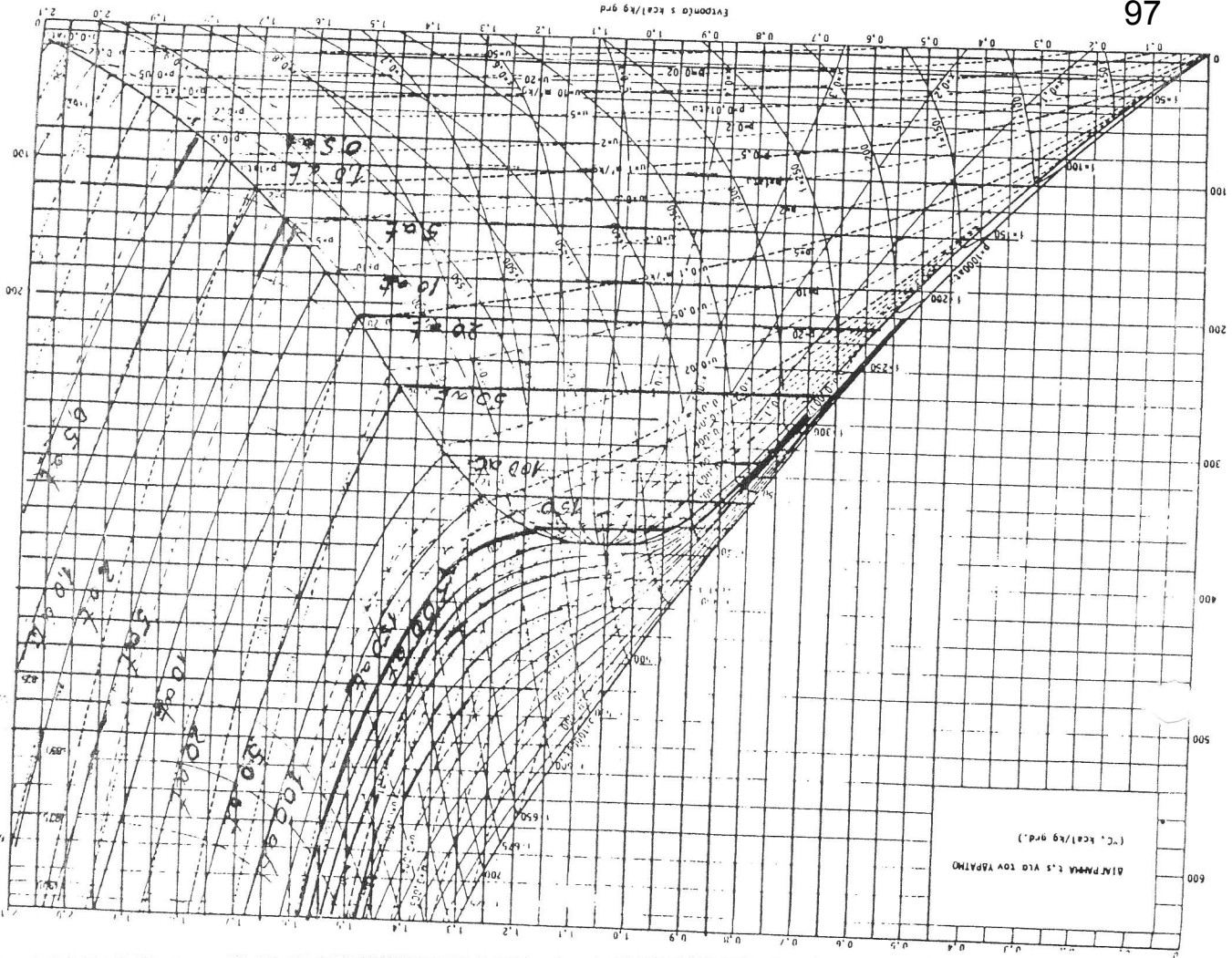


Διάγραμμα h, s για τον υδρατμό (kJ/kg, kJ/kgK)



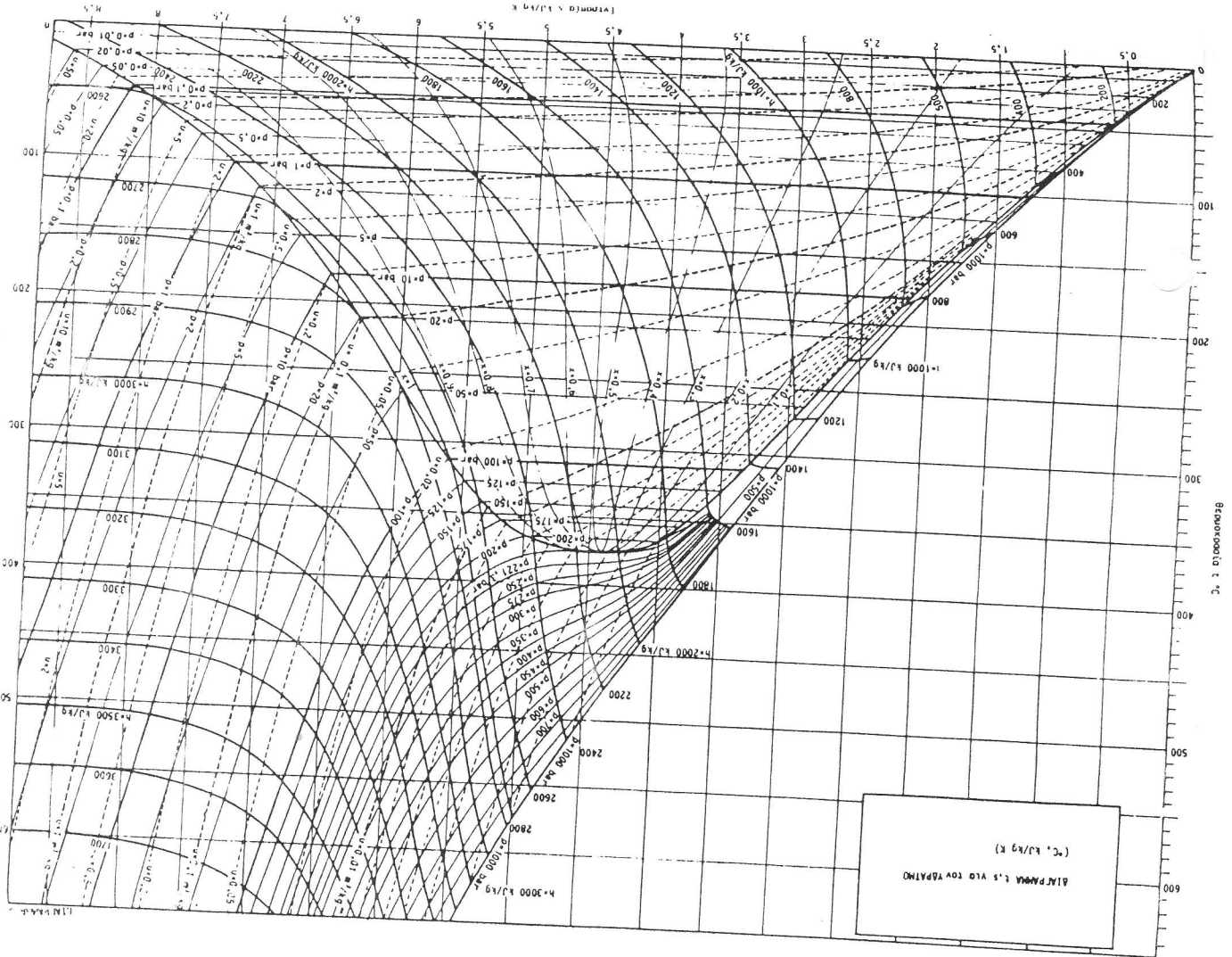
Θεωρία και τεχνική του υδρατμού

Διάγραμμα t, s για τον υδρατμό (°C, kcal/kggrd)



Παράρτημα

Διάγραμμα t, s για τον υδρατμό (°C, kcal/kgK)



Θεωρία και τεχνική του υδρατμού

ΠΙΝΑΚΕΣ ΑΤΜΩΝ

- Πίνακας I Καταστατικά μεγέθη νερού και ατμού κατά τον κορεσμό (πίνακας με βάση την θερμοκρασία) σε μονάδες του Τ.Σ.Μ.
- Πίνακας II Ομοίως αλλά σε μονάδες του Δ.Σ.Μ.
- Πίνακας III Καταστατικά μεγέθη νερού και ατμού κατά τον κορεσμό (πίνακας με βάση την πίεση) σε μονάδες του Τ.Σ.Μ.
- Πίνακας IV Ομοίως αλλά σε μονάδες του Δ.Σ.Μ.
- Πίνακας V Καταστατικά μεγέθη νερού και υπερθέρμου ατμού σε μονάδες του Τ.Σ.Μ. Η οριζόντια γραμμή χωρίζει το νερό από τον ατμό.
- Πίνακας VI Ομοίως αλλά σε μονάδες του Δ.Σ.Μ.

Εδώ

- t = θερμοκρασία σε °C
- p = πίεση σε ata (bar απόλυτα)
- v' = ειδικός όγκος νερού (x=0) σε dm³/kg
- v'' = ειδικός όγκος ατμού (x=1) σε m³/kg
- p'' = πυκνότητα του ατμού (x=1) σε kg/m³
- s' = ειδική εντροπία του νερού (x=0) σε kcal/kggrd (kJ/kgK)
- s'' = ειδική εντροπία του ατμού (x=1) σε kcal/kggrd (kJ/kgK)
- i'(h')
- i''(h'')
- r = ειδική ενθαλπία του νερού (x=0) σε kcal/kg (kJ/kg)
- u' = ειδική εσωτερική ενέργεια του νερού (x=0) σε kcal/kg (kJ/kg)
- u'' = ειδική εσωτερική ενέργεια του ατμού (x=1) σε kcal/kg (kJ/kg)
- υ = ειδικός όγκος νερού και υπερθέρμου ατμού σε m³/kg
- i(h) = ειδική ενθαλπία νερού και υπερθέρμου ατμού σε kcal/kg (kJ/kg)
- s = ειδική εντροπία νερού και υπερθέρμου ατμού σε kcal/kggrd (kJ/kgK)

Πίνακας I

Καταστατικά μεγέθη νερού και ατμού κατά τον κορεσμό (με βάση την θερμοκρασία) σε μονάδες του Τ.Σ.Μ.

°C t	at p	dm ³ /kg v'	m ³ /kg v''	kg/m ³ ρ''	kcal/kg °K		s' - s''
					s	s''	
0	0,006228	1,0002	206,3	0,004847	0	2,1865	2,1865
5	0,008894	1,0000	147,1	0,006798	0,0182	2,1552	2,1370
10	0,012517	1,0002	106,4	0,009399	0,0361	2,1254	2,0893
15	0,017381	1,0008	77,96	0,01283	0,0536	2,0969	2,0433
20	0,02383	1,0017	57,84	0,01729	0,0708	2,0697	1,9989
25	0,03229	1,0029	43,40	0,02304	0,0876	2,0436	1,9560
30	0,04325	1,0043	32,94	0,03036	0,1042	2,0186	1,9144
35	0,05732	1,0059	25,25	0,03960	0,1205	1,9947	1,8742
40	0,07519	1,0078	19,56	0,05113	0,1366	1,9718	1,8352
45	0,09770	1,0099	15,28	0,06544	0,1524	1,9497	1,7973
50	0,12577	1,0121	12,05	0,08298	0,1679	1,9286	1,7607
55	0,16050	1,0146	9,583	0,1044	0,1832	1,9082	1,7250
60	0,2031	1,0172	7,682	0,1302	0,1983	1,8887	1,6904
65	0,2550	1,0200	6,205	0,1612	0,2132	1,8698	1,6566
70	0,3178	1,0229	5,047	0,1981	0,2279	1,8517	1,6238
75	0,3931	1,0260	4,135	0,2418	0,2424	1,8342	1,5918
80	0,4829	1,0293	3,410	0,2933	0,2567	1,8173	1,5605
85	0,5894	1,0327	2,829	0,3535	0,2708	1,8011	1,5303
90	0,7149	1,0363	2,361	0,4235	0,2847	1,7854	1,5007
95	0,8619	1,0400	1,982	0,5045	0,2984	1,7702	1,4718
100	1,03323	1,0438	1,673	0,5977	0,3120	1,7555	1,4435
105	1,2318	1,0479	1,419	0,7047	0,3254	1,7413	1,4159
110	1,4609	1,0520	1,210	0,8264	0,3387	1,7276	1,3889
115	1,7239	1,0563	1,036	0,9652	0,3518	1,7143	1,3625
120	2,0245	1,0608	0,8913	1,122	0,3647	1,7014	1,3367
125	2,3666	1,0654	0,7700	1,299	0,3775	1,6890	1,3115
130	2,7544	1,0702	0,6679	1,497	0,3902	1,6769	1,2867
135	3,192	1,0751	0,5817	1,719	0,4028	1,6652	1,2624
140	3,685	1,0802	0,5083	1,967	0,4152	1,6538	1,2386
145	4,237	1,0855	0,4459	2,243	0,4275	1,6427	1,2152
150	4,854	1,0910	0,3924	2,549	0,4397	1,6319	1,1922
155	5,540	1,0966	0,3464	2,887	0,4518	1,6214	1,1696
160	6,302	1,1024	0,3068	3,260	0,4637	1,6112	1,1475
165	7,146	1,1085	0,2724	3,671	0,4756	1,6012	1,1256
170	8,076	1,1147	0,2426	4,122	0,4874	1,5914	1,1040
175	9,101	1,1211	0,2166	4,617	0,4991	1,5818	1,0827
180	10,225	1,1278	0,1939	5,158	0,5107	1,5724	1,0617
185	11,456	1,1347	0,1739	5,750	0,5222	1,5632	1,0410
190	12,800	1,1418	0,1564	6,394	0,5337	1,5541	1,0204
195	14,265	1,1491	0,1409	7,097	0,5450	1,5451	1,0001

Συνέχεια πίνακα I

°C <i>t</i>	at <i>p</i>	dm ³ /kg <i>v'</i>	m ³ /kg <i>v''</i>	kg/m ³ <i>ρ''</i>	kcal/kg * K		<i>s'' - s'</i> = <i>r/T</i>
					<i>s'</i>	<i>s''</i>	
200	15,857	1,1568	0,1273	7,856	0,5563	1,5363	0,9800
205	17,585	1,1647	0,1151	8,088	0,5676	1,5276	0,9600
210	19,456	1,1729	0,1043	9,588	0,5788	1,5189	0,9401
215	21,478	1,1814	0,09471	10,56	0,5899	1,5103	0,9204
220	23,659	1,1903	0,08611	11,61	0,6010	1,5017	0,9007
225	26,007	1,1994	0,07841	12,75	0,6120	1,4932	0,8812
230	28,531	1,2090	0,07149	13,99	0,6230	1,4847	0,8617
235	31,239	1,2190	0,06527	15,32	0,6340	1,4762	0,8422
240	34,140	1,2293	0,05967	16,76	0,6450	1,4677	0,8227
245	37,244	1,2402	0,05460	18,31	0,6559	1,4592	0,8033
250	40,56	1,2515	0,05002	19,99	0,6668	1,4507	0,7839
255	44,10	1,2633	0,04586	21,81	0,6777	1,4421	0,7644
260	47,87	1,2757	0,04208	23,76	0,6886	1,4335	0,7449
265	51,88	1,2888	0,03865	25,87	0,6996	1,4248	0,7252
270	56,14	1,3025	0,03552	28,15	0,7105	1,4161	0,7056
275	60,66	1,3169	0,03266	30,62	0,7215	1,4073	0,6858
280	65,46	1,3322	0,03005	33,28	0,7324	1,3984	0,6660
285	70,54	1,3483	0,02766	36,16	0,7435	1,3894	0,6469
290	75,92	1,3655	0,02540	39,27	0,7546	1,3804	0,6258
295	81,60	1,3837	0,02345	42,64	0,7658	1,3712	0,6054
300	87,61	1,4033	0,02165	46,19	0,7770	1,3620	0,5850
305	93,95	1,424	0,01989	50,28	0,7884	1,3526	0,5642
310	100,64	1,447	0,01832	54,57	0,7999	1,3431	0,5432
315	107,69	1,471	0,01687	59,29	0,8115	1,3337	0,5222
320	115,12	1,498	0,01549	64,55	0,8234	1,3232	0,4998
325	122,95	1,527	0,01420	70,43	0,8354	1,3118	0,4764
330	131,18	1,560	0,01298	77,02	0,8478	1,2999	0,4521
335	139,85	1,597	0,01184	84,43	0,8605	1,2870	0,4265
340	148,96	1,638	0,01077	92,81	0,8736	1,2735	0,3999
345	158,54	1,687	0,009765	102,4	0,8874	1,2595	0,3721
350	168,63	1,746	0,008803	113,6	0,9021	1,2441	0,3420
355	179,24	1,817	0,007878	126,9	0,9179	1,2270	0,3091
360	190,42	1,908	0,006967	143,5	0,9353	1,2072	0,2719
365	202,21	2,03	0,00604	165,5	0,9557	1,1833	0,2276
370	214,68	2,23	0,00499	200	0,9824	1,1481	0,1657
371	217,26	2,30	0,00474	211	0,9897	1,1387	0,1490
372	219,88	2,37	0,00447	224	0,9984	1,1276	0,1292
373	222,53	2,49	0,00415	241	1,010	1,1136	0,104
374	225,22	2,79	0,00362	276	1,033	1,086	0,053
374,1F	225,65	3,18	0,00318	315	1,058	1,058	0

Συνέχεια πίνακα I

°C <i>t</i>	kcal/kg		kcal/kg <i>r</i>	kcal/kg		<i>u'' - u'</i> = $\frac{p'' - p'}{\rho}$	$\frac{p'' - p'}{(\rho'' - \rho')}$ = $\frac{v'' - v'}{\rho}$
	<i>u'</i>	<i>u''</i>		<i>u'</i>	<i>u''</i>		
0	0	597,2	597,2	597,2	597,2	30,1	
5	5,03	594,4	594,4	599,4	568,9	30,6	
10	10,04	591,6	591,6	590,4	570,5	31,2	
15	15,04	588,8	588,8	572,2	557,1	31,7	
20	20,03	586,0	586,0	573,7	553,7	32,3	
25	25,02	583,2	583,2	575,4	550,4	32,8	
30	30,00	580,4	580,4	577,0	547,0	33,4	
35	34,98	577,5	577,5	578,6	543,6	33,9	
40	39,97	574,7	574,7	580,2	540,3	34,4	
45	44,96	571,8	571,8	581,8	536,8	35,0	
50	49,94	569,0	569,0	583,4	533,5	35,5	
55	54,94	566,1	566,1	585,0	530,1	36,0	
60	59,93	563,2	563,2	586,6	526,7	36,5	
65	64,93	560,2	560,2	588,0	523,1	37,1	
70	69,93	557,3	557,3	589,6	519,7	37,6	
75	74,94	554,3	554,3	591,1	516,2	38,1	
80	79,95	551,3	551,3	592,6	512,7	38,6	
85	84,96	548,1	548,1	594,0	509,0	39,1	
90	89,98	545,0	545,0	595,5	505,5	39,5	
95	95,01	541,9	541,9	596,9	501,9	40,0	
100	100,05	538,8	538,8	598,3	498,3	40,5	
105	105,09	535,5	535,5	599,7	494,6	40,9	
110	110,14	532,3	532,3	601,0	490,9	41,4	
115	115,20	529,0	529,0	602,4	487,2	41,8	
120	120,3	525,7	525,7	603,7	483,5	42,2	
125	125,3	522,3	522,3	604,9	479,7	42,6	
130	130,4	518,9	518,9	606,2	475,9	43,0	
135	135,5	515,4	515,4	607,4	472,0	43,4	
140	140,7	511,8	511,8	608,5	468,0	43,8	
145	145,8	508,2	508,2	609,8	464,1	44,1	
150	150,9	504,6	504,6	610,9	460,1	44,5	
155	156,1	500,9	500,9	612,1	456,1	44,8	
160	161,3	497,1	497,1	613,1	452,0	45,1	
165	166,5	493,2	493,2	614,1	447,8	45,4	
170	171,7	489,3	489,3	615,1	443,6	45,7	
175	176,9	485,4	485,4	616,1	439,4	46,0	
180	182,2	481,2	481,2	616,9	435,0	46,2	
185	187,4	477,1	477,1	617,8	430,6	46,4	
190	192,8	472,7	472,7	618,6	426,3	46,5	
195	198,1	468,3	468,3	619,3	421,0	46,7	

Παράρτημα

Θεωρία και τεχνική του υδρατμού

Συνέχεια πίνακα I

Πίνακας II

Καταστατικά μεγέθη νερού και ατμού κατά τον κορεσμό (με βάση την θερμοκρασία) σε μονάδες του Δ.Σ.Μ.

°C <i>t</i>	kcal/kg		kcal/kg <i>r</i>	kcal/kg		kcal/kg <i>v</i>	$v'' - v'$	$\rho'' - \rho'$	$\rho' - \rho''$
	ρ'	ρ''		v'	v''				
200	203,5	667,3	463,8	203,1	620,1	417,0	46,8	46,8	
205	208,9	668,0	459,1	208,4	620,6	412,2	46,9	46,9	
210	214,3	668,6	454,3	213,8	621,1	407,3	47,0	47,0	
215	219,7	669,2	449,4	219,3	621,6	402,3	47,1	47,1	
220	225,2	669,6	444,4	224,5	621,9	397,4	47,1	47,1	
225	230,8	669,9	439,1	230,1	622,1	392,0	47,1	47,1	
230	236,4	670,0	433,6	235,6	622,3	386,7	47,0	47,0	
235	242,0	670,1	428,1	241,1	621,9	380,8	46,9	46,9	
240	247,7	670,0	422,3	246,7	622,2	375,5	46,7	46,7	
245	253,4	669,8	416,4	252,3	621,7	369,4	46,6	46,6	
250	259,2	669,4	410,2	258,0	621,8	363,8	46,3	46,3	
255	265,0	668,8	403,8	263,7	621,3	357,6	46,1	46,1	
260	270,9	668,1	397,2	269,5	620,9	351,4	45,8	45,8	
265	276,9	667,3	390,4	275,3	619,8	344,5	45,5	45,5	
270	282,9	666,3	383,4	281,2	619,6	338,4	45,1	45,1	
275	289,0	665,1	376,1	287,3	618,3	331,0	44,6	44,6	
280	295,2	663,7	368,5	293,2	617,6	324,4	44,1	44,1	
285	301,5	662,1	360,6	299,4	616,2	316,8	43,5	43,5	
290	307,9	660,4	352,5	305,5	614,9	309,4	42,9	42,9	
295	314,4	658,5	344,1	311,8	613,4	301,0	42,3	42,3	
300	321,1	656,3	335,2	318,2	611,9	293,7	41,5	41,5	
305	327,8	654,0	326,2	324,6	609,8	286,2	40,7	40,7	
310	334,7	651,5	316,8	331,3	608,4	277,1	39,7	39,7	
315	341,8	648,9	307,1	338,0	605,4	267,4	38,7	38,7	
320	349,0	645,5	296,5	345,0	603,7	258,7	37,7	37,7	
325	356,5	641,5	285,0	352,1	599,7	247,6	36,3	36,3	
330	364,2	636,9	272,7	359,4	597,0	237,6	35,1	35,1	
335	372,2	631,6	259,4	367,1	592,8	225,8	33,6	33,6	
340	380,6	625,8	245,2	374,9	588,2	213,3	31,9	31,9	
345	389,4	619,4	230,0	383,3	583,0	199,8	30,1	30,1	
350	398,9	612,0	213,1	392,0	577,2	185,2	27,9	27,9	
355	409,5	603,6	194,1	401,9	570,5	168,6	25,5	25,5	
360	420,9	593,1	172,2	412,4	562,0	149,6	22,6	22,6	
365	434,2	579,4	145,2	424,6	550,8	126,2	19,0	19,0	
370	452,3	558,9	106,6	441,1	533,0	91,9	13,9	13,9	
371	457,2	553,2	96,0	445,5	529,1	83,6	12,4	12,4	
372	462,9	546,3	83,4	450,7	523,3	72,6	10,8	10,8	
373	471,0	538,0	67,0	458,0	515,4	58,4	8,6	8,6	
374	488,0	522,5	34,5	473,3	503,4	30,1	4,4	4,4	
374,15		501,5	0	484,7		0	0	0	

°C <i>t</i>	bar <i>p</i>	dm ³ /kg v'	m ³ /kg v''	kg/m ³ ρ''	kJ/kg ^{°K}		$\rho'' - \rho'$
					ρ'	ρ''	
0	0,006107	1,0002	206,3	0,004846	0,0000	0,0000	9,1545
5	0,008722	1,0000	147,1	0,006797	0,0764	0,0764	8,9470
10	0,012275	1,0002	106,4	0,009399	0,1511	0,1511	8,8985
15	0,017045	1,0008	77,96	0,01283	0,2244	0,2244	8,7793
20	0,02337	1,0017	57,84	0,01729	0,2963	0,2963	8,6652
25	0,03166	1,0029	43,41	0,02304	0,3669	0,3669	8,5561
30	0,04241	1,0043	32,94	0,03036	0,4364	0,4364	8,4516
35	0,05621	1,0059	25,26	0,03960	0,5046	0,5046	8,3514
40	0,07374	1,0078	19,56	0,05114	0,5718	0,5718	8,2553
45	0,09581	1,0099	15,28	0,06543	0,6379	0,6379	8,1631
50	0,12334	1,0121	12,05	0,08298	0,7031	0,7031	8,0745
55	0,15740	1,0146	9,583	0,1044	0,7672	0,7672	7,9893
60	0,1992	1,0172	7,682	0,1302	0,8304	0,8304	7,9074
65	0,2501	1,0200	6,205	0,1612	0,8928	0,8928	7,8286
70	0,3116	1,0229	5,048	0,1981	0,9542	0,9542	7,7526
75	0,3855	1,0260	4,135	0,2418	1,0149	1,0149	7,6794
80	0,4780	1,0293	3,410	0,2933	1,0747	1,0747	7,6088
85	0,5780	1,0327	2,829	0,3535	1,1337	1,1337	7,5407
90	0,7011	1,0363	2,361	0,4235	1,1920	1,1920	7,4749
95	0,8453	1,0400	1,982	0,5045	1,2495	1,2495	7,4114
100	1,0132	1,0438	1,673	0,5978	1,3063	1,3063	7,3500
105	1,2080	1,0479	1,419	0,7047	1,3625	1,3625	7,2906
110	1,4326	1,0520	1,210	0,8267	1,4179	1,4179	7,2331
115	1,6905	1,0563	1,036	0,9652	1,4728	1,4728	7,1775
120	1,9853	1,0608	0,8913	1,122	1,5270	1,5270	7,1236
125	2,3208	1,0654	0,7700	1,299	1,5807	1,5807	7,0714
130	2,7011	1,0702	0,6679	1,497	1,6338	1,6338	7,0208
135	3,131	1,0751	0,5817	1,719	1,6863	1,6863	6,9717
140	3,614	1,0802	0,5084	1,967	1,7383	1,7383	6,9240
145	4,155	1,0855	0,4459	2,243	1,7899	1,7899	6,8776
150	4,760	1,0910	0,3924	2,548	1,8409	1,8409	6,8325
155	5,433	1,0966	0,3464	2,887	1,8915	1,8915	6,7885
160	6,180	1,1024	0,3068	3,260	1,9416	1,9416	6,7456
165	7,008	1,1085	0,2724	3,671	1,9913	1,9913	6,7037
170	7,920	1,1147	0,2426	4,122	2,0407	2,0407	6,6628
175	8,925	1,1211	0,2166	4,617	2,0896	2,0896	6,6227
180	10,027	1,1278	0,1939	5,158	2,1382	2,1382	6,5833
185	11,234	1,1347	0,1740	5,749	2,1864	2,1864	6,5447
190	12,552	1,1418	0,1564	6,393	2,2333	2,2333	6,5067
195	13,989	1,1491	0,1409	7,095	2,2820	2,2820	6,4692

°C t	bar p	dm ³ /kg v'	m ³ /kg v''	kg/m ³ ρ''	kJ/kg °K		ρ'' - ρ'
					u'	u''	
200	15,551	1,1568	0,1273	7,858	2,3293	6,4322	4,1029
205	17,245	1,1647	0,1151	8,686	2,3764	6,3955	4,0191
210	19,080	1,1729	0,1043	9,585	2,4232	6,3593	3,9361
215	21,063	1,1814	0,09471	10,56	2,4698	6,3233	3,8535
220	23,201	1,1903	0,08611	11,61	2,5162	6,2875	3,7713
225	25,504	1,1994	0,07841	12,75	2,5625	6,2518	3,6893
230	27,979	1,2090	0,07150	13,99	2,6086	6,2162	3,6076
235	30,635	1,2190	0,06528	15,32	2,6545	6,1807	3,5262
240	33,480	1,2293	0,05967	16,76	2,7004	6,1452	3,4448
245	36,524	1,2402	0,05460	18,31	2,7461	6,1096	3,3635
250	39,78	1,2515	0,05002	19,99	2,7918	6,0738	3,2820
255	43,24	1,2633	0,04586	21,80	2,8375	6,0380	3,2005
260	46,94	1,2757	0,04209	23,76	2,8832	6,0019	3,1187
265	50,87	1,2888	0,03865	25,87	2,9289	5,9656	3,0367
270	55,05	1,3025	0,03552	28,15	2,9747	5,9290	2,9543
275	59,49	1,3169	0,03266	30,62	3,0206	5,8921	2,8715
280	64,19	1,3322	0,03005	33,28	3,0666	5,8549	2,7883
285	69,17	1,3483	0,02766	36,16	3,1128	5,8174	2,7046
290	74,45	1,3655	0,02546	39,27	3,1593	5,7794	2,6201
295	80,03	1,3837	0,02345	42,65	3,2061	5,7410	2,5349
300	85,92	1,4033	0,02160	46,30	3,2532	5,7022	2,4490
305	92,14	1,424	0,01989	50,27	3,3008	5,6629	2,3621
310	98,70	1,447	0,01832	54,58	3,3489	5,6232	2,2743
315	105,61	1,471	0,01687	59,29	3,3977	5,5837	2,1860
320	112,90	1,498	0,01549	64,55	3,4473	5,5401	2,0928
325	120,57	1,527	0,01420	70,43	3,4978	5,4924	1,9946
330	128,05	1,560	0,01298	77,02	3,5495	5,4422	1,8927
335	137,14	1,597	0,01184	84,43	3,6026	5,3884	1,7858
340	146,08	1,638	0,01077	92,81	3,6577	5,3321	1,6744
345	155,48	1,687	0,009765	102,4	3,7154	5,2733	1,5579
350	165,37	1,746	0,008803	113,6	3,7768	5,2087	1,4319
355	175,77	1,817	0,007878	126,9	3,8431	5,1371	1,2940
360	186,74	1,908	0,006967	143,5	3,9159	5,0545	1,1386
365	198,30	2,03	0,006064	165,5	4,0013	4,9541	0,9528
370	210,52	2,23	0,00499	200	4,1131	4,8069	0,6838
371	213,06	2,30	0,00474	211	4,1437	4,7075	0,6238
372	215,62	2,37	0,00447	224	4,1801	4,7211	0,5410
373	218,22	2,49	0,00415	241	4,229	4,6625	0,434
374	220,86	2,79	0,00362	276	4,325	4,548	0,223
374,15	221,29	3,18	0,00318	315	4,430		0

°C t	kJ/kg		kJ/kg r	kJ/kg		u' - u'' - φ	(v'' - v') - v
	h'	h''		u'	u''		
0	0,00	2500,5	2500,5	2374,5	0	2374,5	126,0
5	21,05	2509,7	2488,6	2360,4	21,05	2339,3	128,2
10	42,03	2518,9	2476,9	2346,3	42,03	2314,2	130,6
15	62,96	2528,1	2465,1	2332,2	62,96	2290,1	132,9
20	83,86	2537,3	2453,4	2318,2	83,86	2267,0	135,3
25	104,74	2546,4	2441,7	2304,3	104,74	2244,8	137,4
30	125,61	2555,5	2429,9	2290,1	125,61	2223,6	139,8
35	146,47	2564,5	2418,0	2276,0	146,46	2204,9	142,0
40	167,34	2573,5	2406,2	2262,0	167,33	2190,4	144,2
45	188,22	2582,4	2394,2	2248,0	188,21	2175,8	146,4
50	209,11	2591,3	2382,2	2233,6	209,10	2161,1	148,6
55	230,00	2600,1	2370,1	2219,3	229,98	2146,3	150,8
60	250,91	2608,8	2357,9	2204,9	250,89	2131,5	153,0
65	271,84	2617,4	2345,5	2190,4	271,81	2116,5	155,2
70	292,78	2625,9	2333,1	2175,8	292,75	2101,4	157,3
75	313,74	2634,2	2320,5	2161,1	313,67	2086,1	159,4
80	334,72	2642,5	2307,8	2146,3	334,67	2070,8	171,3
85	355,72	2650,7	2295,0	2131,5	355,66	2055,3	173,1
90	376,75	2658,7	2281,9	2116,5	376,68	2039,8	174,9
95	397,80	2666,6	2268,8	2101,4	397,71	2024,0	176,7
100	418,88	2674,4	2255,5	2086,1	418,77	2008,1	178,5
105	439,99	2682,1	2242,1	2070,8	439,86	1992,1	180,1
110	461,13	2689,6	2228,5	2055,3	460,98	1975,8	181,8
115	482,31	2697,0	2214,7	2039,8	482,13	1959,6	183,3
120	503,5	2704,2	2200,7	2024,0	503,3	1943,1	184,8
125	524,8	2711,4	2186,6	2008,1	524,6	1926,3	186,3
130	546,1	2718,3	2172,2	1992,1	545,8	1909,5	187,6
135	567,5	2725,1	2157,6	1975,8	567,2	1892,4	188,9
140	588,9	2731,8	2142,9	1959,6	588,5	1875,2	190,1
145	610,4	2738,3	2127,9	1943,1	610,0	1857,6	191,2
150	631,9	2744,5	2112,6	1926,3	631,4	1839,7	192,3
155	653,5	2750,6	2097,1	1909,5	652,9	1821,6	193,3
160	675,2	2756,2	2081,3	1892,4	674,5	1803,1	194,2
165	696,9	2762,2	2065,3	1875,2	696,1	1784,4	194,9
170	718,8	2767,6	2048,8	1857,6	717,9	1765,3	195,5
175	740,7	2772,7	2032,0	1839,7	739,7	1745,8	196,0
180	762,7	2777,6	2014,9	1821,6	761,6	1726,3	196,5
185	784,8	2782,1	1997,3	1803,1	783,5	1706,8	197,0
190	807,0	2786,3	1979,3	1784,4	805,6	1687,3	197,5
195	829,4	2790,2	1960,8	1765,3	827,8	1667,8	198,0

Συνέχεια πίνακα II

Πίνακας III

Καταστατικά μεγέθη νερού και ατμού κατά τον κορεσμό (με βάση την πίεση) σε μονάδες του Τ.Σ.Μ.

at	p	°C		°K	m ³ /kg	kg/m ³	kcal/kg °K		s ⁰ -s ¹
		t	T				s ⁰	s ¹	
0,01	0,01	6,09	279,84	131,6	0,007597	0,0243	2,1450	2,1207	
0,015	0,15	12,73	285,88	89,64	0,01116	0,0457	2,1097	2,1037	
0,02	0,20	17,20	290,35	68,27	0,01465	0,0612	2,0848	2,0236	
0,025	0,25	20,78	293,93	55,28	0,01809	0,0734	2,0655	1,9921	
0,03	0,30	23,77	296,92	46,53	0,02149	0,0835	2,0499	1,9664	
0,04	0,40	28,65	301,80	35,46	0,02820	0,0998	2,0253	1,9255	
0,05	0,50	32,55	305,70	28,73	0,03481	0,1126	2,0063	1,8937	
0,06	0,60	35,83	308,98	24,19	0,04134	0,1232	1,9908	1,8676	
0,08	0,80	41,17	314,32	18,45	0,05421	0,1403	1,9665	1,8262	
0,10	1,00	45,45	318,60	14,95	0,06688	0,1538	1,9478	1,7940	
0,12	1,20	49,06	322,21	12,60	0,07739	0,1650	1,9325	1,7675	
0,15	1,50	53,60	326,75	10,21	0,09792	0,1790	1,9139	1,7349	
0,20	2,00	59,67	332,82	7,794	0,1283	0,1974	1,8899	1,6925	
0,25	2,50	64,56	337,71	6,321	0,1582	0,2119	1,8715	1,6596	
0,30	3,00	68,68	341,83	5,328	0,1877	0,2241	1,8564	1,6324	
0,35	3,50	72,24	345,39	4,614	0,2169	0,2345	1,8437	1,6092	
0,40	4,00	75,42	348,57	4,068	0,2458	0,2436	1,8328	1,5892	
0,50	5,00	80,86	354,01	3,301	0,3030	0,2591	1,8145	1,5554	
0,60	6,00	85,45	358,60	2,782	0,3576	0,2720	1,7996	1,5276	
0,70	7,00	89,45	362,60	2,408	0,4152	0,2832	1,7871	1,5039	
0,80	8,00	92,99	366,14	2,125	0,4705	0,2929	1,7762	1,4833	
0,90	9,00	96,18	369,33	1,904	0,5253	0,3017	1,7667	1,4650	
1,0	10,00	99,09	372,24	1,725	0,5798	0,3095	1,7582	1,4487	
1,1	11,00	101,76	374,91	1,578	0,6339	0,3167	1,7504	1,4337	
1,2	12,00	104,25	377,40	1,454	0,6876	0,3234	1,7434	1,4200	
1,3	13,00	106,56	379,71	1,349	0,7411	0,3296	1,7370	1,4074	
1,4	14,00	108,74	381,89	1,259	0,7944	0,3353	1,7310	1,3957	
1,5	15,00	110,79	384,94	1,180	0,8474	0,3407	1,7255	1,3848	
1,6	16,00	112,73	385,88	1,111	0,9001	0,3458	1,7203	1,3745	
1,8	18,00	116,33	389,48	0,9950	1,005	0,3552	1,7109	1,3557	
2,0	20,00	119,62	392,77	0,9015	1,109	0,3637	1,7024	1,3387	
2,2	22,00	122,64	395,79	0,8245	1,213	0,3715	1,6948	1,3233	
2,4	24,00	125,46	398,61	0,7600	1,316	0,3787	1,6879	1,3092	
2,6	26,00	128,08	401,23	0,7051	1,418	0,3854	1,6815	1,2961	
2,8	28,00	130,55	403,70	0,6577	1,520	0,3916	1,6756	1,2840	
3,0	30,00	132,88	406,03	0,6165	1,622	0,3975	1,6701	1,2726	
3,2	32,00	135,08	408,23	0,5803	1,723	0,4030	1,6650	1,2620	
3,4	34,00	137,18	410,33	0,5482	1,824	0,4082	1,6601	1,2519	
3,6	36,00	139,18	412,33	0,5196	1,925	0,4132	1,6556	1,2424	
3,8	38,00	141,09	414,24	0,4939	2,025	0,4179	1,6513	1,2334	
4,0	40,00	142,92	416,07	0,4706	2,125	0,4224	1,6472	1,2248	
4,5	45,00	147,20	420,35	0,4213	2,373	0,4329	1,6379	1,2050	
5,0	50,00	151,11	424,26	0,3816	2,621	0,4424	1,6295	1,1871	
5,5	55,00	154,71	427,86	0,3489	2,867	0,4511	1,6220	1,1709	
6,0	60,00	158,08	431,23	0,3213	3,112	0,4592	1,6161	1,1561	
6,5	65,00	161,21	434,36	0,2980	3,356	0,4666	1,6087	1,1422	
7,0	70,00	164,17	437,32	0,2778	3,600	0,4737	1,6028	1,1291	

°C	kJ/kg		kJ/kg	kJ/kg		u'' - u'	p - v
	h'	h''		u'	u''		
200	851,8	2793,7	1941,9	850,0	2595,7	1745,7	196,2
205	874,4	2796,8	1922,4	872,4	2598,3	1725,9	196,5
210	897,1	2799,4	1902,3	894,9	2600,4	1705,5	196,8
215	920,0	2801,7	1881,7	917,5	2602,3	1684,8	196,9
220	943,0	2803,4	1860,4	940,2	2603,6	1663,4	197,0
225	966,2	2804,6	1838,4	963,1	2604,6	1641,5	196,9
230	989,6	2805,4	1815,8	986,2	2605,4	1619,2	196,6
235	1013,2	2805,5	1792,4	1009,5	2605,5	1596,0	196,3
240	1036,9	2805,1	1768,2	1032,8	2605,3	1572,5	195,7
245	1060,9	2804,1	1743,3	1056,4	2604,7	1548,3	194,9
250	1085,1	2802,5	1717,4	1080,1	2603,5	1523,4	194,0
255	1109,5	2800,3	1690,7	1104,0	2602,0	1498,0	192,8
260	1134,3	2797,4	1663,1	1128,3	2599,8	1471,5	191,6
265	1159,3	2793,8	1634,5	1152,8	2597,2	1444,4	190,1
270	1184,5	2789,5	1604,9	1177,3	2594,0	1416,7	188,3
275	1210,2	2784,5	1574,3	1202,4	2590,2	1387,8	186,5
280	1236,1	2778,7	1542,5	1227,5	2585,8	1358,3	184,3
285	1262,5	2772,2	1509,6	1253,2	2580,9	1327,7	182,0
290	1289,3	2764,9	1475,6	1279,1	2575,4	1296,3	179,3
295	1316,5	2756,9	1440,2	1305,4	2569,2	1263,8	176,6
300	1344,2	2748,0	1403,6	1332,1	2562,4	1230,3	173,5
305	1372,5	2738,3	1365,5	1359,4	2555,1	1195,7	170,1
310	1401,3	2727,7	1326,0	1387,0	2546,9	1159,9	166,5
315	1430,9	2716,8	1285,8	1415,4	2538,6	1123,2	162,7
320	1461,3	2702,4	1241,3	1444,4	2527,5	1083,1	158,0
325	1492,5	2685,7	1193,1	1474,1	2514,5	1040,4	152,8
330	1524,8	2666,4	1141,5	1504,7	2499,4	994,7	146,9
335	1558,4	2644,3	1086,0	1536,5	2481,9	945,5	140,5
340	1593,5	2620,2	1026,7	1569,6	2462,9	893,3	133,4
345	1630,5	2593,4	963,0	1604,3	2441,0	837,3	125,6
350	1670,3	2562,3	892,2	1641,4	2416,7	775,3	116,7
355	1714,5	2527,3	812,8	1682,6	2388,8	706,2	106,6
360	1762,2	2483,1	720,9	1726,6	2353,0	626,4	94,5
365	1817,9	2425,9	608,0	1777,6	2306,1	528,5	79,5
370	1893,7	2339,9	446,2	1846,8	2234,9	388,1	58,1
371	1914,2	2316,1	401,9	1865,2	2214,2	349,0	52,9
372	1938,1	2287,1	349,0	1887,0	2190,7	303,7	45,3
373	1972,0	2252,3	280,4	1917,7	2161,7	244,0	36,3
374	2043,2	2187,5	144,4	1981,6	2107,5	125,9	18,4
374,15	2099,7	2099,7	0	2029,3	2029,3	0	0

Συνέχεια πίνακα III

at	p	°C t	kcal/kg		kcal/kg r	kcal/kg		u'' - u'	p'' - p'
			ε'	ε''		u'	u''		
0,01		6,69	6,72	600,2	593,5	6,72	599,2	562,5	30,8
0,015		12,73	12,77	602,9	590,1	12,77	571,4	558,6	31,5
0,02		17,23	17,23	604,8	587,6	17,23	572,6	555,4	32,1
0,025		20,78	20,80	606,4	585,6	20,80	574,0	553,2	32,4
0,03		23,77	23,79	607,7	583,9	23,79	575,0	551,2	32,7
0,04		28,65	28,65	609,8	581,1	28,65	576,6	547,9	33,2
0,05		32,55	32,54	611,5	579,0	32,54	577,9	545,4	33,6
0,06		35,83	35,81	612,9	577,1	35,81	578,9	543,1	34,0
0,08		41,17	41,14	615,2	574,1	41,14	580,6	539,5	34,5
0,10		45,45	45,40	617,0	571,6	45,40	582,0	536,6	35,0
0,12		49,06	49,01	618,5	569,5	49,01	583,1	534,1	35,4
0,15		53,60	53,54	620,4	566,9	53,54	584,6	531,1	35,8
0,20		59,67	59,60	623,0	563,4	59,60	586,5	526,9	36,5
0,25		64,56	64,49	625,0	560,5	64,48	587,4	522,9	37,0
0,30		68,08	68,61	626,6	558,0	68,60	589,3	520,7	37,3
0,35		72,24	72,17	628,1	555,9	72,16	590,2	518,0	37,8
0,40		75,42	75,36	629,4	553,9	75,35	591,3	515,9	38,1
0,50		80,86	80,81	631,5	550,7	80,80	592,9	512,1	38,6
0,60		85,45	85,41	633,3	547,9	85,40	594,2	508,8	39,1
0,70		89,45	89,43	634,8	545,4	89,41	595,3	505,9	39,5
0,80		92,99	92,99	636,2	543,2	92,97	596,4	503,4	39,8
0,90		96,18	96,20	637,4	541,2	96,18	597,3	501,1	40,1
1,0		99,09	99,13	638,4	539,3	99,11	598,2	499,1	40,3
1,1		101,76	101,82	639,4	537,6	101,79	598,8	497,0	40,6
1,2		104,25	104,33	640,3	536,0	104,30	599,4	495,1	40,9
1,3		106,56	106,66	641,2	534,5	106,63	600,0	493,4	41,1
1,4		108,74	108,87	642,0	533,1	108,84	600,7	491,9	41,2
1,5		110,79	110,94	642,7	531,8	110,90	601,3	490,4	41,4
1,6		112,73	112,90	643,4	530,5	112,86	601,8	488,9	41,6
1,8		116,33	116,55	644,6	528,1	116,51	602,7	486,2	41,9
2,0		119,62	119,88	645,8	525,9	119,83	603,5	483,7	42,2
2,2		122,64	122,9	646,8	523,8	122,8	604,3	481,5	42,4
2,4		125,46	125,8	647,8	521,9	125,7	605,0	479,3	42,6
2,6		128,08	128,5	648,6	520,1	128,4	605,6	477,2	42,9
2,8		130,55	131,0	649,5	518,4	130,9	606,3	475,4	43,1
3,0		132,88	133,4	650,2	516,8	133,4	607,0	473,7	43,2
3,2		135,08	135,6	650,9	515,3	135,5	607,4	471,9	43,4
3,4		137,18	137,8	651,6	513,8	137,7	607,9	470,2	43,6
3,6		139,18	139,8	652,2	512,4	139,7	608,4	468,7	43,7
3,8		141,09	141,8	652,8	511,0	141,7	608,8	467,1	43,9
4,0		142,92	143,6	653,4	509,8	143,5	609,3	465,8	44,0
4,5		147,20	148,0	654,7	506,7	147,9	610,3	462,4	44,3
5,0		151,11	152,1	655,9	503,8	152,0	611,2	459,2	44,6
5,5		154,71	155,8	656,0	501,1	155,7	612,0	456,3	44,8
6,0		158,08	159,3	657,9	498,6	159,1	612,7	453,6	45,0
6,5		161,21	162,6	658,8	496,2	162,4	613,5	451,1	45,2
7,0		164,17	165,6	659,5	493,9	165,4	613,9	448,5	45,4

Θεωρία και τεχνική του υδρατμού

Συνέχεια πίνακα III

at	p	°C		°K T	m ³ /kg v''	kg/m ³ ρ''	kcal/kg °K		s'' - s'
		t	T				s'	s''	
7,5		166,96	440,11	0,2603	3,842	0,4803	1,5973	1,1170	
8,0		169,61	442,76	0,2448	4,085	0,4865	1,5921	1,1056	
8,5		172,12	445,27	0,2311	4,327	0,4923	1,5873	1,0950	
9,0		174,53	447,68	0,2189	4,568	0,4980	1,5827	1,0847	
9,5		176,82	449,97	0,2080	4,809	0,5033	1,5783	1,0750	
10		179,04	452,19	0,1980	5,050	0,5085	1,5742	1,0667	
11		183,20	456,35	0,1808	5,530	0,5181	1,5665	1,0484	
12		187,08	460,23	0,1664	6,010	0,5270	1,5594	1,0324	
13		190,71	463,86	0,1541	6,489	0,5353	1,5528	1,0175	
14		194,13	467,28	0,1435	6,968	0,5431	1,5467	1,0036	
15		197,36	470,51	0,1343	7,447	0,5504	1,5409	0,9905	
16		200,43	473,58	0,1262	7,926	0,5573	1,5355	0,9782	
17		203,35	476,50	0,1190	8,405	0,5639	1,5304	0,9665	
18		206,14	479,29	0,1125	8,885	0,5701	1,5256	0,9555	
19		208,82	481,97	0,1068	9,365	0,5761	1,5209	0,9448	
20		211,38	484,53	0,1016	9,846	0,5818	1,5165	0,9347	
22		216,23	489,38	0,09250	10,81	0,5926	1,5082	0,9156	
24		220,75	493,90	0,08490	11,78	0,6027	1,5005	0,8978	
26		224,99	498,14	0,07843	12,75	0,6120	1,4932	0,8812	
28		228,98	502,13	0,07285	13,73	0,6208	1,4865	0,8657	
30		232,76	505,91	0,06799	14,71	0,6291	1,4801	0,8510	
32		236,35	509,50	0,06371	15,70	0,6370	1,4740	0,8370	
34		239,77	512,92	0,05992	16,69	0,6445	1,4682	0,8237	
36		243,04	516,19	0,05653	17,69	0,6516	1,4626	0,8110	
38		246,17	519,32	0,05349	18,69	0,6585	1,4573	0,7988	
40		249,18	522,33	0,05074	19,71	0,6650	1,4521	0,7871	
42		252,07	525,22	0,04825	20,73	0,6713	1,4472	0,7759	
44		254,87	528,02	0,04597	21,75	0,6774	1,4424	0,7650	
46		257,56	530,71	0,04388	22,79	0,6833	1,4377	0,7544	
48		260,17	533,32	0,04196	23,83	0,6890	1,4332	0,7442	
50		262,70	535,85	0,04019	24,88	0,6945	1,4289	0,7344	
55		268,70	541,85	0,03631	27,54	0,7076	1,4184	0,7108	
60		274,29	547,44	0,03305	30,25	0,7199	1,4086	0,6887	
65		279,54	552,69	0,03028	33,02	0,7314	1,3993	0,6679	
70		284,48	557,63	0,02789	35,85	0,7423	1,3904	0,6481	
75		289,17	562,32	0,02582	38,74	0,7527	1,3819	0,6292	
80		293,62	566,77	0,02399	41,69	0,7627	1,3738	0,6111	
85		297,86	571,01	0,02237	44,70	0,7722	1,3659	0,5937	
90		301,92	575,07	0,02093	47,78	0,7814	1,3584	0,5770	
95		305,80	578,95	0,01963	50,93	0,7902	1,3511	0,5609	
100		309,53	582,68	0,01846	54,16	0,7988	1,3440	0,5452	
110		316,58	589,73	0,01642	60,89	0,8152	1,3302	0,5150	
120		323,15	596,30	0,01467	68,18	0,8309	1,3160	0,4851	
130		329,30	602,45	0,01315	76,05	0,8460	1,3015	0,4555	
140		335,09	608,24	0,01183	84,57	0,8607	1,2868	0,4259	
150		340,56	613,71	0,01066	93,82	0,8751	1,2719	0,3968	
160		345,74	618,89	0,009620	104,0	0,8895	1,2571	0,3676	
180		355,35	628,50	0,007814	128,0	0,9191	1,2259	0,3068	
200		364,08	637,23	0,00622	161,9	0,9516	1,1880	0,2364	
224		373,6	146,75	0,00389	257	1,0204	1,1012	0,0808	
225,65		374,15	647,30	0,00318	315	1,058		0	

Θεωρία και τεχνική του υδρατμού

Παράρτημα

Συνέχεια πίνακα III

Πίνακας IV Καταστατικά μεγέθη νερού και ατμού κατά τον κορεσμό (με βάση την πίεση) σε μονάδες του Δ.Σ.Μ.

at	P	°C	kcal/kg		kcal/kg	kcal/kg	kcal/kg		u' - u''	p' - p''
			f'	f''			r	u'		
7,5		166,96	168,5	660,2	491,7	168,3	614,5	446,2	45,5	
8,0		169,61	171,3	660,9	489,6	171,1	614,9	443,8	45,8	
8,5		172,12	173,9	661,5	487,7	173,7	615,4	441,7	45,9	
9,0		174,53	176,4	662,1	485,7	176,2	615,9	439,7	45,9	
9,5		176,82	178,9	662,7	483,8	178,6	616,4	437,8	46,0	
10		179,04	181,2	663,2	482,0	180,9	616,8	435,9	46,1	
11		183,20	185,5	664,1	478,6	185,2	617,5	432,3	46,3	
12		187,08	189,7	664,9	475,3	189,4	618,2	428,8	46,4	
13		190,71	193,5	665,7	472,1	193,2	618,8	425,6	46,5	
14		194,13	197,2	666,3	469,1	196,8	619,2	422,4	46,7	
15		197,36	200,6	666,8	466,2	200,2	619,6	419,4	46,8	
16		200,43	203,9	667,3	463,4	203,5	620,0	416,5	46,9	
17		203,35	207,1	667,8	460,7	206,6	620,4	413,8	46,9	
18		206,14	210,1	668,2	458,1	209,6	620,7	411,1	47,0	
19		208,82	213,0	668,5	455,5	212,5	621,0	408,5	47,0	
20		211,38	215,8	668,8	453,0	215,2	621,2	406,0	47,0	
22		216,23	221,1	669,3	448,2	220,5	621,6	401,1	47,1	
24		220,75	226,1	669,6	443,6	225,4	621,8	396,4	47,1	
26		224,99	230,8	669,9	439,1	230,1	622,2	392,1	47,0	
28		228,98	235,2	670,0	434,8	234,4	622,2	387,8	47,0	
30		232,76	239,5	670,1	430,6	238,6	622,3	383,7	46,9	
32		236,35	243,5	670,1	426,6	242,6	622,3	379,7	46,9	
34		239,74	247,4	670,0	422,6	246,4	622,2	375,8	46,8	
36		243,04	251,1	669,9	418,7	250,1	622,2	372,1	46,7	
38		246,17	254,7	669,7	414,9	253,6	622,1	368,5	46,5	
40		249,18	258,2	669,5	411,3	257,0	621,9	364,9	46,4	
42		252,07	261,6	669,2	407,6	260,4	621,7	361,3	46,3	
44		254,87	264,9	668,9	404,0	263,6	621,5	357,9	46,1	
46		257,56	268,0	668,5	400,5	266,6	621,1	354,5	46,0	
48		260,17	271,1	668,1	397,0	269,7	620,9	352,2	45,8	
50		262,70	274,1	667,7	393,6	272,6	620,6	348,0	45,6	
55		268,70	281,3	666,5	385,2	279,6	619,7	340,1	45,2	
60		274,29	288,2	665,2	377,0	286,4	618,8	332,4	44,7	
65		279,54	294,7	663,8	369,1	292,7	617,7	325,0	44,1	
70		284,48	300,9	662,3	361,4	298,7	616,5	317,8	43,6	
75		289,17	306,9	660,7	353,8	304,5	615,3	310,8	43,0	
80		293,62	312,6	659,0	346,4	310,0	613,9	303,9	42,5	
85		297,86	318,2	657,3	339,1	315,4	612,7	297,3	41,8	
90		301,92	323,6	655,5	331,9	320,6	611,3	290,7	41,2	
95		305,80	328,9	653,6	324,7	325,7	609,9	284,2	40,5	
100		309,53	334,1	651,7	317,6	330,7	608,5	277,8	39,8	
110		316,58	344,0	647,7	303,7	340,2	605,5	265,3	38,4	
120		323,15	353,7	643,0	289,3	349,4	601,9	251,5	36,8	
130		329,30	363,1	637,5	274,4	358,4	597,6	239,2	35,2	
140		335,09	372,4	631,6	259,2	367,2	592,9	225,7	33,5	
150		340,56	381,6	625,1	243,5	375,8	587,7	211,9	31,6	
160		345,74	390,8	618,3	227,5	384,4	582,2	197,8	29,7	
180		355,35	410,2	603,0	192,8	402,5	570,1	167,6	25,2	
200		364,08	431,5	582,1	150,7	422,1	553,2	131,1	19,6	
224		373,6	478,5	530,8	52,3	464,8	510,4	45,6	6,7	
225,65		374,15	501,5	0	0	484,7	484,7	0	0	

bar	°C		°K	m ³ /kg	kg/m ³	kJ/kg		r/T
	t	T				e'	e''	
0,01	6,98	280,14	280,14	129,2	0,00773	0,1061	8,9734	8,8673
0,015	13,03	286,19	286,19	87,99	0,01136	0,1957	8,8256	8,6299
0,02	17,51	290,67	290,67	67,02	0,01492	0,2607	8,7214	8,4607
0,025	21,09	294,25	294,25	54,27	0,01843	0,3119	8,6409	8,3290
0,03	24,10	297,26	297,26	45,68	0,02189	0,3543	8,5754	8,2211
0,04	28,98	302,14	302,14	34,81	0,02873	0,4223	8,4725	8,0502
0,05	32,90	306,06	306,06	28,20	0,03546	0,4761	8,3930	7,9169
0,06	36,19	309,35	309,35	23,75	0,04211	0,5206	8,3283	7,8077
0,08	41,54	314,70	314,70	18,11	0,05522	0,5922	8,2266	7,6344
0,10	45,84	319,00	319,00	14,68	0,06812	0,6489	8,1480	7,4991
0,12	49,45	322,61	322,61	12,37	0,08086	0,6959	8,0841	7,3882
0,15	54,00	327,16	327,16	10,03	0,09974	0,7545	8,0061	7,2516
0,20	60,09	333,25	333,25	7,652	0,1307	0,8316	7,9060	7,0744
0,25	64,99	338,15	338,15	6,206	0,1611	0,8927	7,8287	6,9360
0,30	69,12	342,28	342,28	5,231	0,1912	0,9435	7,7657	6,8222
0,40	75,89	349,05	349,05	3,994	0,2504	1,0255	7,6667	6,6412
0,50	81,35	354,51	354,51	3,241	0,3086	1,0906	7,5903	6,4997
0,60	85,95	359,11	359,11	2,732	0,3660	1,1449	7,5280	6,3831
0,70	89,96	363,12	363,12	2,305	0,4229	1,1915	7,4754	6,2839
0,80	93,51	366,67	366,67	2,087	0,4792	1,2324	7,4300	6,1976
0,90	96,71	369,87	369,87	1,869	0,5350	1,2690	7,3901	6,1211
1,0	99,63	372,79	372,79	1,694	0,5905	1,3022	7,3544	6,0522
1,1	102,32	375,48	375,48	1,549	0,6456	1,3324	7,3222	5,9898
1,2	104,81	377,97	377,97	1,428	0,7003	1,3603	7,2928	5,9325
1,3	107,13	380,29	380,29	1,325	0,7548	1,3862	7,2658	5,8796
1,4	109,32	382,48	382,48	1,236	0,8090	1,4104	7,2409	5,8305
1,5	111,37	384,53	384,53	1,159	0,8630	1,4331	7,2177	5,7846
1,6	113,32	386,48	386,48	1,091	0,9167	1,4544	7,1960	5,7416
1,8	116,93	390,09	390,09	0,9769	1,024	1,4938	7,1565	5,6627
2,0	120,23	393,39	393,39	0,8852	1,130	1,5295	7,1212	5,5917
2,2	123,27	396,43	396,43	0,8096	1,235	1,5622	7,0893	5,5271
2,4	126,09	399,25	399,25	0,7462	1,340	1,5923	7,0602	5,4679
2,6	128,73	401,89	401,89	0,6923	1,445	1,6203	7,0335	5,4132
2,8	131,21	404,37	404,37	0,6458	1,548	1,6465	7,0088	5,3623
3,0	133,54	406,70	406,70	0,6054	1,652	1,6711	6,9859	5,3148
3,2	135,76	408,92	408,92	0,5698	1,755	1,6942	6,9644	5,2702
3,4	137,86	411,02	411,02	0,5383	1,858	1,7161	6,9442	5,2281
3,6	139,87	413,03	413,03	0,5102	1,960	1,7370	6,9252	5,1882
3,8	141,79	414,95	414,95	0,4849	2,062	1,7568	6,9072	5,1504
4,0	143,63	416,79	416,79	0,4621	2,164	1,7757	6,8902	5,1145
4,5	147,92	421,08	421,08	0,4137	2,417	1,8197	6,8511	5,0314
5,0	151,85	425,01	425,01	0,3746	2,669	1,8596	6,8161	4,9565
6,0	158,84	432,00	432,00	0,3155	3,170	1,9300	6,7555	4,8255
7,0	164,96	438,12	438,12	0,2727	3,667	1,9909	6,7041	4,7132
8,0	170,41	443,57	443,57	0,2403	4,161	2,0447	6,6594	4,6147
9,0	175,36	448,52	448,52	0,2149	4,654	2,0931	6,6198	4,5267
10,0	179,88	453,04	453,04	0,1944	5,144	2,1370	6,5843	4,4473

Θεωρία και Γεωμετρική του υδρατμού

Συνέχεια Πίνακα IV

bar p	°C		°K T	m³/kg v'	kg/m³ ρ''	kJ/kg·K		s'' - s'
	t	τ				s'	s''	
11,0	184,06	457,22	0,1775	5,634	2,1774	6,5519	4,3745	
12,0	187,96	461,12	0,1633	6,123	2,2148	6,5221	4,3073	
13,0	191,60	464,76	0,1512	6,612	2,2497	6,4946	4,2449	
14,0	195,04	468,20	0,1408	7,100	2,2823	6,4689	4,1866	
15,0	198,28	471,44	0,1318	7,589	2,3131	6,4448	4,1317	
16,0	201,37	474,53	0,1238	8,077	2,3422	6,4221	4,0799	
17,0	204,30	477,40	0,1167	8,566	2,3698	6,4006	4,0308	
18,0	207,11	480,27	0,1104	9,056	2,3961	6,3802	3,9841	
19,0	209,79	482,95	0,1048	9,546	2,4212	6,3608	3,9396	
20,0	212,37	485,53	0,09964	10,04	2,4453	6,3422	3,8969	
22,0	217,24	490,40	0,09074	11,02	2,4906	6,3072	3,8160	
24,0	221,78	494,94	0,08328	12,01	2,5327	6,2748	3,7421	
26,0	226,03	499,19	0,07692	13,00	2,5720	6,2445	3,6725	
28,0	230,04	503,20	0,07144	14,00	2,6089	6,2159	3,6070	
30,0	233,84	507,00	0,06667	15,00	2,6438	6,1890	3,5452	
32	237,44	510,60	0,06247	16,01	2,6769	6,1634	3,4865	
34	240,88	514,04	0,05874	17,02	2,7084	6,1389	3,4305	
36	244,16	517,32	0,05542	18,05	2,7385	6,1155	3,3770	
38	247,31	520,47	0,05243	19,07	2,7672	6,0931	3,3259	
40	250,33	523,49	0,04973	20,11	2,7949	6,0714	3,2765	
42	253,24	526,40	0,04728	21,15	2,8215	6,0506	3,2291	
44	256,05	529,21	0,04504	22,20	2,8471	6,0304	3,1833	
46	258,76	531,92	0,04299	23,26	2,8718	6,0109	3,1391	
48	261,38	534,54	0,04111	24,33	2,8958	5,9919	3,0961	
50	263,92	537,08	0,03937	25,40	2,9190	5,9735	3,0545	
55	269,94	543,10	0,03556	28,12	2,9741	5,9294	2,9553	
60	275,56	548,72	0,03236	30,90	3,0257	5,8880	2,8623	
65	280,83	553,99	0,02904	33,74	3,0743	5,8487	2,7744	
70	285,80	558,96	0,02729	36,64	3,1203	5,8113	2,6910	
75	290,51	563,67	0,02525	39,60	3,1640	5,7755	2,6115	
80	294,98	568,14	0,02346	42,63	3,2059	5,7412	2,5363	
85	299,24	572,40	0,02187	45,73	3,2460	5,7081	2,4621	
90	303,31	576,47	0,02045	48,89	3,2847	5,6762	2,3915	
95	307,22	580,38	0,01918	52,13	3,3220	5,6454	2,3234	
100	310,96	584,12	0,01803	55,45	3,3582	5,6155	2,2573	
110	318,04	591,20	0,01602	62,42	3,4277	5,5584	2,1307	
120	324,44	597,80	0,01429	69,98	3,4941	5,4971	2,0030	
130	330,81	603,97	0,01279	78,17	3,5580	5,4353	1,8773	
140	336,63	609,79	0,01149	87,04	3,6203	5,3726	1,7523	
150	342,12	615,28	0,01034	96,71	3,6818	5,3104	1,6286	
160	347,32	620,48	0,009314	107,4	3,7433	5,2471	1,5038	
180	356,96	630,12	0,007518	133,0	3,8707	5,1062	1,2355	
200	365,71	638,87	0,00591	169,3	4,0151	4,9375	0,9224	
220	373,7	646,86	0,00385	260	4,2802	4,6023	0,3221	
221,29	374,11	647,31	0,00318	315	4,430	0	0	

Παράρτημα

Συνέχεια Πίνακα IV

bar p	kJ/kg		kJ/kg τ	kJ/kg		u'' - u'		p - v' (v'' - v')
	h'	h''		u'	u''	φ	v	
0,01	29,35	2513,4	2484,0	29,35	2384,2	2354,9	129,2	
0,015	54,72	2524,5	2469,8	54,72	2392,5	2337,8	131,9	
0,02	73,45	2532,7	2459,3	73,45	2398,7	2325,3	134,0	
0,025	88,43	2539,3	2450,8	88,43	2403,6	2315,2	135,7	
0,03	100,97	2544,7	2443,8	100,97	2407,7	2306,7	137,0	
0,04	121,36	2553,6	2432,3	121,36	2414,4	2293,0	139,2	
0,05	137,71	2560,7	2423,0	137,71	2419,7	2282,0	141,0	
0,06	151,42	2566,7	2415,2	151,42	2424,2	2272,8	142,5	
0,08	173,76	2576,3	2402,5	173,76	2431,4	2257,6	144,9	
0,10	191,71	2583,9	2392,2	191,70	2437,1	2245,4	146,8	
0,12	206,80	2590,3	2383,5	206,79	2441,9	2235,1	148,4	
0,15	225,82	2598,3	2372,5	225,80	2447,9	2222,1	150,5	
0,20	251,28	2608,9	2357,6	251,26	2455,9	2204,6	153,0	
0,25	271,81	2617,4	2345,6	271,78	2462,3	2190,5	155,1	
0,30	289,11	2624,4	2335,3	289,08	2467,5	2178,4	156,9	
0,40	317,46	2635,7	2318,3	317,42	2475,9	2158,5	159,7	
0,50	340,37	2644,7	2304,4	340,32	2482,7	2142,4	162,0	
0,60	359,73	2652,2	2292,5	359,67	2488,3	2128,6	163,9	
0,70	376,58	2658,6	2282,1	376,51	2493,1	2116,6	165,5	
0,80	391,83	2664,3	2272,7	391,45	2497,3	2105,9	166,9	
0,90	405,02	2669,3	2264,3	404,93	2501,1	2096,2	168,1	
1,0	417,33	2673,8	2256,5	417,23	2504,4	2087,2	169,3	
1,1	428,66	2678,0	2249,3	428,55	2507,6	2079,1	170,3	
1,2	439,18	2681,8	2242,6	439,05	2510,4	2071,4	171,2	
1,3	449,01	2685,3	2236,3	448,78	2513,1	2064,3	172,1	
1,4	458,24	2688,6	2230,3	458,09	2515,6	2057,5	172,9	
1,5	466,95	2691,6	2224,7	466,79	2517,8	2051,0	173,7	
1,6	475,20	2694,5	2219,3	475,03	2519,9	2044,9	174,4	
1,8	490,52	2699,8	2209,3	490,33	2524,0	2033,7	175,7	
2,0	504,52	2704,6	2200,1	504,31	2527,6	2023,3	176,8	
2,2	517,4	2708,9	2191,5	517,2	2531,2	2014,2	177,3	
2,4	529,5	2712,9	2183,4	529,2	2533,8	2006,0	178,8	
2,6	540,7	2716,6	2175,9	540,4	2536,6	1996,2	179,7	
2,8	551,3	2720,0	2168,7	551,0	2539,2	1988,2	180,5	
3,0	561,2	2723,2	2161,9	560,9	2541,7	1976,1	181,3	
3,2	570,7	2726,2	2155,5	570,4	2543,9	1973,5	182,0	
3,4	579,7	2729,0	2149,2	579,3	2546,0	1966,7	182,7	
3,6	588,3	2731,6	2143,3	587,9	2547,9	1960,0	183,3	
3,8	596,5	2734,1	2137,6	596,1	2549,8	1953,7	183,9	
4,0	604,4	2736,5	2132,1	604,0	2551,7	1947,7	184,4	
4,5	622,9	2742,0	2119,0	622,4	2555,8	1933,4	185,7	
5,0	639,9	2746,8	2107,0	639,4	2559,5	1920,1	186,8	
6,0	670,1	2755,2	2085,1	669,4	2565,9	1896,5	188,6	
7,0	696,7	2762,1	2065,4	695,6	2571,2	1875,6	190,1	
8,0	720,6	2768,0	2047,5	719,7	2575,8	1856,1	191,4	
9,0	742,2	2773,1	2030,8	741,2	2579,7	1839,5	192,4	
10,0	762,2	2777,5	2015,3	761,1	2583,1	1825,0	193,3	

Θεωρία και Γεχνική του υδρατμού

Πίνακας V

Καταστατικά μεγέθη νερού και υπερθέρσιμου ατμού
σε μονάδες του I.C.M.

t °C	1.0 at			5.0 at			10.0 at			25 at		
	v	u	s	v	u	s	v	u	s	v	u	s
0	0.001000	0.0	0.0000	0.001000	0.1	0.0000	0.001000	0.2	0.0000	0.000000	0.6	0.0001
10	0.001000	10.1	0.0361	0.001000	20.1	0.0361	0.001000	10.3	0.0361	0.000000	10.6	0.0361
20	0.001002	20.1	0.0708	0.001002	20.1	0.0708	0.001000	20.2	0.0708	0.000000	20.6	0.0707
30	0.001004	30.0	0.1042	0.001004	30.1	0.1042	0.001004	30.2	0.1042	0.000003	30.5	0.1040
40	0.001008	40.0	0.1366	0.001008	40.1	0.1366	0.001008	40.2	0.1366	0.000007	40.5	0.1363
50	0.001012	50.0	0.1679	0.001012	50.0	0.1679	0.001012	50.1	0.1678	0.000011	50.4	0.1676
60	0.001017	59.9	0.1983	0.001017	60.0	0.1983	0.001017	60.1	0.1982	0.000016	60.4	0.1980
70	0.001023	69.9	0.2278	0.001023	70.0	0.2278	0.001023	70.1	0.2278	0.000022	70.4	0.2276
80	0.001029	80.0	0.2567	0.001029	80.0	0.2567	0.001029	80.1	0.2566	0.000028	80.4	0.2563
90	0.001038	90.0	0.2847	0.001038	90.1	0.2846	0.001038	90.2	0.2845	0.000035	90.4	0.2843
100	1.730	638.9	1.7595	0.001044	100.1	0.3119	0.001043	100.2	0.3118	0.001043	100.5	0.3116
110	1.780	644.2	1.7734	0.001052	110.2	0.3380	0.001052	110.3	0.3385	0.001051	110.5	0.3382
120	1.830	649.1	1.7860	0.001061	120.3	0.3647	0.001060	120.4	0.3646	0.001059	120.6	0.3642
130	1.879	653.9	1.7980	0.001070	130.5	0.3902	0.001070	130.6	0.3901	0.001069	130.8	0.3897
140	1.927	658.6	1.8095	0.001080	140.7	0.4152	0.001080	140.7	0.4150	0.001079	141.0	0.4147
150	1.977	663.3	1.8207	0.001091	150.9	0.4397	0.001091	151.0	0.4396	0.001090	151.2	0.4392
160	2.024	667.9	1.8317	0.3917	661.4	1.6425	0.001102	161.3	0.4636	0.001101	161.5	0.4632
170	2.072	672.6	1.8423	0.4026	666.8	1.6553	0.001114	171.7	0.4873	0.001113	171.9	0.4869
180	2.119	677.3	1.8528	0.4131	672.3	1.6671	0.1896	669.9	1.5757	0.001127	182.3	0.5102
190	2.167	682.0	1.8630	0.4234	677.4	1.6782	0.2047	670.5	1.5901	0.001141	192.9	0.5332
200	2.215	686.7	1.8730	0.4337	682.4	1.6890	0.2105	676.4	1.6028	0.001156	208.5	0.5560
210	2.263	691.4	1.8829	0.4438	687.4	1.6994	0.2161	682.0	1.6145	0.001172	214.3	0.5788
220	2.310	696.1	1.8925	0.4538	692.4	1.7096	0.2215	687.4	1.6256	0.001190	223.3	0.6009
230	2.358	700.8	1.9020	0.4638	697.3	1.7195	0.2269	692.7	1.6362	0.08384	676.4	1.5080
240	2.406	705.5	1.9113	0.4738	702.2	1.7291	0.2322	698.0	1.6465	0.08642	682.6	1.5222
250	2.453	710.3	1.9204	0.4837	707.1	1.7386	0.2374	703.1	1.6565	0.08905	689.3	1.5352
260	2.501	715.0	1.9294	0.4935	712.1	1.7479	0.2426	708.3	1.6663	0.09157	695.6	1.5475
270	2.548	719.8	1.9383	0.5034	717.0	1.7571	0.2477	713.5	1.6758	0.09401	701.7	1.5585
280	2.596	724.5	1.9470	0.5132	721.9	1.7660	0.2528	718.5	1.6851	0.09638	707.7	1.5693
290	2.643	729.3	1.9555	0.5230	726.7	1.7747	0.2579	723.6	1.6942	0.09870	713.5	1.5797
300	2.690	734.1	1.9640	0.5327	731.7	1.7835	0.2630	728.7	1.7032	0.1010	719.2	1.5897
310	2.738	738.9	1.9723	0.5424	736.6	1.7920	0.2680	733.8	1.7119	0.1032	724.8	1.5994
320	2.785	743.7	1.9805	0.5522	741.6	1.8004	0.2730	738.8	1.7206	0.1054	730.3	1.6089
330	2.833	748.6	1.9886	0.5619	746.5	1.8086	0.2780	743.9	1.7290	0.1076	735.8	1.6181
340	2.880	753.4	1.9965	0.5715	751.4	1.8167	0.2830	748.9	1.7373	0.1098	741.3	1.6271
350	2.927	758.3	2.0044	0.5812	756.4	1.8247	0.2879	754.0	1.7455	0.1119	746.7	1.6358
360	2.974	763.1	2.0121	0.5908	761.3	1.8326	0.2929	759.1	1.7536	0.1141	752.1	1.6445
370	3.022	768.0	2.0198	0.6005	766.3	1.8404	0.2978	764.1	1.7615	0.1162	757.5	1.6529
380	3.069	772.9	2.0274	0.6101	771.3	1.8481	0.3027	769.2	1.7693	0.1183	762.9	1.6612
390	3.116	777.8	2.0348	0.6197	776.5	1.8557	0.3076	774.3	1.7770	0.1204	768.2	1.6693
400	3.163	782.8	2.0422	0.6293	781.3	1.8631	0.3125	779.3	1.7846	0.1224	773.6	1.6773
410	3.211	787.7	2.0495	0.6389	786.3	1.8705	0.3174	784.4	1.7921	0.1245	778.9	1.6851
420	3.258	792.7	2.0567	0.6488	791.3	1.8778	0.3223	789.5	1.7995	0.1265	784.2	1.6929
430	3.305	797.7	2.0638	0.6580	796.3	1.8850	0.3271	794.6	1.8068	0.1286	789.5	1.7005
440	3.352	802.6	2.0709	0.6676	801.3	1.8921	0.3320	799.7	1.8140	0.1306	794.8	1.7080
450	3.400	807.7	2.0778	0.6771	806.4	1.8992	0.3368	804.8	1.8212	0.1326	800.1	1.7154
460	3.447	812.7	2.0847	0.6867	811.5	1.9061	0.3417	810.0	1.8282	0.1347	805.4	1.7226
470	3.494	817.7	2.0910	0.6962	816.6	1.9130	0.3465	815.1	1.8352	0.1367	810.7	1.7298
480	3.541	822.8	2.0983	0.7057	821.6	1.9198	0.3513	820.2	1.8420	0.1387	816.0	1.7369
490	3.588	827.8	2.1050	0.7153	826.8	1.9266	0.3561	825.4	1.8489	0.1407	821.4	1.7439
500	3.635	832.9	2.1116	0.7248	831.9	1.9332	0.3609	830.6	1.8556	0.1427	826.7	1.7508
510	3.683	838.0	2.1182	0.7343	837.0	1.9398	0.3657	835.8	1.8622	0.1446	832.0	1.7577
520	3.730	843.1	2.1247	0.7438	842.2	1.9464	0.3706	841.0	1.8688	0.1466	837.3	1.7644
530	3.777	848.3	2.1311	0.7533	847.3	1.9528	0.3754	846.2	1.8754	0.1486	842.7	1.7711
540	3.824	853.4	2.1375	0.7628	852.5	1.9592	0.3802	851.4	1.8818	0.1506	848.0	1.7777
550	3.871	858.6	2.1438	0.7723	857.7	1.9656	0.3850	856.6	1.8882	0.1525	853.3	1.7842

Παράρτημα

Συνέχεια πίνακα IV

bar	kJ/kg		kJ/kg	kJ/kg	kJ/kg		p' (v' - v')
	h'	h''			u'	u''	
11.0	780.7	2781.3	2000.6	779.5	2586.1	1807.6	194.0
12.0	797.9	2784.7	1986.7	796.5	2588.7	1792.2	194.6
13.0	814.2	2787.6	1973.4	812.7	2591.0	1778.3	195.1
14.0	829.5	2790.2	1960.7	827.9	2593.1	1765.2	195.5
15.0	844.1	2792.5	1948.4	842.4	2594.8	1752.4	196.0
16.0	858.0	2794.6	1936.6	856.2	2596.5	1740.4	196.2
17.0	871.3	2796.4	1925.1	869.3	2598.0	1728.7	196.4
18.0	884.0	2798.0	1914.0	881.9	2599.3	1717.4	196.6
19.0	896.2	2799.3	1903.2	894.0	2600.2	1706.2	197.0
20.0	908.0	2800.6	1892.6	905.7	2601.3	1695.7	197.0
22.0	930.3	2802.5	1872.2	927.7	2602.9	1675.2	197.0
24.0	951.3	2803.9	1852.7	948.4	2604.0	1655.6	197.0
26.0	971.0	2804.8	1833.8	967.9	2604.8	1636.9	196.9
28.0	989.8	2805.4	1815.6	986.4	2605.4	1619.0	196.6
30.0	1007.7	2805.5	1797.9	1004.1	2605.5	1601.4	196.4
32	1024.7	2805.4	1780.7	1020.8	2605.5	1584.7	196.0
34	1041.1	2805.0	1763.9	1036.9	2605.3	1568.4	195.5
36	1056.9	2804.4	1747.5	1052.4	2604.9	1552.5	195.1
38	1072.1	2803.5	1731.4	1067.4	2604.3	1536.9	194.5
40	1086.7	2802.4	1715.7	1081.7	2603.5	1521.8	193.9
42	1100.9	2801.2	1700.2	1095.6	2602.6	1507.0	193.3
44	1114.7	2799.7	1685.0	1109.1	2601.5	1492.4	192.6
46	1128.1	2798.2	1670.1	1122.3	2600.4	1478.1	191.9
48	1141.1	2796.5	1655.3	1135.0	2599.2	1464.2	191.2
50	1153.8	2794.6	1640.8	1147.4	2597.8	1450.4	190.4
55	1184.2	2789.6	1605.3	1177.0	2594.0	1417.0	188.4
60	1213.1	2783.9	1570.8	1205.2	2589.7	1384.5	186.2
65	1240.5	2777.7	1537.2	1231.8	2585.0	1353.2	184.0
70	1266.7	2771.1	1504.3	1257.2	2580.1	1322.9	181.6
75	1292.0	2764.1	1472.0	1281.5	2574.7	1293.2	178.9
80	1316.4	2756.9	1440.4	1305.7	2569.2	1263.5	177.0
85	1339.9	2749.4	1409.2	1328.0	2563.5	1235.5	174.0
90	1362.9	2741.6	1378.5	1350.2	2557.6	1207.4	171.3
95	1385.2	2733.7	1348.2	1371.6	2551.5	1179.9	168.6
100	1407.0	2725.6	1318.2	1392.5	2545.3	1152.8	165.8
110	1449.3	2708.7	1258.9	1432.9	2532.5	1099.6	159.9
120	1490.2	2687.2	1196.3	1471.9	2519.7	1044.2	153.2
130	1530.2	2663.5	1132.3	1509.8	2507.2	987.4	145.9
140	1569.6	2637.7	1066.7	1547.1	2476.8	929.7	138.3
150	1608.9	2610.5	999.7	1584.0	2455.4	871.4	130.2
160	1648.5	2581.2	929.9	1621.1	2432.2	811.1	121.6
180	1732.9	2511.4	778.5	1699.6	2376.1	676.5	102.0
200	1826.7	2416.0	589.3	1785.5	2297.8	512.3	77.0

Θεωρία και τεχνική του υδρατμού

Συνέχεια πίνακα V

t °C	50 at			75 at			100 at			125 at		
	v	i	ρ	v	i	ρ	v	i	ρ	v	i	ρ
250	0,001250	259,2	0,6663	0,001245	259,2	0,6649	0,001241	259,2	0,6635	0,001237	259,2	0,6622
260	0,001275	270,9	0,6855	0,001270	270,8	0,6870	0,001265	270,8	0,6854	0,001261	270,7	0,6840
270	0,001517	675,0	1,4423	0,001298	282,8	0,7092	0,001292	282,6	0,7075	0,001287	282,5	0,7058
280	0,004331	684,0	1,4588	0,001329	205,2	0,7317	0,001322	294,8	0,7298	0,001316	294,6	0,7279
290	0,004492	692,3	1,4736	0,001370	307,9	0,7547	0,001357	307,5	0,7524	0,001349	307,1	0,7503
300	0,004643	700,0	1,4872	0,02774	673,5	1,4045	0,001398	320,7	0,7755	0,001388	320,1	0,7732
310	0,004787	707,2	1,4997	0,02879	684,0	1,4226	0,01853	652,4	1,3452	0,001434	833,8	0,7969
320	0,004924	714,2	1,5115	0,03062	693,6	1,4388	0,01984	666,3	1,3688	0,001491	348,5	0,8218
330	0,050587	720,8	1,5227	0,03116	702,3	1,4535	0,02101	678,6	1,3893	0,01447	648,1	1,3217
340	0,05186	727,3	1,5333	0,03224	710,6	1,4671	0,02206	689,6	1,4074	0,01561	663,3	1,3467
350	0,05311	733,6	1,5435	0,03326	718,3	1,4796	0,02304	699,6	1,4236	0,01662	676,7	1,3683
360	0,05433	739,5	1,5534	0,03423	725,7	1,4914	0,02394	708,9	1,4384	0,01758	688,7	1,3874
370	0,05543	745,9	1,5629	0,03517	732,8	1,5025	0,02479	717,6	1,4519	0,01838	698,5	1,4045
380	0,05657	751,8	1,5721	0,03607	739,6	1,5131	0,02559	724,7	1,4646	0,01916	709,6	1,4199
390	0,05787	757,7	1,5811	0,03695	744,3	1,5233	0,02636	731,5	1,4764	0,01988	718,9	1,4341
400	0,05902	763,6	1,5898	0,03781	752,9	1,5330	0,02709	741,0	1,4876	0,02057	727,6	1,4472
410	0,06015	769,4	1,5983	0,03865	759,3	1,5425	0,02780	748,2	1,4982	0,02122	735,9	1,4594
420	0,06127	775,1	1,6067	0,03947	765,5	1,5518	0,02849	755,2	1,5084	0,02184	743,9	1,4710
430	0,06237	780,8	1,6149	0,04027	771,8	1,5605	0,02916	763,0	1,5181	0,02244	751,5	1,4819
440	0,06347	786,5	1,6229	0,04105	777,9	1,5691	0,02981	768,7	1,5276	0,02301	758,8	1,4923
450	0,06456	792,2	1,6308	0,04185	783,9	1,5775	0,03045	775,2	1,5367	0,02357	766,0	1,5022
460	0,06564	797,5	1,6385	0,04262	789,9	1,5857	0,03107	781,7	1,5453	0,02412	773,0	1,5116
470	0,06671	803,4	1,6461	0,04338	795,8	1,5938	0,03169	788,0	1,5541	0,02465	779,8	1,5211
480	0,06778	809,1	1,6535	0,04414	801,8	1,6017	0,03229	794,3	1,5625	0,02517	786,5	1,5300
490	0,06883	814,5	1,6609	0,04489	807,6	1,6095	0,03289	800,5	1,5707	0,02568	793,1	1,5387
500	0,06989	820,1	1,6681	0,04563	813,5	1,6172	0,03348	806,6	1,5787	0,02618	799,6	1,5471
510	0,07093	825,7	1,6753	0,04636	819,3	1,6245	0,03406	812,7	1,5865	0,02667	806,0	1,5554
520	0,07198	831,2	1,6823	0,04709	825,1	1,6318	0,03464	818,8	1,5942	0,02714	812,3	1,5634
530	0,07301	836,8	1,6893	0,04782	830,8	1,6390	0,03521	824,8	1,6017	0,02764	818,0	1,5713
540	0,07405	842,3	1,6961	0,04853	836,8	1,6462	0,03578	830,7	1,6091	0,02812	823,8	1,5790
550	0,07507	847,8	1,7029	0,04926	842,3	1,6532	0,03634	836,7	1,6163	0,02858	829,0	1,5865
560	0,07610	853,4	1,7096	0,04999	848,0	1,6601	0,03689	842,6	1,6238	0,02905	834,1	1,5940
570	0,07712	859,1	1,7162	0,05068	853,7	1,6669	0,03745	848,5	1,6308	0,02951	839,2	1,6012
580	0,07814	864,8	1,7227	0,05138	859,4	1,6736	0,03799	854,4	1,6375	0,02996	844,3	1,6084
590	0,07915	870,0	1,7291	0,05208	865,1	1,6803	0,03854	860,2	1,6443	0,03042	849,5	1,6154
600	0,08016	875,5	1,7355	0,05278	870,8	1,6868	0,03908	866,1	1,6510	0,03086	854,7	1,6224
610	0,08117	881,0	1,7418	0,05348	876,5	1,6933	0,03962	871,9	1,6577	0,03131	860,0	1,6292
620	0,08218	886,6	1,7481	0,05417	882,2	1,6997	0,04015	877,8	1,6642	0,03175	865,3	1,6359
630	0,08318	892,1	1,7542	0,05486	887,9	1,7060	0,04069	883,6	1,6707	0,03219	870,9	1,6425
640	0,08418	897,7	1,7604	0,05554	893,6	1,7123	0,04122	889,4	1,6771	0,03263	876,2	1,6491
650	0,08518	903,2	1,7664	0,05623	899,3	1,7185	0,04175	895,2	1,6834	0,03304	881,2	1,6555
660	0,08617	908,8	1,7724	0,05691	905,0	1,7246	0,04227	901,0	1,6897	0,03340	886,7	1,6619
670	0,08717	914,4	1,7784	0,05759	910,6	1,7306	0,04280	906,8	1,6959	0,03378	892,0	1,6682
680	0,08816	920,0	1,7842	0,05827	916,3	1,7367	0,04332	912,6	1,7020	0,03415	897,4	1,6745
690	0,08915	925,6	1,7901	0,05895	922,0	1,7426	0,04384	918,4	1,7080	0,03457	903,1	1,6806
700	0,09014	931,2	1,7959	0,05962	927,7	1,7485	0,04435	924,2	1,7140	0,03498	909,0	1,6867
710	0,09112	936,8	1,8016	0,06030	933,4	1,7543	0,04487	930,0	1,7200	0,03540	915,0	1,6927
720	0,09211	942,4	1,8073	0,06097	939,1	1,7600	0,04539	935,8	1,7258	0,03582	921,0	1,6987
730	0,09309	948,0	1,8129	0,06164	944,8	1,7658	0,04590	941,6	1,7316	0,03624	927,0	1,7046
740	0,09408	953,6	1,8185	0,06231	950,5	1,7715	0,04641	947,4	1,7374	0,03666	933,0	1,7104
750	0,09506	959,3	1,8241	0,06297	956,3	1,7771	0,04692	953,2	1,7431	0,03708	939,0	1,7162
760	0,09604	965,0	1,8296	0,06364	962,0	1,7827	0,04743	959,0	1,7487	0,03751	945,0	1,7219
770	0,09702	970,7	1,8350	0,06431	967,7	1,7882	0,04794	964,8	1,7543	0,03794	951,0	1,7276
780	0,09799	976,3	1,8405	0,06498	973,5	1,7937	0,04845	970,6	1,7599	0,03837	957,0	1,7332
790	0,09897	982,0	1,8458	0,06563	979,4	1,7992	0,04895	976,5	1,7654	0,03880	963,0	1,7388
800	0,09994	987,7	1,8512	0,06629	985,0	1,8046	0,04945	982,3	1,7709	0,03926	969,0	1,7443

Παράρτημα

Συνέχεια πίνακα V

t °C	1,0 at			5,0 at			10,0 at			25 at		
	v	i	ρ	v	i	ρ	v	i	ρ	v	i	ρ
550	3,871	858,6	2,1438	0,7723	857,7	1,9656	0,3850	856,6	1,8882	0,1525	853,3	1,7842
560	3,918	863,8	2,1500	0,7918	862,9	1,9719	0,3897	861,9	1,8945	0,1545	858,7	1,7907
570	3,965	869,0	2,1562	0,7913	868,1	1,9781	0,3945	867,1	1,9008	0,1565	864,0	1,7971
580	4,013	874,2	2,1624	0,8008	873,4	1,9843	0,3993	872,4	1,9070	0,1584	869,4	1,8034
590	4,060	879,4	2,1685	0,8103	878,6	1,9904	0,4041	877,7	1,9132	0,1604	874,3	1,8097
600	4,107	884,7	2,1745	0,8198	883,9	1,9965	0,4089	883,0	1,9193	0,1623	880,2	1,8159
610	4,154	889,9	2,1805	0,8292	889,2	2,0025	0,4136	888,3	1,9253	0,1643	885,6	1,8221
620	4,201	895,2	2,1865	0,8387	894,5	2,0085	0,4184	893,6	1,9313	0,1662	891,0	1,8281
630	4,248	900,5	2,1924	0,8482	899,8	2,0144	0,4232	898,9	1,9373	0,1682	896,4	1,8342
640	4,295	905,8	2,1982	0,8577	905,1	2,0203	0,4279	904,3	1,9434	0,1701	901,8	1,8402
650	4,342	911,1	2,2040	0,8672	910,5	2,0261	0,4327	909,7	1,9491	0,1721	907,3	1,8461
660	4,390	916,5	2,2098	0,8766	915,9	2,0319	0,4375	915,1	1,9549	0,1740	912,7	1,8520
670	4,437	921,9	2,2155	0,8861	921,2	2,0376	0,4422	920,5	1,9606	0,1759	918,2	1,8578
680	4,484	927,2	2,2212	0,8955	926,6	2,0433	0,4470	925,9	1,9663	0,1779	923,7	1,8636
690	4,531	932,6	2,2268	0,9050	932,1	2,0490	0,4517	931,3	1,9720	0,1798	929,2	1,8693
700	4,578	938,0	2,2324	0,9144	937,5	2,0546	0,4565	936,8	1,9776	0,1817	934,7	1,8750
710	4,625	943,5	2,2380	0,9239	942,9	2,0603	0,4612	942,2	1,9832	0,1836	940,2	1,8806
720	4,672	948,9	2,2435	0,9333	948,4	2,0657	0,4660	947,7	1,9888	0,1856	945,7	1,8862
730	4,719	954,4	2,2490	0,9428	953,9	2,0712	0,4707	953,2	1,9943	0,1875	951,3	1,8918
740	4,766	959,9	2,2544	0,9523	959,4	2,0766	0,4755	958,7	1,9997	0,1894	956,8	1,8973
750	4,814	965,4	2,2598	0,9617	964,9	2,0820	0,4802	964,2	2,0052	0,1913	962,4	1,9028
760	4,861	970,9	2,2652	0,9712	970,4	2,0874	0,4850	969,7	2,0106	0,1933	968,0	1,9082
770	4,908	976,4	2,2705	0,9806	975,9	2,0927	0,4897	975,3	2,0159	0,1952	973,6	1,9136
780	4,955	982,0	2,2758	0,9901	981,5	2,0980	0,4945	980,9	2,0212	0,1971	979,2	1,9190
790	5,002	987,5	2,2810	0,9995	987,1	2,1033	0,4992	986,5	2,0265	0,1990	984,8	1,9243
800	5,049	993,1	2,2863	1,0090	992,6	2,1085	0,5039	992,1	2,0317	0,2009	99	

Θεωρία και τεχνική του υδρατμού

Συχνότητα πίνακα V

Table with columns for temperature (t, °C) and saturation pressure (p) at 150 at, 200 at, 250 at, and 300 at. It lists values for temperature, pressure, and specific volume (v) for various temperatures.

Table with columns for temperature (t, °C) and saturation pressure (p) at 350 at, 400 at, 450 at, and 500 at. It lists values for temperature, pressure, and specific volume (v) for various temperatures.

Παράρτημα

Συχνότητα πίνακα V

Table with columns for temperature (t, °C) and saturation pressure (p) at 150 at, 200 at, 250 at, and 300 at. It lists values for temperature, pressure, and specific volume (v) for various temperatures.

Θεωρία και Τεχν. του υδρατμού

Πίνακας VI Καταστατικά μεγέθη νερού και υπερθέρμνου ατμού σε μονάδες του Δ.Ι.Μ.

Table with 12 columns: t (°C), 1.0 bar ts = 99,63 °C, 5.0 bar ts = 151,85 °C, 10.0 bar ts = 179,88 °C, 25 bar ts = 223,94 °C. Rows include properties like v, h, s, v, h, s, v, h, s for various temperatures from 0 to 800 °C.

Παράρτημα

Συνοψισιο πίνακα V

Table with 12 columns: t (°C), 350 at, 400 at, 450 at, 500 at. Rows include properties like v, i, s, v, i, s, v, i, s, v, i, s for various temperatures from 250 to 800 °C.

Θεωρία και Ισχυική του υδραπίου

Συνέχεια πίνακα VI

Table with 12 columns: t °C, 50 bar, 75 bar, 100 bar, 125 bar. Each bar section has sub-columns for v, h, s, and ρ. Data rows range from 250 to 800 °C.

Παράρτημα

Συνέχεια πίνακα VI

Table with 12 columns: t °C, 1.0 bar, 5.0 bar, 10.0 bar, 151.85 °C, 179.88 °C, 223.94 °C. Each bar section has sub-columns for v, h, s, and ρ. Data rows range from 550 to 800 °C.

Table with 12 columns: t °C, 50 bar, 75 bar, 100 bar, 125 bar. Each bar section has sub-columns for v, h, s, and ρ. Data rows range from 0 to 240 °C.

Συνέχεια πίνακα VI

Table with 16 columns: t, °C, 150 bar, 200 bar, 250 bar, 300 bar. Rows include values for v, h, s, and f for various temperatures and pressures.

Table with 16 columns: t, °C, 350 bar, 400 bar, 450 bar, 500 bar. Rows include values for v, h, s, and f for various temperatures and pressures.

Συνέχεια πίνακα VI

Table with 16 columns: t, °C, 150 bar, 200 bar, 250 bar, 300 bar. Rows include values for v, h, s, and f for various temperatures and pressures.

350 bar

400 bar

450 bar

500 bar

Θεωρία και τεχνική του υδρατμού

Πίνακας VII

Μοριακή μάζα, σταθερά R, πυκνότητα και ειδική θερμοχωρητικότητα αερίων.

Αέριο	Μορ.	Μάζα κ	R	ρ ₀	h ₀	ρ ₀	ρ ₀	ρ ₀	ρ ₀	ρ ₀	ρ ₀	ρ ₀	ρ ₀	ρ ₀
Ηλιο	H ₂	2	2078,0	0,1789	1,271	0,0755	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,319
Αργό	Ar	1	40	0,129	0,129	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Ψευδάργυρο	Zn	2	287,0	0,240	0,240	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Νιτρικό	N ₂	2	28	0,240	0,240	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Άζωτο	N ₂	2	28	0,240	0,240	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Μονοξείδιο του άνθρακα	CO	2	28	0,240	0,240	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Διοξείδιο του άνθρακα	CO ₂	3	44	0,1957	0,1957	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Αμμωνία	NH ₃	4	17	0,491	0,491	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Αεθυλίλη	C ₂ H ₂	4	26	0,3613	0,3613	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319
Μεθάνιο	CH ₄	5	16	0,515	0,515	1,301	1,400	1,402	1,402	1,402	1,402	1,402	1,402	1,319

:: Κατά προέγγραφο για την πράξη.

Παράρτημα

Συνοχέια πίνακα VI

t °C	350 bar			400 bar			450 bar			500 bar		
	ρ	h	s	ρ	h	s	ρ	h	s	ρ	h	s
250	0,0012047	1088,9	2,7263	0,0011987	1090,1	2,7172	0,0011929	1091,5	2,7084	0,0011875	1093,0	2,6999
260	0,0012240	1154,8	2,8133	0,0012172	1135,7	2,8035	0,0012108	1136,7	2,7940	0,0012047	1137,9	2,7849
270	0,0012448	1218,4	2,8999	0,0012363	1181,9	2,8791	0,0012301	1182,3	2,8703	0,0012234	1183,3	2,8603
280	0,0012675	1281,8	2,9864	0,0012589	1228,8	2,9749	0,0012509	1228,9	2,9658	0,0012434	1229,3	2,9553
290	0,0012922	1277,1	3,0729	0,0012824	1276,5	3,0603	0,0012734	1276,1	3,0483	0,0012649	1276,0	3,0369
300	0,0013184	1326,4	3,1596	0,0013082	1325,0	3,1458	0,0012978	1324,0	3,1327	0,0012883	1323,4	3,1202
310	0,0013465	1376,8	3,2469	0,0013364	1374,6	3,2315	0,0013245	1372,8	3,2171	0,0013136	1371,5	3,2035
320	0,0013832	1428,7	3,3350	0,0013678	1425,3	3,3178	0,0013539	1422,7	3,3018	0,0013414	1420,5	3,2868
330	0,0014214	1482,1	3,4244	0,0014029	1477,4	3,4049	0,0013866	1473,6	3,3870	0,0013279	1470,5	3,3704
340	0,0014633	1537,6	3,5155	0,0014427	1531,1	3,4932	0,0014231	1525,9	3,4729	0,0014059	1521,5	3,4543
350	0,0015165	1595,5	3,6092	0,0014882	1586,7	3,5831	0,0014645	1579,6	3,5599	0,0014439	1573,8	3,5388
360	0,001570	1656,7	3,7053	0,001540	1644,9	3,6760	0,001510	1636,2	3,6488	0,001490	1627,8	3,6247
370	0,001625	1722,9	3,8039	0,001600	1706,5	3,7723	0,001570	1694,8	3,7409	0,00154	1684,3	3,7158
380	0,001675	1804,9	3,9241	0,001668	1773,1	3,8759	0,001630	1757,2	3,8382	0,00160	1743,4	3,8058
390	0,00169	1882,4	4,0528	0,001678	1845,9	3,9869	0,001670	1822,9	3,9487	0,00166	1804,5	3,9000
400	0,00212	1987,9	4,1920	0,00191	1928,0	4,1114	0,00180	1895,4	4,0465	0,00174	1870,2	3,9973
410	0,00257	2120,2	4,4087	0,00209	2021,4	4,2486	0,00192	1973,7	4,1637	0,00183	1940,6	4,1041
420	0,00323	2322,8	4,6431	0,00237	2131,1	4,4077	0,00207	2060,3	4,3004	0,00194	2017,2	4,2140
430	0,00373	2442,6	4,8755	0,00274	2259,2	4,5940	0,00228	2157,5	4,4286	0,00208	2098,4	4,3312
440	0,00437	2569,4	5,0545	0,00322	2388,2	4,7771	0,00255	2263,4	4,5803	0,00226	2186,3	4,4548
450	0,00495	2670,8	4,1948	0,00372	2504,5	4,9404	0,00288	2372,5	4,7321	0,00248	2280,5	4,5866
460	0,00540	2754,9	5,3166	0,00419	2610,5	5,0849	0,00324	2479,0	4,8787	0,00272	2377,7	4,7206
470	0,00582	2827,3	5,4072	0,00462	2703,3	5,2084	0,00360	2578,7	5,0126	0,00300	2474,4	4,8493
480	0,00620	2890,3	5,4918	0,00489	2786,0	5,2621	0,00386	2663,6	5,1309	0,00330	2563,6	4,9718
490	0,00655	2948,6	5,5683	0,00525	2849,2	5,3397	0,00429	2748,6	5,2385	0,00360	2651,5	5,0857
500	0,00689	3002,3	5,6382	0,00557	2911,0	5,4801	0,00459	2819,4	5,3298	0,00386	2731,1	5,1895
510	0,00720	3052,3	5,7026	0,00587	2968,1	5,5536	0,00488	2884,3	5,4124	0,00415	2802,6	5,2817
520	0,00749	3099,3	5,7622	0,00615	3021,3	5,6210	0,00514	2943,3	5,4872	0,00438	2867,9	5,3634
530	0,00778	3143,7	5,8178	0,00642	3071,2	5,6835	0,00539	2998,3	5,566	0,00462	2928,9	5,4428
540	0,00804	3185,9	5,8701	0,00668	3118,2	5,7417	0,00563	3050,0	5,6202	0,00484	2984,4	5,5115
550	0,00830	3226,2	5,9193	0,00692	3162,8	5,7963	0,00586	3098,8	5,6798	0,00505	3030,7	5,5756
560	0,00855	3264,9	5,9661	0,00716	3205,4	5,8476	0,00608	3145,1	5,7357	0,00525	3083,2	5,6311
570	0,00879	3302,3	6,0106	0,00738	3246,1	5,8963	0,00630	3189,3	5,7884	0,00545	3133,4	5,6874
580	0,00902	3338,4	6,0532	0,00760	3285,3	5,9423	0,00653	3231,6	5,8383	0,00564	3178,5	5,7406
590	0,00925	3373,4	6,0940	0,00781	3323,2	5,9866	0,00670	3272,3	5,8857	0,00583	3221,7	5,7910
600	0,00947	3407,6	6,1334	0,00802	3359,9	6,0289	0,00689	3311,5	5,9302	0,00601	3263,4	5,8390
610	0,00968	3440,9	6,1713	0,00822	3395,6	6,0695	0,00708	3349,0	5,9742	0,00618	3303,7	5,8848
620	0,00989	3473,6	6,2081	0,00841	3430,3	6,1087	0,00726	3386,5	6,0156	0,00636	3342,7	5,9287
630	0,01009	3505,6	6,2437	0,00860	3464,3	6,1465	0,00744	3422,5	6,0559	0,00652	3380,6	5,9709
640	0,01029	3537,0	6,2784	0,00879	3497,6	6,1831	0,00762	3457,6	6,0946	0,00668	3417,5	6,0116
650	0,01049	3568,0	6,3121	0,00897	3530,2	6,2187	0,00778	3491,9	6,1320	0,00684	3453,5	6,0508
660	0,01068	3598,6	6,3450	0,00914	3562,3	6,2532	0,00795	3525,6	6,1682	0,00700	3489,8	6,0888
670	0,01087	3628,7	6,3772	0,00932	3593,9	6,2869	0,00811	3558,7	6,2036	0,00715	3525,3	6,1256
680	0,01106	3658,0	6,4094	0,00949	3625,0	6,3197	0,00827	3591,2	6,2378	0,00730	3557,2	6,1614
690	0,01124	3688,0	6,4399	0,00966	3655,7	6,3518	0,00843	3623,2	6,2712	0,00745	3590,5	6,1962
700	0,01143	3717,2	6,4695	0,00983	3686,1	6,3832	0,00858	3654,8	6,3038	0,00759	3623,3	6,2300
710	0,01161	3746,1	6,4981	0,00999	3716,1	6,4139	0,00873	3686,0	6,3357	0,00773	3655,7	6,2631
720	0,01178	3775,0	6,5268	0,01015	3745,9	6,4440	0,00888	3716,8	6,3669	0,00787	3687,9	6,2954
730	0,01196	3803,3	6,5557	0,01031	3775,4	6,4735	0,00903	3747,5	6,3974	0,00801	3719,1	6,3270
740	0,01213	3831,6	6,5848	0,01047	3804,6	6,5025	0,00918	3777,4	6,4274	0,00814	3750,2	6,3579
750	0,01231	3859,7	6,6124	0,01063	3833,6	6,5310	0,00932	3807,3	6,4567	0,00828	3781,1	6,3882
760	0,01248	3887,7	6,6396	0,01078	3862,4	6,5590	0,00946	3837,0	6,4856	0,00841	3811,6	6,4179
770	0,01264	3915,5	6,6664	0,01093	3891,0	6,5865	0,00960	3866,4	6,5139	0,00854	3841,9	6,4470
780	0,01281	3943,2	6,6928	0,01108	3919,4	6,6137	0,00974	3895,6	6,5418	0,00867	3871,9	6,4756
790	0,01298	3970,8	6,7189	0,01123	3947,7	6,6404	0,00988	3924,7	6,5692	0,00879	3901,7	6,5038
800	0,01314	3998,2	6,7446	0,01138	3975,8	6,6667	0,01001	3953,5	6,5962	0,00892	3931,2	6,5315

Παράρτημα

Πίνακας VIII

Μέση ειδική θερμοχωρητικότητα υπό σταθερή πίεση σε κJ/kg K*

Table with columns for temperature (T), and specific heat capacity (Cp) for various gases: H2, O2, CO, H2O, CO2, SO2. The table lists values for temperatures from 0 to 3000 K.

* Κατά Baehr-Hartmann-Pohl-Schomächer: Thermodynamische Funktionen idealer Gase für Temperaturen bis 6000K. Springer, Berlin-Heidelberg, New York, 1967. Οι τιμές του αέρα προέρχουν από υπολογισμούς.

Θεωρία και τεχνική υδρατμού

Πίνακας IX

Ενθαλπία Η (MJ/kmol) αερίων σε κατάσταση τελείου αερίου κατά Gurnis, Temad. Sv. Instn. Vesc., Μόσχα. Το μηδενικό σημείο h0=0 εκλέχθηκε για τα H2, O2, N2. Το OK. Για τα υπόλοιπα καθορίστηκε από τις θετικές (ή αρνητικές) θερμοπτώξες αντίδρασης.

Large table showing enthalpy values for various gases (H2, O2, CO, NO, CO2, N2, OH, H2O) at different temperatures (T [K]). The table includes columns for each gas and a final column for NH3.

Μέγες ποσότητες βερνικιών και στεγερών (p → 0, t = 0 °C)

Η =	2,016	2,016	28,02	28,16	32,00	17,01	20,01	20,01	18,02	34,02	44,09	44,01	44,02	64,06	17,03	28,03	28,964	16,04	28,05	26,04
t	6,84	6,96	6,96	6,96	6,96	7,16	7,16	6,96	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
H ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
N ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
από αέρια	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
O ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
OH	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
CO	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
NO	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
H ₂ O	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
H ₂ S	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
CO ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
N ₂ O	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
SO ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
NH ₃	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
Αέρας	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
CH ₄	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
C ₂ H ₄	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
C ₂ H ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13

Θεωρία και τεχνική υδατίου

956

Αντίθετες ποσότητες βερνικιών και στεγερών (p → 0, t = 0 °C)

Η =	2,016	2,016	28,02	28,16	32,00	17,01	20,01	20,01	18,02	34,02	44,09	44,01	44,02	64,06	17,03	28,03	28,964	16,04	28,05	26,04
t	6,84	6,96	6,96	6,96	6,96	7,16	7,16	6,96	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
H ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
N ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
από αέρια	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
O ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
OH	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
CO	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
NO	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
H ₂ O	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
CO ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
N ₂ O	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
SO ₂	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13
Αέρας	7,02	7,02	7,02	7,02	7,02	7,16	7,16	7,02	7,16	8,00	8,10	8,10	8,10	9,29	8,36	8,36	6,95	8,27	10,02	10,13

Παράρτημα

956

Πίνακας XIα,β. Διαφορά εσωτερικής ενέργειας $\Delta U_M = U_{Mt} - U_{Mo}$ (αριστερά)

και ενθαλπίας $\Delta I_M = I_{Mt} - I_{Mo}$ (δεξιά) σε kcal/kmol.

t °C	H ₂	N ₂ καθα- ρό	O ₂	CO	H ₂ O	CO ₂	SO ₂	Αέρας	N ₂ από αέρα
0	0	0	0	0	0	0	0	0	0
25	122	124	125	124	150	169	184	124	123
100	493	498	506	498	607	715	775	498	495
200	993	1001	1034	1004	1233	1522	1634	1005	997
300	1493	1512	1583	1521	1880	2405	2558	1522	1505
400	1996	2035	2156	2054	2556	3451	3531	2053	2026
500	2502	2574	2751	2604	3261	4348	4551	2601	2562
600	3013	3132	3363	3173	3996	5388	5606	3160	3116
700	3530	3703	3988	3757	4760	6464	6677	3750	3686
800	4055	4292	4624	4354	5555	7572	7785	4345	4270
900	4689	4991	5270	4963	6480	8806	8894	5051	4965
1000	5133	5502	5926	5584	7235	9862	10016	5569	5472
1100	5686	6121	6589	6213	8117	11035	11145	6194	6088
1200	6241	6738	7249	6840	9014	12215	12281	6818	6701
1300	6829	7394	7936	7495	9956	13421	13420	7468	7343
1400	7416	8026	8618	8145	10910	14639	14580	8115	7981
1500	8011	8675	9306	8800	11885	15869	15740	8769	8626
1600	8614	9329	10000	9460	12878	17109	16910	9428	9277
1700	9225	9989	10705	10126	13839	18358	18090	10093	9933
1800	9845	10652	11409	10794	14915	19612	19270	10762	10591
1900	10472	11318	12118	11466	15956	20872	20460	11434	11352
2000	11108	11988	12837	12142	17013	22139	21660	12111	11917
2100	11751	12660	13559	12820	18084	23412	—	12790	12584
2200	12401	13335	14278	13500	19169	24692	—	13473	13253
2300	13057	14012	15018	14183	20260	25977	—	14158	13934
2400	13719	14693	15756	14869	21381	27268	—	14847	14603
2500	14385	15375	16497	15556	22506	28563	—	15537	15283

H ₂	N ₂ καθα- ρό	O ₂	CO	H ₂ O	CO ₂	SO ₂	Αέρας	N ₂ από αέρα
0	0	0	0	0	0	0	0	0
172	174	175	174	200	219	234	174	174
692	697	705	697	806	916	974	697	694
1390	1398	1431	1401	1630	1919	2031	1402	1394
2099	2108	2179	2117	2476	3001	3154	2116	2101
2791	2830	2951	2849	3351	4146	4325	2848	2821
3496	3568	3745	3593	4255	5342	5544	3595	3556
4205	4324	4555	4365	5138	6580	6798	4360	4308
4921	5096	5379	5146	6151	7855	8067	5141	5077
5645	5862	6214	5914	7145	9162	9374	5935	5860
6378	6630	7053	6752	8169	10495	10680	6740	6654
7120	7489	7913	7571	9222	11849	12000	7556	7459
7872	8307	8775	8399	10303	13221	13330	8380	8273
8636	9133	9644	9235	11409	14510	14660	9213	9096
9412	9967	10519	10078	12539	16004	16000	10051	9926
10193	10908	11400	10927	13692	17421	17360	10897	10763
10992	11556	12267	11731	14866	18850	18720	11750	11607
11794	12509	13130	12640	16058	20289	20090	12608	12457
12604	13367	14083	13504	17267	21736	21470	13471	13311
13422	14229	14926	14371	18492	23189	22840	14339	14168
14248	15094	15894	15242	19732	24640	24230	15210	15129
15082	15962	16811	16115	20987	26113	25460	16085	15991
15924	16833	17732	16993	22257	27585	—	16963	16757
16773	17707	18650	17672	23541	29064	—	17845	17625
17628	18583	19589	18754	24839	30548	—	18729	18505
18488	19462	20525	19638	26150	32037	—	19616	19377
19355	20373	21455	20524	27474	33531	—	20505	20251

Πίνακας XIγ Διαφορά εντροπίας $\Delta S_{Mu} = S_{Mut} - S_{Mu0}$ σε kcal/kmol grd.

t °C	H ₂	N ₂ καθα- ρό	O ₂	CO	H ₂ O	CO ₂	SO ₂	Αέρας	N ₂ από αέρα
0	0	0	0	0	0	0	0	0	0
100	1,48	1,56	1,59	1,56	1,88	2,17	2,47	1,56	1,55
200	2,66	2,73	2,84	2,77	3,37	4,06	4,53	2,74	2,72
300	3,63	3,70	3,90	3,71	4,58	5,73	6,35	3,69	3,68
400	4,39	4,53	4,83	4,56	5,64	7,26	7,96	4,55	4,50
500	5,13	5,27	5,64	5,33	6,00	8,62	9,40	5,31	5,24
600	5,75	5,94	6,38	6,04	7,51	9,87	10,69	6,02	5,91
700	6,32	6,57	7,07	6,65	8,37	11,03	11,88	6,68	6,53
800	6,82	7,13	7,69	7,28	9,15	12,19	12,96	7,28	7,09
900	7,29	7,66	8,27	7,83	9,90	13,21	13,96	7,82	7,61
1000	7,73	8,17	8,81	8,32	10,62	14,14	14,88	8,32	8,12
1100	8,14	8,65	9,21	8,82	11,29	15,04	15,75	8,80	8,59
1200	8,53	9,11	9,79	9,26	11,93	15,87	16,55	9,25	9,05
1300	8,90	9,52	10,23	9,68	12,55	16,71	17,30	9,67	9,45
1400	9,35	9,92	10,64	10,08	13,14	17,46	18,04	10,07	9,84
1500	9,68	10,30	11,03	10,46	13,69	18,16	18,69	10,44	10,22
1600	10,00	10,66	11,41	10,83	14,23	18,83	19,35	10,79	10,57
1700	10,31	11,00	11,78	11,09	14,75	19,47	19,94	11,13	10,91
1800	10,61	11,32	12,13	11,43	15,21	20,02	20,53	11,44	11,22
1900	10,90	11,63	12,47	11,76	15,69	20,58	21,06	11,75	11,53
2000	11,18	11,93	12,79	12,07	16,16	21,15	21,58	12,05	11,81
2100	11,45	12,22	13,10	12,36	16,61	21,70	22,09	12,34	12,10
2200	11,72	12,49	13,42	12,65	17,06	22,22	22,57	12,63	12,37
2300	11,99	12,76	13,71	12,93	17,50	22,75	23,04	12,90	12,63
2400	12,24	13,03	13,99	13,20	17,92	23,25	23,43	13,16	12,89
2500	12,48	13,27	14,24	13,45	18,31	23,73	23,91	13,41	13,13

Πίνακας XII

Θερμότητα δόνηση H₀ και H_u, μέγιστο αντισταθρέτο έργο - (L_t)_{max} και εξέργεια E_B ενταίων καυσίμων σε kcal/kmol.

Καύσιμα	H ₀	H _u	-L _{trev}	E _B
Στερεά				
C	393,5	393,5	394,4	410,5
S	296,6	296,6	299,8	-
Αέρια				
H ₂	285,9	241,8	237,3	235,3
CO	283,0	283,0	257,3	275,4
CH ₄	890,5	802,3	818,1	830,3
C ₂ H ₂	1300	1256	1235	1265
C ₂ H ₄	1411	1323	1332	1360
C ₂ H ₆	1560	1428	1468	1494
C ₃ H ₆	2059	1926	1970	2012
C ₃ H ₈	2220	2044	2109	2149
n-C ₄ H ₁₀	2879	2658	2748	2803
Υγρά				
n-C ₅ H ₁₂	3510	3245	3386	3455
C ₆ H ₆	3268	3135	3202	3293
C ₆ H ₁₂	3920	3656	3817	3902
n-C ₆ H ₁₄	4164	3855	4023	4106
C ₇ H ₈	3906	3730	3820	3925
n-C ₇ H ₁₆	4817	4465	4660	4757
n-C ₈ H ₁₈	5471	5074	5297	5408
n-C ₈ H ₂₀	6125	5684	5934	6059
n-C ₁₀ H ₂₂	6779	6294	6571	6711
CH ₃ OH	726,6	638,4	702,5	716,7
C ₂ H ₅ OH	1367,1	1234,8	1325,8	1354,1

Παράρτημα






















Θεωρία και τεχνική

υδραυλικός

957

957

1.3.1. Σωληνώσεις


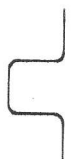

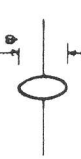

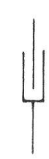
1.1	Ατμός		s = 1,2 mm
1.2	Συμπύκνωμα και νερό		s = 0,5 mm
1.3	Ατμός που περιέχει λάδι		s = 1,2 mm
1.4	Συμπύκνωμα που περιέχει λάδι		s = 0,5 mm d = 2,0 mm
1.5	Νερό ακατέργαστο		s = 0,5/0,3 mm
1.6	Διαλύματα		s = 0,5/0,3 mm
1.7	Στρατσόνα ή ακάθαρτο νερό		s = 0,3 mm
1.8	Γραμμή εντολών		s = 0,3 mm
1.9	Γραμμές επενέργειας αυτοματίων συστημάτων		s = 0,3 mm
1.10	Καύσιμο αέριο		s = 0,4/0,2 mm
1.11	Καπναέρια		s = 0,2/0,4/0,2 mm b = 0,1 mm
1.12	Αέρας		s = 0,4/0,2 mm b = 0,4 mm
1.13	Γαϊάνθρακας		s = 0,2/1,0/0,2 b = 1,0 mm
1.14	Τέφρα κ.λπ.		s = 0,2/0,8/0,2 b = 0,8 mm
1.15	Επεκτάσεις μελλοντικές κ.λπ.		Διακεκομμένες γραμμές
1.16	Διασταυρώσεις με ένωση των σωλήνων		κ.λπ.
1.17	Διασταυρώσεις στον χώρο χωρίς ένωση των σωλήνων		κ.λπ.
1.18	Διακλάδωση		κ.λπ.
1.19	Κινητή γραμμή		
1.20	Γραμμή με μανδύα		
1.21	Γραμμή με παράλληλη γραμμή		






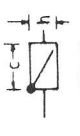


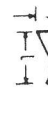





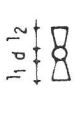



21 Τεχνική του υδραμιού

ΠΤΕΙΝΟΜΕΝΟΙ ΣΥΜΒΟΛΙΣΜΟΙ

Λειτουργούν κατανοητά σε ένα σχέδιο συνδεσμολογίας ή θερμικού δικτύου ενδιάφορα μηχανήματα και όργανα αποφασισίτικα να σημειώνονται με ειδικά Σημεία επόμενα δίδονται οι συμβολισμοί κατά την γερμανική τυποποίηση και σύμφωνα με τα φυλλάδια DIN 2429, 2430, 3400, 2425, 2481, τις προτιροπές του VDI 2261 και τις VGB.

1.3.4. Εξομοιωτές μικρών (διαστολικά)

4.1	Διαστολικό εν γένει		$d = 8 \text{ mm}$
4.2	Διαστολικό ου		$l_1 = l_2 = l_3 = 6 \text{ mm}$
4.3	Διαστολικό ωμέγα (λύρα)		
4.4	Διαστολικό φακοειδές		$\varphi = 6 \text{ mm}$
4.5	Σπαστός σωλήνας		$l = 12, h = 5 \text{ mm}$
4.6	Διαστολικό με στυπιοθλίπτη		

17	Δικλείδα αντεπιστροφής		
18	Δικλείδα αντεπιστροφής με φλαντζες		
19	Απλή βαλβίδα αντεπιστροφής τοποθετούμενη μεταξύ φλαντζών		$l = h = 5 \text{ mm}$
20	Ομοίως με ελατήριο		$l = h = 5 \text{ mm}$
21	Κλαπέττο εν γένει		$l = 7, h = 4 \text{ mm}$
22	Κλαπέττο αντεπιστροφής εν γένει		$l = 7, h = 4 \text{ mm}$
23	Κλαπέττο αποφρακτικό		
24	Κλαπέττο ρυθμιστικό		
25	Σύρτης (βάννα)		
26	Μειωτής πίεσεως		$l = 9, h = 5 \text{ mm}$ $p_1 > p_2$
27	Όργανο αντεπιστροφής εν γένει με δυνατότητα αποφράξεως της ροής		
3.28	Ποτήρι αναρροφήσεως		$l = h = 4 \text{ mm}$
3.29	Γωνιακή δικλείδα		$l_1 = l_2 = 3 \text{ mm}$
3.30	Γωνιακό ασφαλιστικό με αντίβαρο		
3.31	Γωνιακή δικλείδα αντεπιστροφής με δυνατότητα αποφράξεως της ροής		
3.32	Κρουνός		$l_1 = l_2 = 3, d = 2 \text{ mm}$
3.33	Κρουνός γωνιακός		
3.34	Τρίστομος κρουνός		

5.1	Ατμοπαγίδα εν γένει		$d = 4 \text{ mm}$
5.2	Ατμοπαγίδα με φλάντζες		
5.3	Συλλεκτήριος αγωγός συμπυκνωμάτων με ατμοπαγίδα		$d_1 = 7 \text{ mm}$ $d_2 = 4 \text{ mm}$
5.4	Ροοδείκτης		$a_1 = a_2 = 6 \text{ mm}$
5.5	Φίλτρο		
5.6	Κόσκινο (απλό συρμάτινο φίλτρο)		$l = 10, h = 5 \text{ mm}$
5.7	Εκροή προς αποχέτευση		
5.8	Κάλυμμα έναντι βροχής		
5.9	Ρυθμιστής ταχύτητας		
5.10	Ρυθμιστής πίεσεως		
5.11	Ρυθμιστής θερμοκρασίας (θερμοστάτης)		
5.12	Ρυθμιστής στάθμης		$l = 12 \text{ mm}$ $h = 5 \text{ mm}$
5.13	Ρυθμιστής ποσότητας		
5.14	Ρυθμιστής ασφαλείας (ρυθμιστής ταχείας διακοπής)		$d_1 = 6, d_2 = 3 \text{ mm}$
5.15	Μετρητής πίεσεως (μανόμετρο)		$d = 5 \text{ mm}$
5.16	Πιεσόμετρο υγρό		
5.17	Διαφορικό μανόμετρο		

5.18	Διαφορικό υγρό πιεσόμετρο		
5.19	Μετρητής θερμοκρασίας		
5.20	Υγρό θερμομέτρο		
5.21	Θερμοληκτρικό στοιχείο		
5.22	Θερμόμετρο αντιτάσεως		
5.23	Θερμόμετρο διμεταλλικό		
5.24	Θερμόμετρο ακτινοβολίας (οπτικό)		
5.25	Μετρητικό ακροφύσιο ή φλάντζα χωρίς τοπικό όργανο ενδείξεως		
5.26	Όμοιος με τοπικό όργανο ενδείξεως		$d = 3 \text{ mm}$
5.27	Μετρητής Venturi με τοπικό όργανο ενδείξεως		
5.28	Μετρητής με πτερώγια		$l = 7 \text{ mm}$
5.29	Μετρητής ογκου		
5.30	Μετρητής CO ₂		$d = 3 \text{ mm}$
5.31	Ενδείκτης στάθμης		$l = 12, h = 4 \text{ mm}$
5.32	Όμοιος με τοπική ένδειξη		
5.33	Μετρητής στρωφών		
5.33	Μετρητής τάσεως, εντάσεως, ισχύος		

1.3.3. Όργανα διακοπής

3.1	Όργανο διακοπής εν γένει		$l = 7, f = 3 \text{ mm}$
3.2	Όμοιος ανοικτό		
3.3	Όμοιος κλειστό		
3.4	Όργανο διακοπής με τροχό		
3.5	Όργανο διακοπής με στρόφαλο		
3.6	Όργανο διακοπής με έμβολο		$l = 7, a = 4 \text{ mm}$
3.7	Όργανο διακοπής μαγνητικό		$l = 7, a = 4 \text{ mm}$
3.8	Όργανο διακοπής με κινητήρα		$l = 7, a = 4 \text{ mm}$
3.9	Όργανο διακοπής υδραυλικό		$l = 7, a = 3 \text{ mm}$
3.10	Όργανο διακοπής με λάδι		$l = 7, a = 3 \text{ mm}$
3.11	Όργανο διακοπής με μεμβράνη		
3.12	Όργανο διακοπής με πλωτήρα		
3.13	Δικλείδα κοινή (διελεύσας)		
3.14	Ασφαλιστικό με αντίβαρο		
3.15	Ασφαλιστικό με ελατήριο		
3.16	Δικλείδα με βαλβίδα αντεπιστροφής και δυνατότητα διακοπής της ροής		

και τεχνική του υδραμιού

3	Σύνδεση γενικά		
4	Σύνδεση με φλάντζες		
5	Συνδέσεις με φλάντζες και ζυφλή με σπή		
6	Τυφλή φλάντζα		
7	Σύνδεση με μούφα		
8	Σύνδεση με σφαιρική μούφα		
9	Μούφα ωθήσεως		$c = 4,0 \text{ mm}$
10	Συνδέσεις		$c = 4,0 \text{ mm}$
11	Σύνδεση βιδωτή		$c = 4,0 \text{ mm}$
12	Σύνδεσμος (κόπλερ)		$c = 4,0 \text{ mm}$
13	Σύνδεση με συγκόλληση ή κόλληση εν γένει		$e = 4 \text{ mm}$
14	Συγκολλούμενη μούφα		$e = 4 \text{ mm}$
15	Συγκολλούμενη σφαιρική μούφα		$e = 4 \text{ mm}$
16	Συγκολλούμενη μούφα ωθήσεως		$e = 4 \text{ mm}$
17	Συγκολλούμενη αποφρακτική δικλείδα		$e = 4 \text{ mm}$

$l = 6, f = 3 \text{ mm}$
Ανάλογη παράσταση άλλων συγκολλούμενων οργάνων

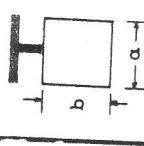
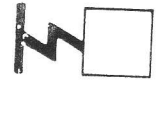


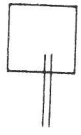



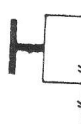

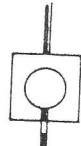



1.3.7. Σημείγματα σωλήνων

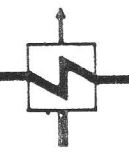
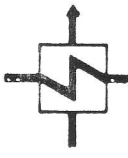
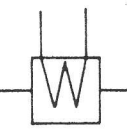
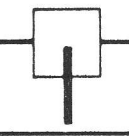
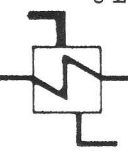
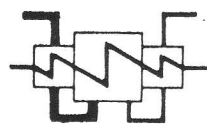
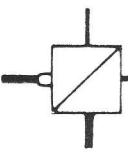
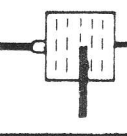
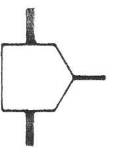
7.1	Έδρανο ολισθήσεως εν γένει	
7.2	Έδρανο ολισθήσεως με οδηγό	
7.3	Έδρανο ολισθήσεως με κυλινδρικούς	
7.4	Έδρανο ολισθήσεως με σφαιρικές	
7.5	Σταθερό σημείο	
7.6	Ομοίως με δυνατότητα περιστροφής	
7.7	Έδρανο υποβασταζόμενο εν γένει	
7.8	Έδρανο κρεμώμενο εν γένει	
7.9	Έδρανο κρεμώμενο ελατηριωτά	
7.10	Έδρανο υποβασταζόμενο ελατηριωτά	
7.11	Έδρανο με υποστήριξη εξισούμενη	

α και τεχνική του υδραυλικού

Επί μέρους στοιχεία αφορώντα στα όργανα

Ανοίγει με αύξηση του ρυθμιστικού μεγέθους		$d = 4 \text{ mm}$
Ανοίγει με μείωση του ρυθμιστικού μεγέθους		
Ανοίγει με αύξηση του ρυθμιστικού μεγέθους υπεράνω της τιμής...		
Ανοίγει με μείωση του ρυθμιστικού μεγέθους κάτω της τιμής...		
Κλείνει με αύξηση του ρυθμιστικού μεγέθους υπεράνω της τιμής...		
Κλείνει με μείωση του ρυθμιστικού μεγέθους κάτω της τιμής...		
Έμβολο		$a = b = 6 \text{ mm}$
Έμβολο με σύνδεση λαδιού και από τις δύο πλευρές		
Έμβολο με ελατήριο και λάδι		
Πέδη ελαίου		
Διάταξη βαλβίδας - έδρας		
Ελατήριο		$a = b = 6 \text{ mm}$
Σταθερό σημείο μηχανισμού ρυθμίσεως		
Οριακή πρόσκρουση		


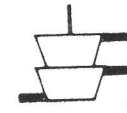





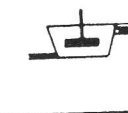
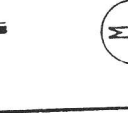
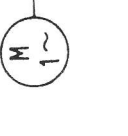
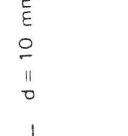
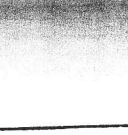
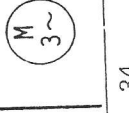
8.1	Ατμοπαραγωγός χωρίς υπερθερμάνητρα		$a = b = 10 \text{ mm}$
8.2	Ατμοπαραγωγός με υπερθερμάνητρα		
8.3	Ατμοπαραγωγός με εστία κόνεως		
8.4	Ομοίως, με εστία εσχάρας		
8.5	Ομοίως, με εστία πετρελαίου		
8.6	Ομοίως, με εστία αερίου		
8.7	Ομοίως, με τηκόμενη τέφρα		
8.8	Ατμοπαραγωγός αποθερμότητας		
8.9	Ηλεκτρικός ατμοπαραγωγός		
8.10	Απαιρωτής γαιανθράκων		
8.11	Εξαερωτής γαιανθράκων		
8.12	Προθερμαντήρας νερού με καπναέρια		γωνία 60° $g = 6 \text{ mm}$
8.13	Υπερθερμαντήρας ατμού με καπναέρια		γωνία 60°
8.14	Προθερμαντήρας νερού με ατμό συμπυκνούμενο		

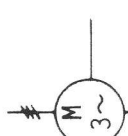
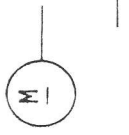
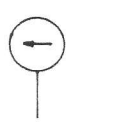
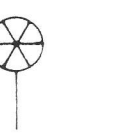
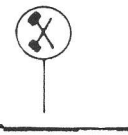
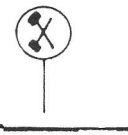
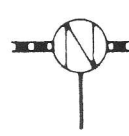
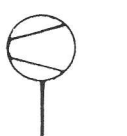
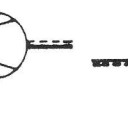
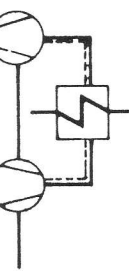
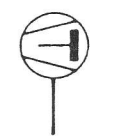
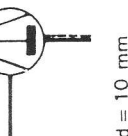
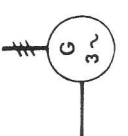
8.15	Υπερθερμαντήρας ατμού με ατμό συμπυκνούμενο		
8.16	Υπερθερμαντήρας ατμού με ρεόντα ατμό		
8.17	Προθερμαντήρας νερού με θερμό νερό		
8.18	Προθερμαντήρας νερού με ανάμιξη ατμού		
8.19	Προθερμαντήρας νερού με ατμό (επιφανείας)		$a_1 = c_1 = 6 \text{ mm}$ $b_1 = 10 \text{ mm}$
8.20	Ομοίως, με αποθερμανση υπερθέρμου ατμού και υπόψηξη συμπυκνωμάτων		
8.21	Μετατροπέας ατμού με επιφάνεια		$a = b = 10 \text{ mm}$
8.22	Ψύκτης ατμού με διαβίβαση υπερθέρμου ατμού κάτω από το νερό		
8.23	Εξυδατωτής ατμού		

8.34	Ψυγείο αέρα	
8.35	Ψυγείο αναμίξεως	
8.36	Εκτόνωση ατμού στο περιβάλλον	
8.37	Δοχείο χωρίς πίεση	
8.38	Ανοικτό δοχείο	
8.39	Δοχείο με μαξιλάρια ατμού ή προστατευτικού αερίου	
8.40	Δοχείο με υπερπίεση	
8.41	Ισόθλιπτος αποταμιευτής	
8.42	Αποταμιευτής νερού με προθερμαντήρα αναμίξεως	
8.43	Αποταμιευτής θλιπτικής πίεσης (Ruths)	
8.44	Απαιριωτής	
8.45	Τζιφάρι ατμού για εξαγωγή αέρα	
8.46	Τζιφάρι νερού για εξαγωγή αέρα	
8.47	Τροφοδοτικό τζιφάρι ατμοπαγωγών	

24	Εκτονωτής	
25	Κυκλικός διαχωριστής τέφρας	
26	Ηλεκτρόφιλτρο	
3.27	Διαχωριστής με παντελόνια	
8.28	Υγρός διαχωριστής	
8.29	Εκκαπνιστές	
8.30	Καταναλωτής θερμότητας χωρίς επιφάνεια (μιξέως)	
8.31	Καταναλωτής θερμότητας με επιφάνεια	
8.32	Ψυγείο επιφανείας με φρέσκο νερό	
8.33	Ψυγείο επιφανείας με νερό ανακυκλοφορούμενο (πύργος ψύξεως)	
8.32	Ψυγείο επιφανείας με φρέσκο νερό	
8.33	Ψυγείο επιφανείας με νερό ανακυκλοφορούμενο (πύργος ψύξεως)	

9. Μηχανές

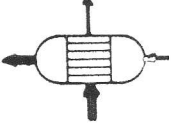
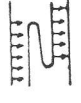
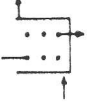

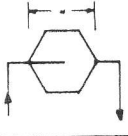
1	Ατμοστρόβιλος		$m = 10 \text{ mm}$
2	Ατμοστρόβιλος με μη ρυθμιζόμενη απομάστευση		
3	Ατμοστρόβιλος με ρυθμιζόμενη απομάστευση		
4	Διπλός ατμοστρόβιλος (κουβαρίστρα)		
5	Ατμοστρόβιλος με ενδιάμεση υπερθέρμανση (με αναθέρμανση)		
6	Αεριοστρόβιλος		
7	Αεριοστρόβιλος		
8	Υδροστρόβιλος		
9	Εμβολοφόρα μηχανή γενικά		
9.10	Εμβολοφόρα ατμομηχανή		
9.11	Μηχανή εσωτερικής καύσεως		
9.12	Ηλεκτροκινητήρας εναλλασσόμενου ρεύματος μονοφασικός		$d = 10 \text{ mm}$
9.13	Ομοίως τριφασικός		

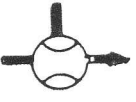

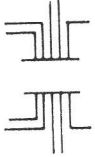
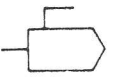

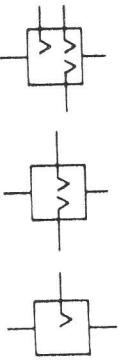

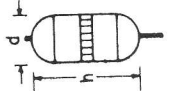
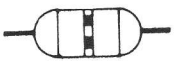
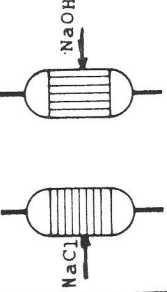
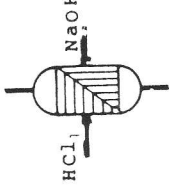
9.14	Ομοίως με δακτυλίου		
9.15	Ηλεκτροκινητήρας συνεχούς ρεύματος		
9.16	Αντλία φυγοκεντρική		$d = 8 \text{ mm}$
9.17	Αντλία εμβολοφόρα		
9.18	Μηχανή προωθήσεως εν γένει		
9.19	Μύλος λειοτριβήσεως		
9.20	Διανομέας (π.χ. γαϊάνθρακα)		$d = 8 \text{ mm}$
9.21	Στροβιλοσυμπιεστής εν γένει		$d = 10 \text{ mm}$
9.22	Στροβιλοσυμπιεστής αέρα		
9.23	Στροβιλοσυμπιεστής αέρα με ενδιάμεσο ψυγείο		
9.24	Εμβολοφόρος συμπιεστής εν γένει		
9.25	Εμβολοφόρος συμπιεστής αέρα		$d = 10 \text{ mm}$
9.26	Ηλεκτρογεννήτρια εναλλασσόμενου ρεύματος, τριφασικού		

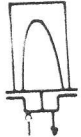
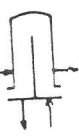




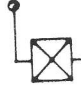


1.3.10. Πρόσθετοι συμβολισμοί θερμάνσεων

10.1	Λέβητας νερού		8 x 10 mm
10.2	Θερμαντικό σώμα		10 x 6 mm
10.3	Θερμαντικό σώμα με φέτες		
10.4	Επίπεδο θερμαντικό σώμα		
10.5	Κονβέρτερ		
10.6	Περιμετρικό θερμαντικό σώμα		
10.7	Πτερυγοφόρος σωλήνας		
10.8	Σερπαντίνα		
10.9	Σωληνωτός θερμαντήρας αέρα		
10.10	Εναλλάκτης θερμότητας με επιφάνεια, γενικώς		10 x 10 mm
10.11	Σωληνωτός εναλλάκτης με ευθύγραμμους σωλήνες διασταυρούμενης απλής ροής		
10.12	Ομοίως, διπλής ροής		i = 16, d = 8 mm

9.27	Ομοίως, μονοφασικού	
9.28	Ηλεκτρογεννήτρια τριφασικού εναλλασσόμενου ρεύματος με διέγερση	
9.29	Ομοίως, μονοφασικού	
9.30	Ηλεκτρογεννήτρια με αναψυχόμενο αέρα	
9.31	Ηλεκτρογεννήτρια με ψύξη υδρόγονου	
9.32	Ηλεκτρογεννήτρια συνεχούς ρεύματος	
9.33	Στροβιλογεννήτρια με σταθερό σύνδεσμο	
9.34	Ομοίως με λυόμενο (οπισθοδρομούντα σύνδεσμο)	
9.35	Ηλεκτροκίνητος συμπιεστής με ρυθμιζόμενο σύνδεσμο	
9.37	Στροβιλογεννήτρια με κιβώτιο σταθερής σχέσεως μεταβολής στροφών	
9.36	Ηλεκτροκίνητος συμπιεστής με ρυθμιζόμενη σχέση μεταβολής στροφών	

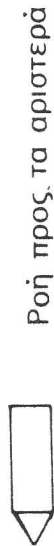
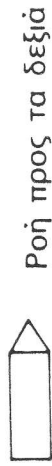
8.59	Βραστήρας ατμού	
8.60	Ψυκτήρας καταιονισμού	
8.61	Ψυκτήρας με σερπαντίνα	$a = b = 8 \text{ mm}$ 
8.62	Ψυκτήρας ατμού με διασκορπισμό νερού	
8.63	Ψυκτικός πύργος	$k = 10 \text{ mm}$ 

8.48	Τζιφάρι συμπίεσεως ατμού	
8.49	Υπερχείλιση δοχείου	
8.50	Συλλέκτης γραμμών	
8.51	Δοχείο αντιδράσεως	
8.52	Δοχείο αναδεύσεως με τάρρακτρο	$a = b = 8 \text{ mm}$ 
8.53	Διανεμητής μιας, δυο, τριών διακλαδώσεων	
8.54	Δοσιμετρική διάταξη	
8.55	Φίλτρο μηχανικού καθαρισμού	$d = 7, h = 16 \text{ mm}$ 
8.56	Φίλτρο ενεργού άνθρακα	
8.57	Εναλλάκτης (Na), (OH)	
8.58	Εναλλάκτης μικτού στρώματος	

0.13	Ομοίως, με φουρκέτες	
10.14	Ομοίως αντίρροπης και ομόροπης ροής	
10.15	Ομοίως διασταυρούμενης λόγω φραγμάτων ροής	
10.16	Θερμαντήρας με σερπαντίνα	
10.17	Αερόθερμο τοίχου a = ανακυκλοφορούμενος, b = εξωτερικός αέρας	
10.18	Φράκτης ρυθμίσεως ελκυσμού	
10.19	Βαλβίδα εξαερισμού	
10.20	Αερισμός, εξαερισμός	
10.21	Πυροστάτης	

1.4. ΠΡΟΤΕΙΝΟΜΕΝΑ ΧΡΩΜΑΤΑ ΣΩΛΗΝΩΣΕΩΝ

Οι σωληνώσεις συνιστάται να βάφονται με κάποιο ουδέτερο χρώμα π.χ. γκρι. Φέρνουν όμως επ' αυτών επιγραφές ορθογώνιες με περίγραμμα λευκό και βέλος που δείχνει την κατεύθυνση της ροής ως εξής:



Το εσωτερικό των επιγραφών βάφεται με χρώμα που αντιστοιχεί στο ρέον ρευστό, όπως στον πίνακα 1.

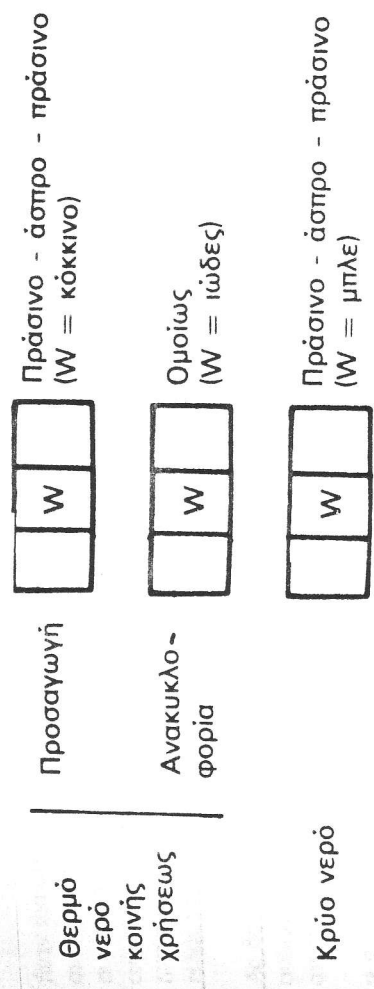
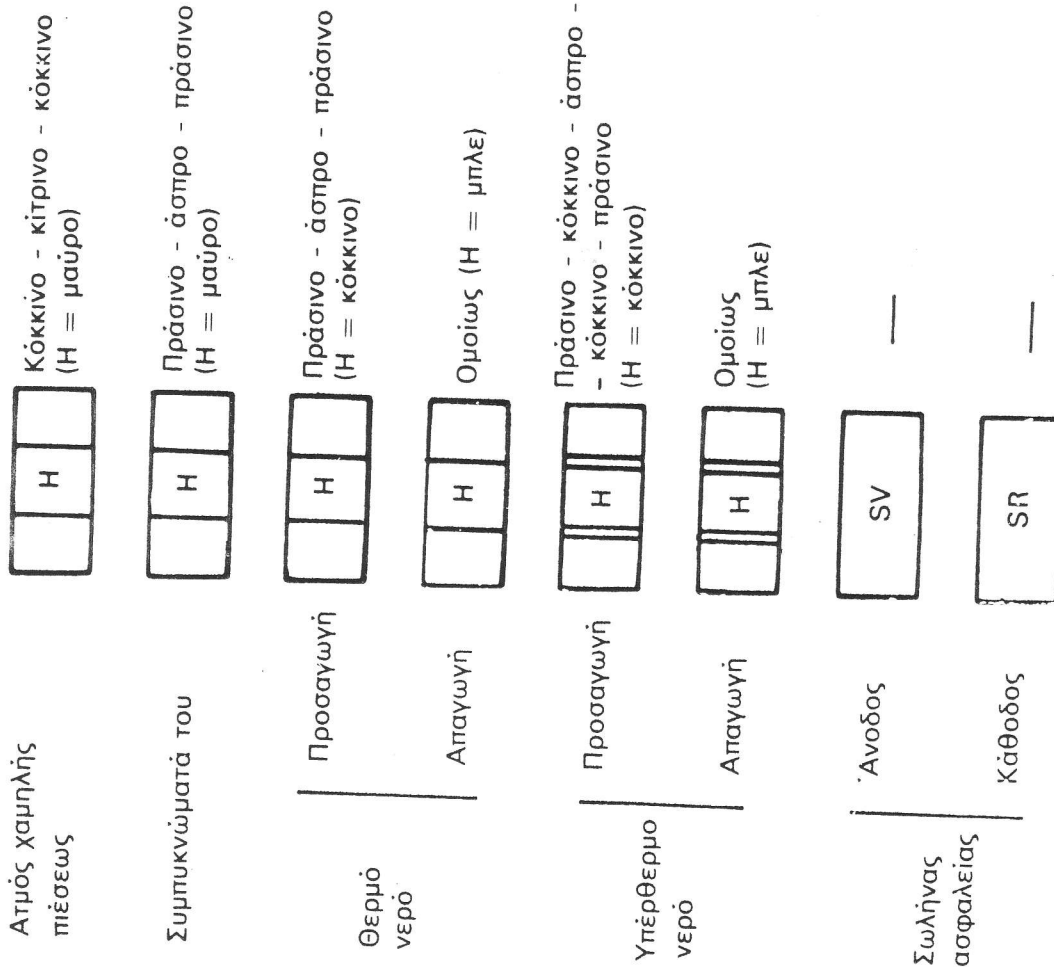
Πίνακας 1

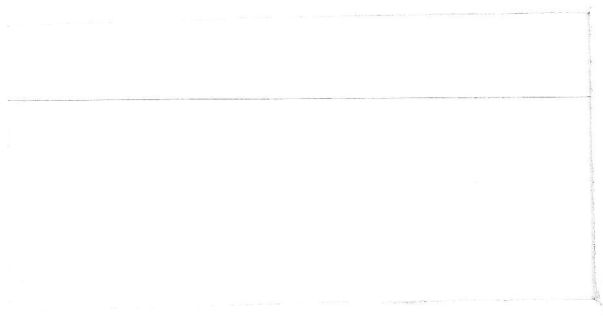
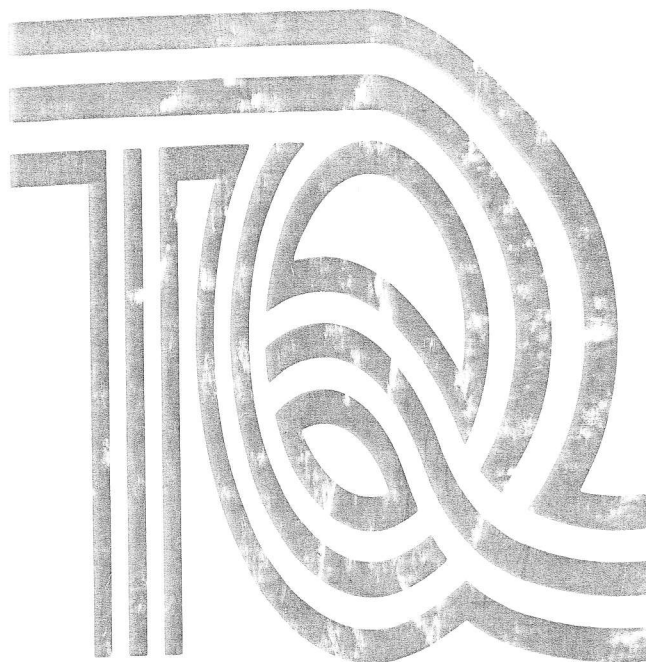
Χρώματα σωληνώσεων

Ομάδα	Ρέον ρευστό	Χρώμα Ορθογωνίου	Βέλος
1	Νερό	Πράσινο	Πράσινο
2	Ατμός	Κόκκινο	Κόκκινο
3	Αέρας	Μπλε	Μπλε
4	Αέριο, καύσιμο	Κίτρινο	Κόκκινο
5	Αέριο, μη καύσιμο	Κίτρινο	Κίτρινο
6	Οξεία	Πορτοκαλί	Πορτοκαλί
7	Βασείς	Λώδες	Λώδες
8	Υγρά, καύσιμα	Καφέ	Κόκκινο
9	Υγρά, μη καύσιμα	Καφέ	Καφέ
0	Κενό	Γκρι	Γκρι

Πρόσθετα διευκρινιστικά στοιχεία αναγράφονται μέσα στα ορθογώνια με γράμματα ή σύμβολα π.χ. στην ομάδα 2, $p = 10 \text{ bar}$, $t = 20^\circ\text{C}$, ή στην ομάδα 4, $H_0 = 37,5 \text{ MJ/Nm}^3$, $p = 25 \text{ mbar}$ ή στην ομάδα 6, H_2SO_4 n/10.

Για διάκριση οι σωληνώσεις θερμάνσεως και ψυχρού νερού δεν φέρουν βέλη. Το ορθογώνιο τους χωρίζεται σε τρία ή πέντε τμήματα το δε μεσαίο φέρει ενδεικτικό γράμμα διαφόρου χρώματος ως εξής:





TecEquipment

TD800 STEAM POWER PLANT
INSTRUCTIONAL MANUAL

written by

Dr. M. A. Bell

Senior Lecturer, Plymouth Polytechnic, U.K

The equipment described in this manual is supplied by

T E C Q U I P M E N T
Group of Companies

Suppliers of Technological Laboratory
Equipment designed for Teaching

BONSALL STREET, LONG EATON, NOTTINGHAM, NG10 2AN, ENGLAND

TELEPHONE: LONG EATON 722611 TELEX: 377828

© TecEquipment Limited

No part of this publication may be reproduced or transmitted in any form or by any means, electronic or mechanical, including photocopy, recording, or any information storage and retrieval system, without the express permission of TecEquipment Limited.

Whilst all due care has been taken to ensure that the contents of this manual are accurate and up to date, no responsibility, direct or consequential, can be accepted for any errors or omissions.

A Packing Contents List is supplied with the equipment and it is recommended that the customer checks carefully the contents of the package(s) against the list ensuring that no items are missed.

Should there be any items missing, the customer should contact the local TecEquipment agent or TecEquipment direct.

- CONTENTS -

Section	Page	
1	GENERAL INTRODUCTION & DESCRIPTION OF THE PLANT	1
1.1	Theory of Steam Plant	
1.2	Plant Description	
2	LIST of EXPERIMENTS	13
3	INSTRUMENTATION	15
3.1	Fuel System	
3.2	Steam Circuit	
3.3	Condensate Circuit	
3.4	Condenser Cooling Water Circuit	
3.5	The Turbine	
4	SAFETY PRECAUTIONS and NORMAL OPERATING PROCEDURE	19
4.1	General Safety Precautions	
4.2	Operating Procedure	
4.3	Alternative Operating Modes	
5	CALIBRATION of MEASURING INSTRUMENTS	28
6	EXPERIMENTAL PROCEDURES	31
6.1	Steam Mass Flow Rate	
6.2	Boiler Efficiency	
6.3	Turbine Isentropic Efficiency	
6.4	Steam Cycle Thermal Efficiency	
6.5	Overall Plant Thermal Efficiency	
6.6	Heat Exchanger Effectiveness	
6.7	Steady State Energy Analyses	
6.8	Insulation Effectiveness	
7	TYPICAL EXPERIMENTAL RESULTS and ANALYSIS	35
7.1	Steam Mass Flow Rate	
7.2	Boiler Efficiency	
7.3	Turbine Isentropic Efficiency	
7.4	Steam Cycle Thermal Efficiency	
7.5	Overall Plant Thermal Efficiency	
7.6	Heat Exchanger Effectiveness	
7.7	Steady State Energy Analyses	
7.8	Insulation Effectiveness	
8	LOG SHEET and SYSTEM DIAGRAM	44
9	BIBLIOGRAPHY	47

LIST of FIGURES

Figure	Title	Page
1	Basic Steam Cycle	1
2	Steam Plant System Diagrammatic	7
3	Cross-section of the Turbine	8

LIST of PLATES

Plate	Title	
1	Overall View of the Plant	9
2	The Boiler and Accumulator	10
3	The Turbine	11
4	The Electrical Control Console	12

LIST of SYMBOLS USED

Symbols	Subscripts
E Heat Exchanger Effectiveness	f Saturated liquid
g Gravitational Acceleration	g Saturated vapour
h Specific Enthalpy	s Steam
N RPM	cw Cooling Water
p Pressure	fu Fuel
Q Heat Quantity	amb Ambient
s Specific Entropy	in Inlet
v Velocity	out Outlet
W Work Quantity	
z Datum height	Location reference numbers
Δ 'difference'	may also be used as subscripts
m Mass flow rate	(See System Diagram)
x Dryness fraction	
A Surface area	
C Specific Heat Capacity	
η Efficiency	

SECTION 1

GENERAL INTRODUCTION & DESCRIPTION OF THE PLANT

1.1 THEORY OF STEAM PLANT

A simple basic steam cycle is shown diagrammatically in Fig. 1. In theory the system is completely closed and the thermodynamic working fluid is pure steam or water. The system constitutes a heat engine, where heat is supplied, (\dot{Q}_{in}) by the boiler (or steam generator), mechanical power, (\dot{W}_{out}) is produced by the expander (an impulse turbine in this plant) as the high pressure steam expands to a lower pressure. Heat is rejected, (\dot{Q}_{out}) by the condenser. The cycle is closed by means of the feed pump which pumps the condensed steam (condensate) back into the boiler. A small amount of mechanical power is required to drive the feed pump, (\dot{W}_{in}).

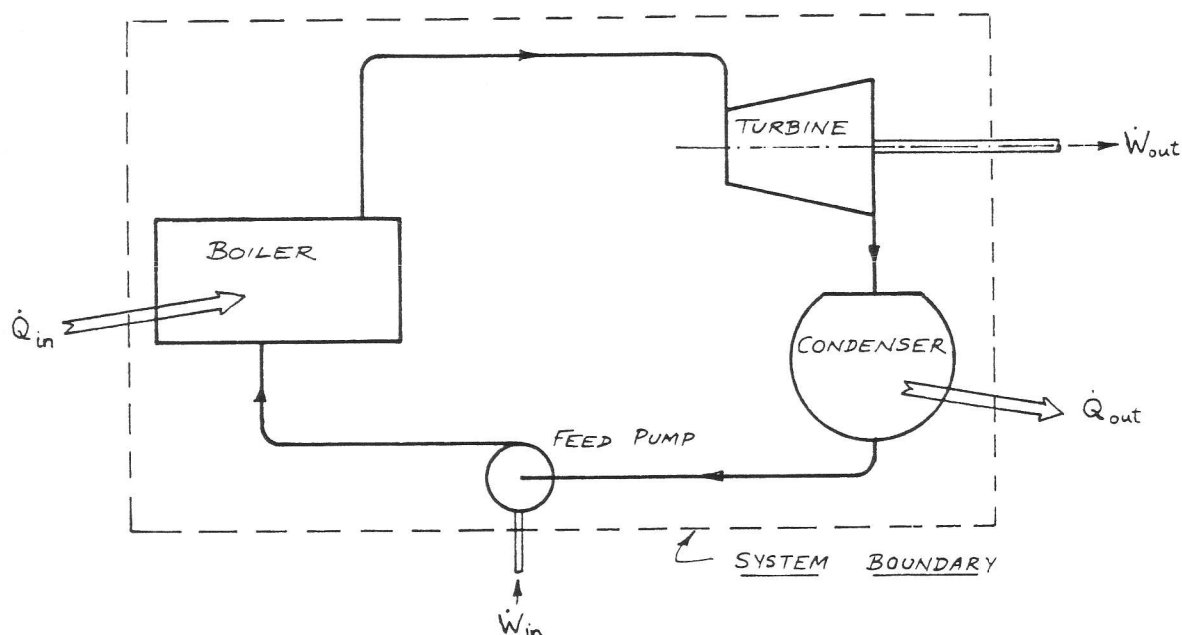


Fig. 1 Basic Steam Cycle

In the absence of any heat or frictional losses, and with steady state operation, an energy balance must exist such that:

$$\dot{Q}_{in} + \dot{W}_{in} = \dot{Q}_{out} + \dot{W}_{out}$$

The theoretical thermal efficiency of the heat engine is the ratio:

$$\eta_{th} = \frac{\text{Nett Mechanical Power Output}}{\text{Thermal Power Input}}$$

In practice real steam plant is very much more complex than that shown in Fig. 1 owing to the need to provide adequate and safe means of starting, controlling, and stopping the plant, providing for the transfer of heat to and from the system, compensating for leakage, preventing corrosion etc. Fig. 2 shows the actual steam plant in diagrammatic form.

The remainder of this Instructional Manual is written with the assumption that the reader is familiar with basic steam theory, aware of the properties of steam/water, and aware of the thermodynamic processes involved in the Rankine steam cycle.

The Bibliography gives a selection of reference material graduated from elementary texts to advanced material. The reader should select appropriate material from this list for further reading if required.

The Steam property tables and enthalpy/entropy chart (Mollier chart) used throughout is:

Thermodynamic Tables in S.I. (metric) Units 2nd edition
by R.W. Haywood (Cambridge University Press 1972)

S.I. (metric) units are used in all measurements and calculations.

1.2 PLANT DESCRIPTION

A diagrammatic scheme of the plant is shown in Fig. 2 and a general view of the plant is shown in Plate 1. Each component of the plant is described below.

1.2.1 The Boiler and Steam Accumulator (See Plate 2)

The GARIONI GMT-45 boiler is a water-tube boiler designed to produce a maximum steam flow of 450 kg/h at a pressure of 10 bar (gauge) and 270°C. i.e. It produces super-heated steam via a coiled tube superheater located at the end of the combustion chamber.

The boiler is oil fired and is equipped with a double flame automatic burner. Once started, the boiler is automatic in operation. It is fitted with all the necessary instrumentation, safety devices, controls and interlocks to ensure safe and correct operation.

Water is fed to the boiler continuously by one of the two reciprocating feed pumps located beneath the main body of the boiler. The feed pump operates at either a low or high speed depending on whether one or both burner flames is selected. The feed pump flow rates are such as to produce saturated steam which enters the steam accumulator.

If superheated steam is required (normal operation), the valves are set to direct the saturated steam from the accumulator to the superheater coils. If saturated steam is required, the superheater coils may be by-passed. Note that under these conditions provision is made to direct a flow of cooling water through the superheater coils to prevent their overheating.

The steam accumulator acts as a steam storage reservoir and allows a steady steam supply to be delivered irrespective of fluctuations in saturated steam supply. Condensate may form in the accumulator either

because of heat loss from the accumulator or water carry-over from the saturated steam generator. The maximum condensate level is controlled by a bucket steam trap. If the condensate level rises beyond a safe level the boiler automatically shuts down. The condensate level may be observed on the sight glass situated on the side of the accumulator.

Further details concerning the boiler can be found from the Boiler Operation Handbook supplied.

1.2.2 The Turbine (See Plate 3)

The COPPUS RLA 12M turbine is a single-stage velocity compounded impulse turbine. The turbine wheel is 380 mm in diameter and its maximum permitted rotational speed is 3630 RPM, (the trip speed). It has four steam nozzles, three of which can be shut off by hand valves.

Supplied with steam at 9 bar exhausting to -0.8 bar it is capable of supplying 8 kW at 3000 RPM with all steam nozzles open.

The turbine is directly coupled to the drive with no gear reduction. Integral with the turbine is its speed control governor which acts to maintain a steady turbine speed irrespective of the shaft power requirement (within its operational limits). The governor is self-contained with its own oil supply. In addition to the governor there is an over-speed trip which acts to shut off the steam supply completely if the turbine speed reaches or exceeds a dangerous level.

Consult the Turbine Operating Handbook for further details concerning the turbine. Instructions concerning the adjustments, maintenance and operation of the governor and over-speed trip can also be found in the Turbine Operating Handbook.

A general cross-section through the turbine is shown in Fig. 3.

1.2.3 The Condenser

The condenser is a simple single pass shell-and-tube heat-exchanger. Cooling water from the cooling tower enters one end of the condenser, while steam enters from the opposite end. Condensate drains by gravity into the condensate vessel.

The condenser normally operates under vacuum. The vacuum pump removes air from the condenser during plant operation.

A pressure relief valve is fitted to prevent the condenser from being subjected to excessive pressure, and a cooling water high temperature warning is also provided.

1.2.4 The Condensate Vessel

The condensate vessel is a closed container which receives condensate from the condenser. It has a total capacity of approximately 60 litres. The vessel is fitted with a float switch which turns the condensate extraction pump ON when the condensate level reaches its upper limit and OFF at its lower limit. The capacity between the float level switch settings is approximately 20 litres. The sight glass enables the condensate level to be ascertained. Air or steam is thus prevented from

entering the condensate extraction pump. There are two condensate extraction pumps, only one of which is needed to operate the plant.

1.2.5 The Feed Water Tank (or Hot Well)

The feed water tank has a capacity of approximately 550 litres and acts as a water reservoir for the plant. Any water lost during plant operation would result in a reduction of water level in the feed tank. However, lost water is replaced by 'make-up' water which enters the feed tank from the water softener under the control of a float valve. The sight glass enables the feed water level to be ascertained.

1.2.6 The Cooling Tower

The APV HALL PN16/600 cooling tower is a single cell, induced draft, cooling tower. It is designed to dissipate approximately 300 kW of heat at design conditions where the hot water temperature to the tower is 45°C and the ambient air wet bulb temperature is 29°C.

The cooling effect from a cooling tower is achieved by passing the hot water over packing material to give it a large exposed surface area. Air drawn across the packing in the opposite direction to the water flow causes evaporation where the majority of the latent heat required for evaporation is extracted as sensible heat from the water thus reducing its temperature.

The water lost by evaporation is made-up via a float valve which maintains the water level in the storage tank which forms the base of the cooling tower.

Further details of the cooling tower can be found in the Cooling Tower manual supplied.

1.2.7 The Automatic Water Softener

In order to, prevent the build-up of scale on the boiler tubes, it is necessary to remove from the supply water the dissolved minerals which cause it. This is accomplished by the ion-exchange water softener unit. Its operation depends on the substitution of low solubility ions (usually Ca++) with high solubility ions (Typically Na+).

The operation and regeneration of the water softening medium (the ion exchange resin) is accomplished automatically. Refer to the Water Softener Operation Manual supplied for further details concerning the water softening unit, and in respect of timing and when to replace the resin and regeneration salt.

A 25 litre drum of sulphite/phosphate/polymer (L7) boiler treatment is provided. This concentrated liquid solution for the prevention of corrosion and sludge formation can be added to the feed water tank. 1 litre should be added to the full tank of clean water before commissioning and replenished at the rate of 2 litres every 3 months.

Note: Prior to a long shut-down period it is recommended that the boiler tube is left filled with feed water which has been treated with 2 litres of L7 solution per full feed tank.

Reference 5 (Bibliography) gives further information concerning water softening and treatment.

1.2.8 The Electrical Control Console

The electrical control console contains all the electrical switches, controls and indicators necessary for plant operation except for the boiler which has its own control panel.

It also includes the dynamometer controls and indicators together with cooling water high temperature and high condensate level alarms.

The temperature and pressure at various locations on the plant may be selected and read on the digital readouts. The location from which the pressure or temperature is being read is shown by the illuminated lights on the mimic diagram situated above the control console.

See Plate 4 in order to identify each of the controls and indicators.

1.2.9 The Fuel Tank

The fuel tank has a capacity of 100 litres. It is fitted with a burette to enable fuel flow measurements to be made. The burette can be filled by means of the fuel hand pump when the fuel level is low.

The fuel tank can be filled from an externally located fuel reservoir using the hand pump.

1.2.10 Pumps

There are four electrically driven pumps required to operate the plant:

- (1) The feed water pump (dual)-selected from the boiler control panel, runs continuously during boiler operation.
- (2) The condensate extraction pump (dual) - switched either automatically, by the condensate vessel float switches, or manually.
- (3) The vacuum pump - switched manually. It normally runs continuously during plant operation.
- (4) The cooling water pump (dual) - switched manually. It normally runs continuously during plant operation.

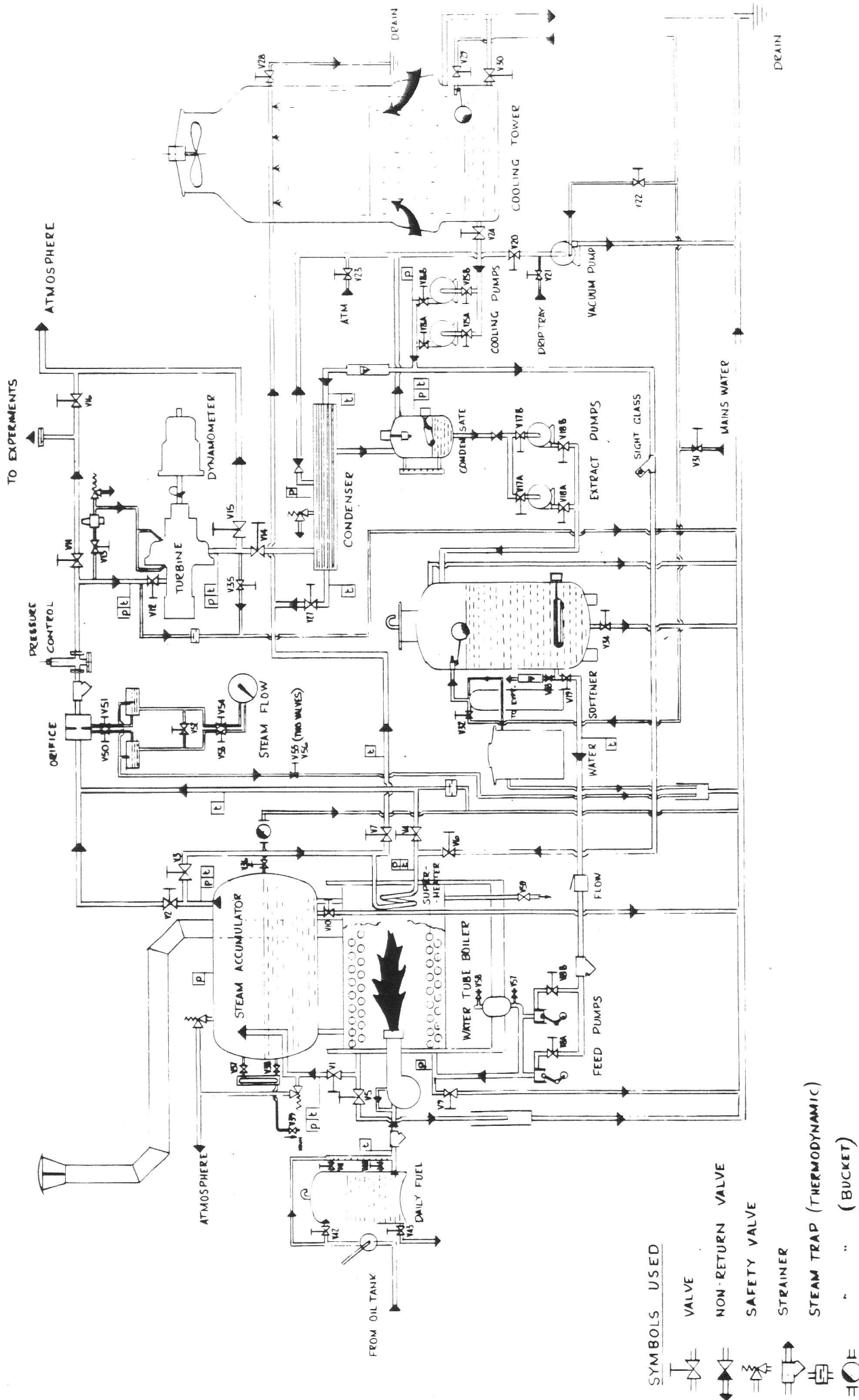
1.2.11 Ancilliary Equipment

The plant is appropriately equipped with various small components which are generally termed 'ancilliary'. i.e. They perform necessary but secondary functions compared with the major components described above. They comprise:

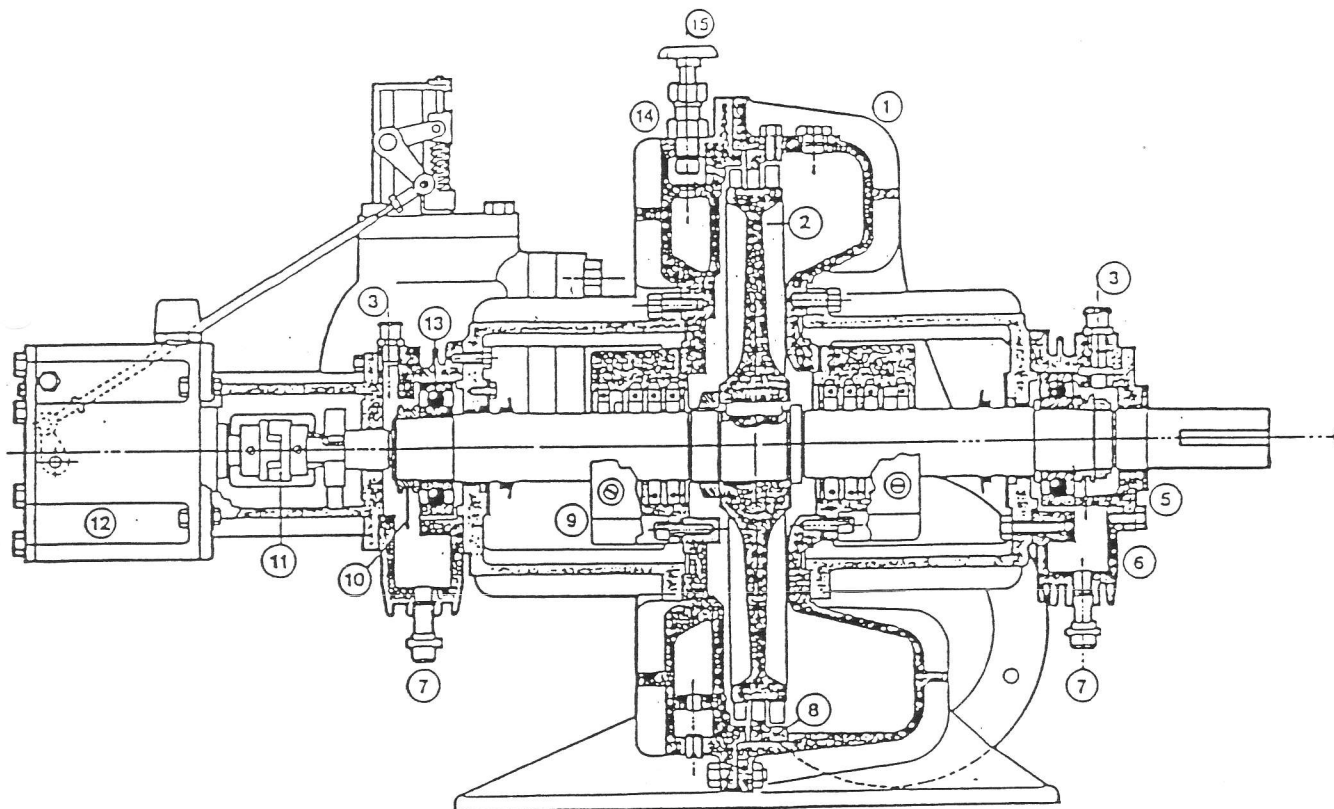
- (1) Safety valves - open to release steam if the pressure applied to them exceeds a preset level.
- (2) Pressure regulating (or reducing) valves - maintain a constant downstream pressure irrespective of the steam flow. A pressure regulating valve is essentially a pressure controlled throttle valve.
- (3) Steam traps - prevent the escape of steam, i.e. The steam is 'trapped', but allow the escape of condensate which is discharged to drain.

- (4) Non-return (or check) valves - permit the flow of fluid in one direction but prevent flow in the opposite direction.
- (5) Strainers (or filters) - trap particles of dirt or debris and prevent them from being circulated around the system where they could cause damage. Inspect strainers regularly and clean or renew them as necessary.
- (6) Manual valves - hand operated valves allow, prevent or regulate the flow of fluid.

NOTES:



FLOW DIAGRAM TD800



TURBINE LEGEND

- | | |
|-----------------------|--------------------------------|
| 1 - Turbine casing | 9 - Oil seal assembly |
| 2 - Turbine rotor | 10 - Lubrication ring |
| 3 - Oil plug | 11 - Coupling joint |
| 4 - Main shaft | 12 - Hydraulic governor |
| 5 - Bearing cover | 13 - Bearing |
| 6 - Bearing box | 14 - Stator cover with nozzles |
| 7 - Oil drain plug | 15 - Inlet valves |
| 8 - Fixed vane sector | |

KEY TO PLATE 1

- 1 - Boiler & Accumulator
- 2 - Feed Tank
- 3 - Orifice & Gauge
- 4 - Turbine & Dynamometer
- 5 - Condenser
- 6 - Condensate Vessel
- 7 - Vacuum pump
- 8 - Condensate Extraction pumps
- 9 - Cooling water pumps
- 10- Fuel supply tank
- 11- Electrical Control Console
- 12- Mimic Diagram

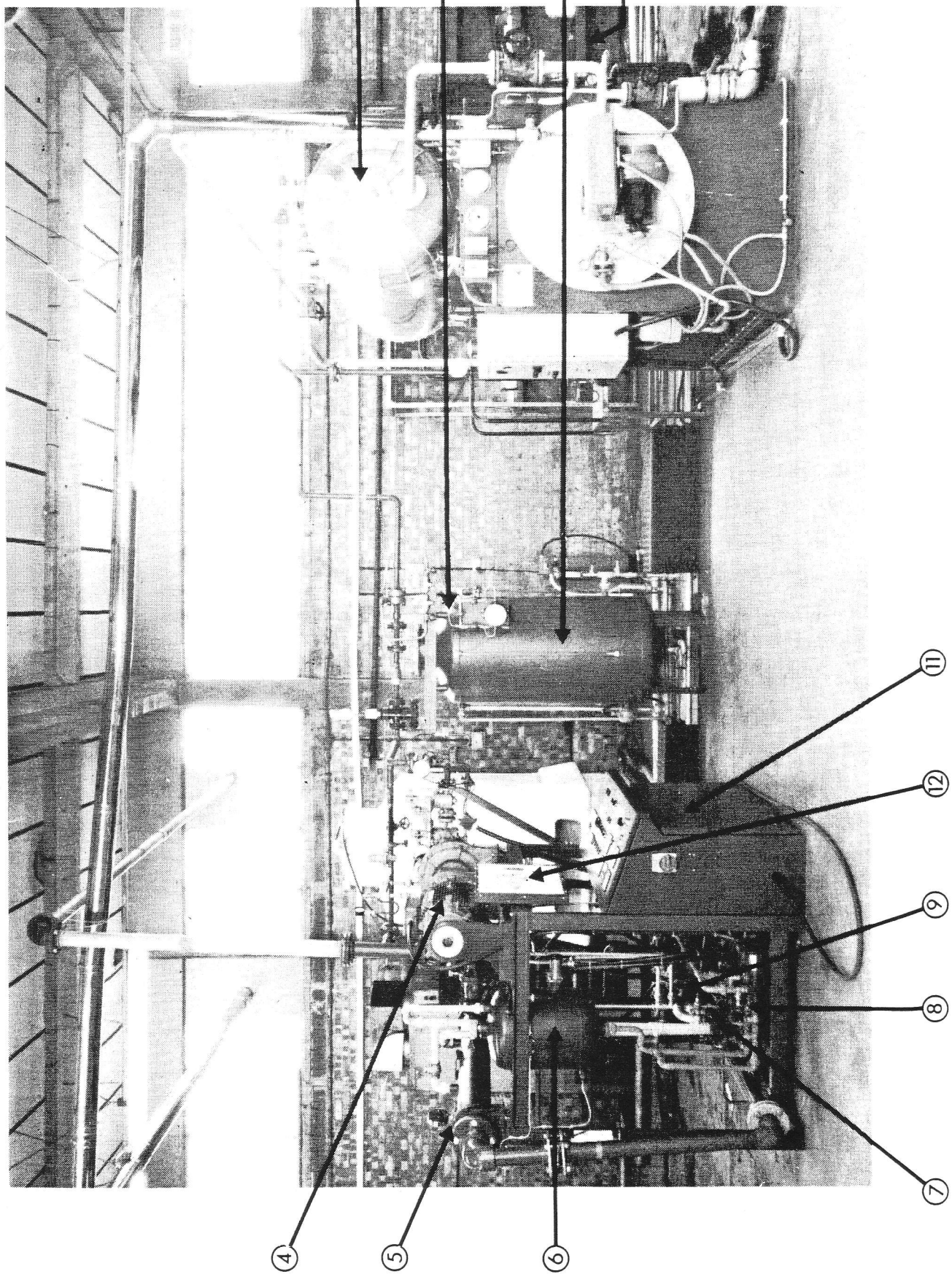


PLATE 1 OVERALL VIEW OF THE PLAN.

KEY TO PLATE 2

- 1 - Burner
- 2 - Feed pumps
- 3 - Accumulator
- 4 - Sight glass
- 5 - Safety valves
- 6 - Control Panel
- 7 - Steam pressure gauge
- 8 - Saturated Steam Temperature Gauge
- 9 - Superheated Steam Temperature Gauge
- 10- Trips from left to right:-
 - Maximum feed water pressure
 - Maximum steam pressure (sealed)
 - Burner/Feed pump HI / LOW pressure set
 - Burner cut-out pressure set
- 11- Feed pump hydraulic accumulator

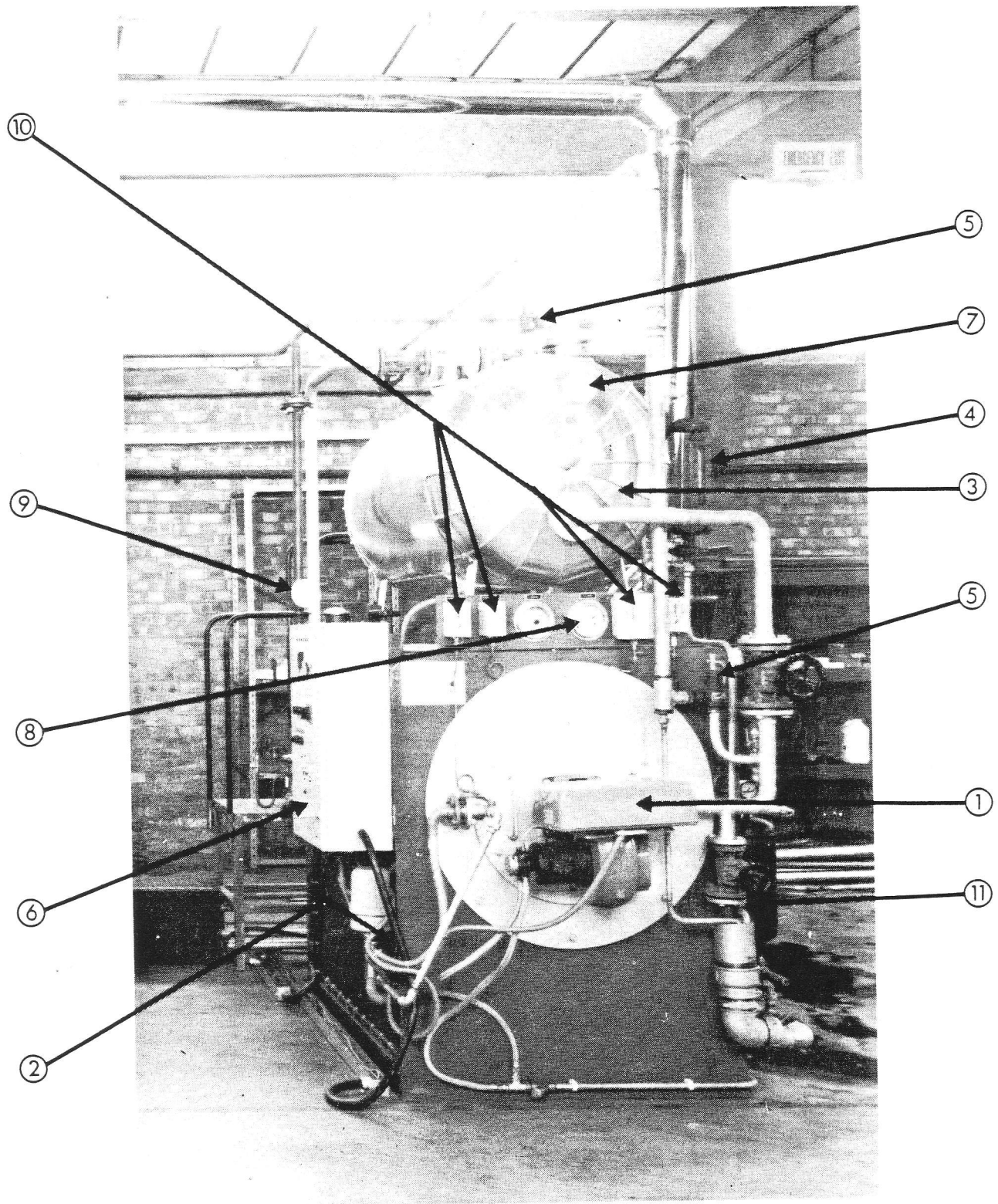


PLATE 2 THE BOILER AND ACCUMULATOR

KEY TO PLATE 3

- 1 - Turbine
- 2 - Governor
- 3 - Overspeed Trip valve
- 4 - Steam inlet valve
- 5 - Steam exhaust valve
- 6 - Dynamometer
- 7 - Nozzle hand wheels

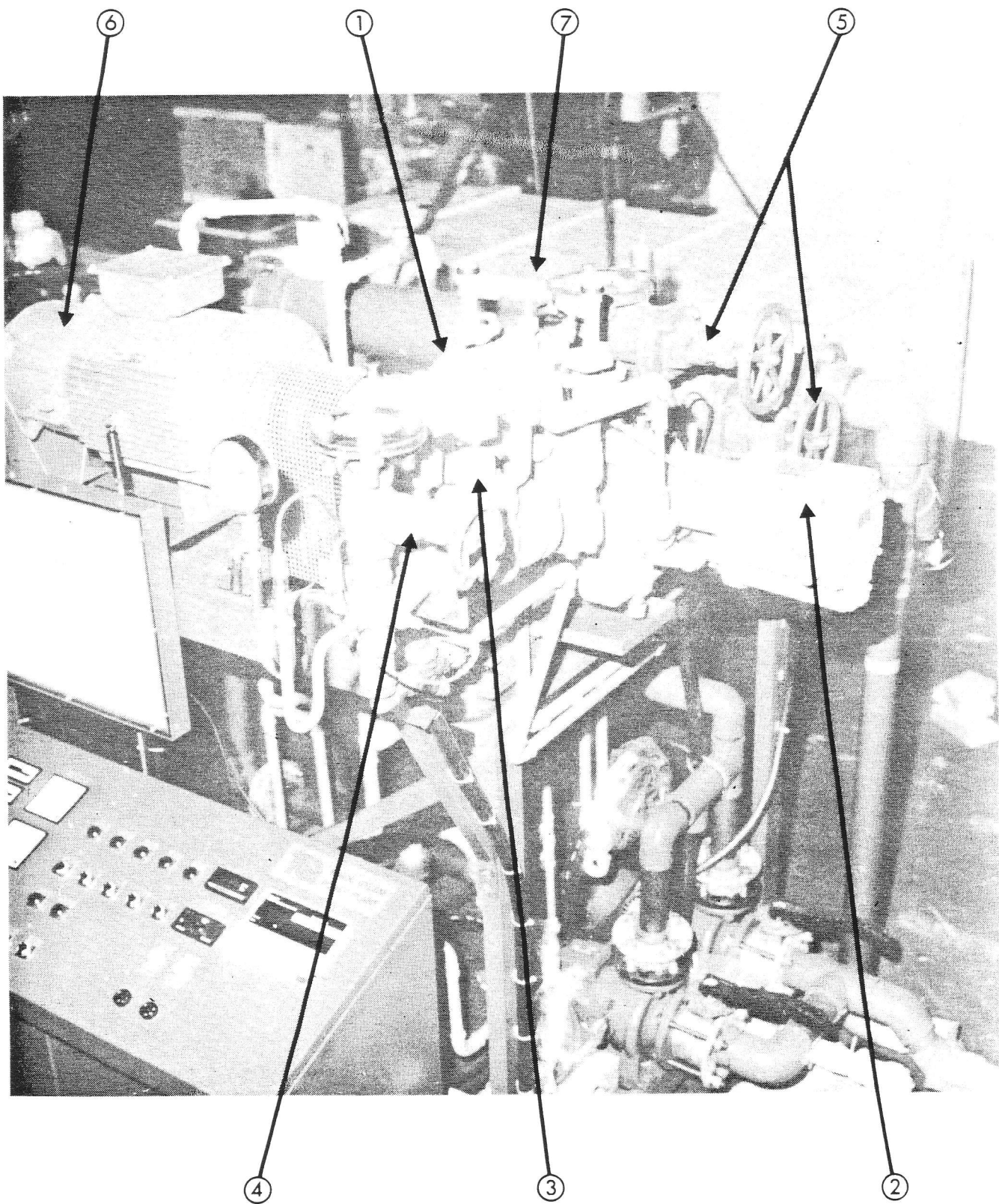


PLATE 3 THE TURBINE

KEY TO PLATE 4

- 1 - Master Switch
- 2 - Dynamometer Armature Amps / Volts Indicator
- 3 - Dynamometer Field Amps / Volts Indicator
- 4 - Dynamometer Control Rheostat
- 5 - Turbine Torque Indicator (Digital + Analogue)
- 6 - Turbine RPM Indicator (Digital + Analogue)
- 7 - Switches for Vacuum pump
 - Cooling water pumps
 - Cooling tower fan
 - Condensate Extract pumps
- 8 - Digital Pressure Indicator & Selector
- 9 - Digital Temperature Indicator & Selector
- 10 - Cooling Water High Temperature Warning Light & Siren
- 11 - Condensate High Level Warning Light & Siren

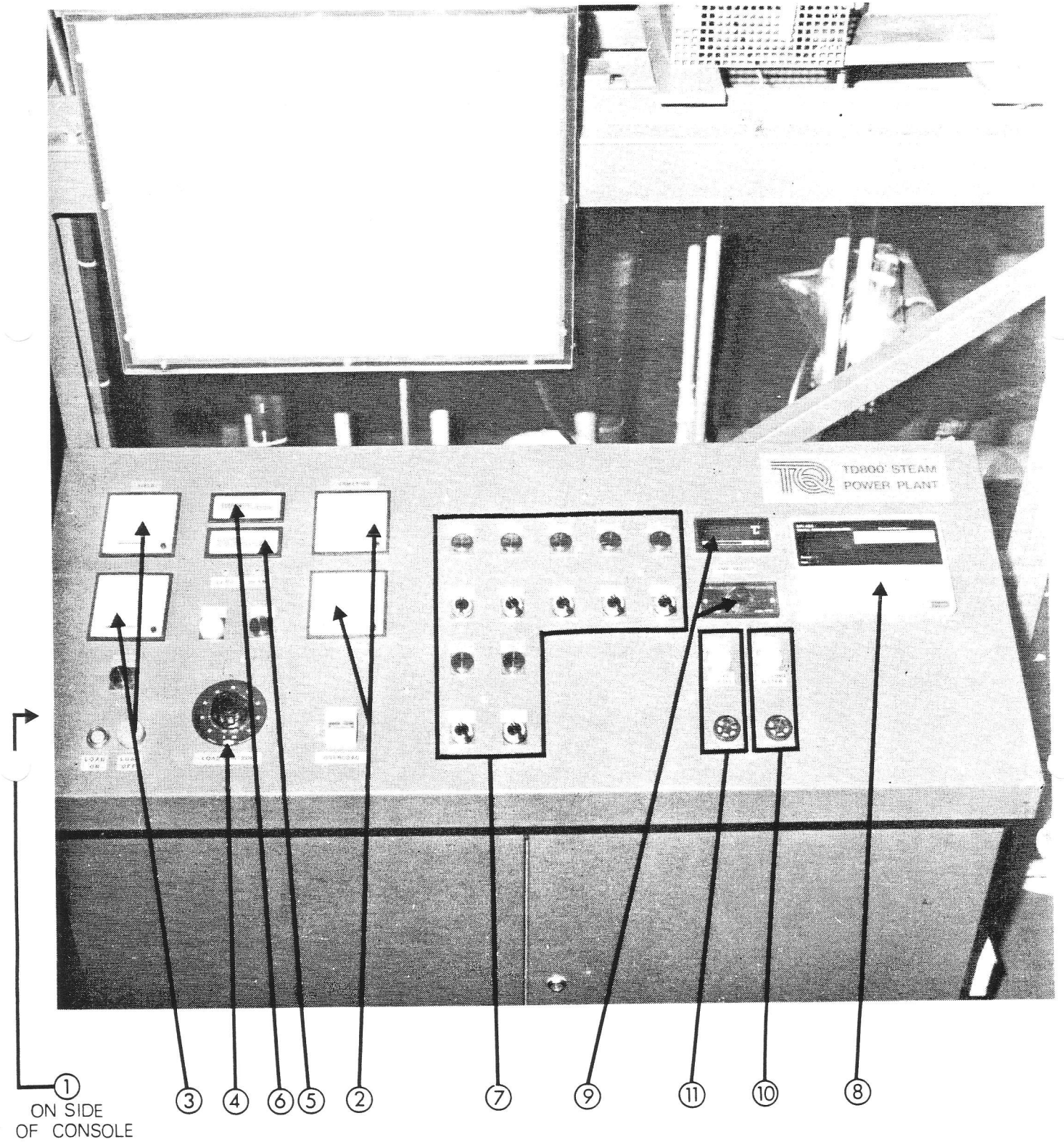


PLATE 4 THE ELECTRICAL CONTROL CONSOLE

SECTION 2

LIST of EXPERIMENTS

2.1 STANDARD EXPERIMENTS

Using the Plant and Instrumentation as supplied by TECQUIPMENT the following experiments may be accomplished:

- (1) Measurement of Steam Mass Flow.
- (2) Determination of Boiler Efficiency.
- (3) Determination of Turbine Isentropic Efficiency.
- (4) Determination of Steam Cycle Thermal Efficiency.
- (5) Determination of Overall Plant Efficiency.
- (6) Determination of Heat-Exchanger Effectiveness and Overall Heat Transfer Coefficient.
- (7) Steady State Energy Analysis on each Plant Component.
- (8) Measurement of Insulation effectiveness.

2.2 DEMONSTRATIONS

The basic principles and practise of steam generating plant operation may be demonstrated using the experimental plant. However, because of the small scale nature of this experimental plant the demonstrations should not be regarded as typical of large scale steam plant without proper cognisance of the differences which occur between small and large scale plant. For example, this plant does not incorporate feed-heaters, air pre-heaters, economisers, re-heaters or multi-stage turbines, all of which would normally be used in typical large scale plant.

All aspects of starting and running and shut-down as described in Section 4 may be demonstrated together with operation of some of the safety features.

Demonstration of the turbine being exhausted direct to atmosphere rather than into the condenser may also be performed, but it is not recommended that the plant be operated for long periods in this mode in order to avoid large amounts of water passing through the water softener, and requiring renewal of the feed water treatment (L7).

2.3 FURTHER EXPERIMENTS

If additional equipment is available further experiments may be performed such as described below:

(1) Using Gas Analysis Equipment:

- Dry Exhaust Gas Analysis O_2 and CO
- Determination of Air/Fuel Ratio using the gas analysis results
- Determination of the Combustion Efficiency.

(2) Using Airflow Measuring Equipment and a Hygrometer:

- Determination of the Cooling Tower Performance.

(3) Using Boiler Water Analysis Equipment:

- Chemical analysis of the boiler water.

(4) Using a Throttling Calorimeter:

- Determination of the steam dryness fraction.

NB This manual does not give details of the above experiments. Further information can be found from references given in Section 9, or from Instruction Manuals which would be supplied with the above equipment.

SECTION 3

INSTRUMENTATION

Instruments are provided in order to monitor the plant during operation, and to measure its performance. The following describes each instrument and its use according to its function.

3.1 COMBUSTION SYSTEM

3.1.1 Fuel Flow

A burette and auxilliary reservoir is connected to the fuel tank and may be used to measure the fuel flow rate to the burner with the aid of a stopwatch, (not supplied).

To measure the fuel flow rate:

- (1) Close the main fuel supply valve (V40) thus allowing the burner to be fed from the burette.
- (2) Fill the burette with fuel (if necessary) by closing the burette vent valve (V41) and operating the hand pump.
- (3) Time the period required for the fuel to fall between the zero and 250 ml levels on the burette.
- (4) OPEN the main fuel supply valve (V40) IMMEDIATELY to avoid fuel starvation to the burner.

3.1.2 Fuel Temperature

The fuel temperature is read directly by selecting location [8] on the control console temperature selector.

3.1.3 Flue Gas Temperature

The flue gas temperature is read directly by selecting location [10] on the control console temperature selector.

3.1.4 Flue Gas Analysis

A gas sample can be taken from the tap at the base of the flue, and analysed with direct readout of O_2 and CO .

3.2 STEAM CIRCUIT

3.2.1 Boiler pressure

The boiler pressure is read directly on the 0 to 20 bar pressure gauge situated at the front of the boiler. The accumulator steam pressure may

also be read directly on the 0 to 20 bar pressure gauge situated on the front of the accumulator.

NOTE: ALL pressure gauges and the digital pressure indicator show GAUGE pressure. In order to convert GAUGE pressure to ABSOLUTE pressure (required when using steam tables or charts) ADD the current atmospheric pressure. If a barometer is not available assume a standard sea level atmospheric pressure of 1.013 bar corrected for altitude. Convert the pressure reading to appropriate S.I. units:

To convert bar to kPa: MULTIPLY by 100
To convert bar to MPa: DIVIDE by 10

3.2.2 Accumulator Condensate Level

The accumulator condensate level is shown directly on the sight glass fitted to the accumulator.

3.2.3 Steam Pressure and Temperature

The SATURATED steam pressure and temperature (from the accumulator) may be read directly by selecting location [1] on the control console pressure and temperature selector respectively.

The SUPERHEATED steam pressure and temperature (from the superheater coils) may be read directly by selecting location [2] on the control console pressure and temperature selector respectively.

3.2.4 Steam Flow Rate

The steam flow rate from the boiler is measured using the pressure differential across a stainless steel orifice plate installed in the steam main. The differential pressure is measured on a differential pressure gauge which is calibrated directly to indicate steam flow in the range 0 to 500 kg/h.

Note that this gauge has been calibrated for steam at 10 bar(absolute) and 250°C, (density 4.2955 kg/m³). For other steam conditions an appropriate correction for density must be applied. See Section 7.1.

To measure the steam mass flow rate proceed as follows:

- (1) Check that valves V52, V53 and V54 are CLOSED, then OPEN orifice line valve V50. OPEN its associated drain valve (V55) slowly to allow air and excess condensate to escape to drain. CLOSE the drain valve when only steam issues freely from the drain.
- (2) Repeat the above procedure with valve V51 and its drain valve (V56).
- (3) OPEN both pressure gauge valves V53 & V54 slowly and once the differential pressure level has stabilised read the steam flow rate.
- (4) All valves (except V52) may be left open to monitor steam flow rate. Periodically crack open the drain valves to prevent the orifice lines becoming filled with condensate, but always close isolating valves V53 and V54 when draining.

- (5) Close all valves when finished with the steam flow meter but open both drain valves to prevent vacuum as the system cools. Close the drain valves when the system has cooled to room temperature.

3.2.5 Turbine Inlet Steam Pressure and Temperature

The steam pressure supplied to the turbine (upstream of the governor controlled throttle valve) is read directly on the 0 to 16 bar pressure gauge.

The pressure and temperature of the steam supplied to the turbine is also read directly by selecting location [3] on the control console pressure and temperature selectors respectively.

3.2.6 Turbine Exhaust Steam Pressure and Temperature

The turbine exhaust pressure is read directly on the -1 to 2 bar pressure gauge (located on the condenser).

The pressure and temperature of the turbine exhaust steam is also read directly by selecting location [4] on the control console pressure and temperature selectors respectively.

3.2.7 Condenser Pressure

The condenser pressure is read directly on the -1 to 2 bar pressure gauge fitted to the condenser.

3.2.8 Lagging Temperature

The inside and outside temperature of the lagging may be read directly by selecting locations [11] and [12] respectively on the control console temperature selector.

3.3 CONDENSATE CIRCUIT

3.3.1 Condensate Pressure and Temperature

The pressure and temperature of the condensate in the condensate vessel is read directly by selecting location [5] on the control console pressure and temperature selectors respectively.

3.3.2 Feed Water Temperature

The temperature of the feed water leaving the feed tank is read directly by selecting location [9] on the control console temperature selector.

3.3.3 Feed Water Flow Rate

The average feed water flow rate is found by timing a reasonable change in the feed water totalising meter readings.

3.4 CONDENSER COOLING WATER CIRCUIT

3.4.1 Condenser Cooling Water Inlet and Exit Temperature

The condenser cooling water inlet and exit temperatures are read directly by selecting locations [6] (inlet) and [7] (exit) on the control console temperature selector.

3.4.2 Condenser Cooling Water Flow Rate

The condenser cooling water flow rate is measured by an indirect flow meter across an orifice installed in the cooling water inlet pipe. The flow meter is calibrated to measure the primary flow. The flow rate range is 8 to 40 m³/h. Sight across the top of the float.

3.5 THE TURBINE

3.5.1 Turbine Speed

The turbine speed [N] is read directly on the digital tachometer in revolutions per minute (RPM).

3.5.2 Turbine Torque

The torque developed by the turbine [T] is read directly from the digital torque indicator in Newton-meters (N.m).

NOTE: The turbine power output is given by:

$$W = 2 * \pi * N * T / 60,000 \quad \text{kW}$$

3.6 SAFETY INSTRUMENTATION

See Section 4.2 regarding the use of these instruments.

3.6.1 Superheater Coil Cooling Water Flow and Temperature.

A flow detector is provided to show whether there exists a positive flow to the superheater coils. A temperature indicator (0 to 120°C) monitors the cooling water temperature leaving the superheater coils.

3.6.2 Saturated Steam Temperature

A temperature gauge (0 to 300°C) is located on the front of the boiler to monitor the temperature of the steam supplied to the accumulator.

SECTION 4

SAFETY PRECAUTIONS and NORMAL OPERATING PROCEDURE

4.1 GENERAL SAFETY PRECAUTIONS

Nothing contributes more to the safe operation of a plant than a thorough knowledge of its working principles. Steam can be dangerous! Its saturation pressure rises rapidly with temperature and its working temperature and heat content alone is sufficient to inflict severe burns.

The plant has built-in safety features and various functions such as the accumulator condensate level and turbine speed are controlled or limited automatically.

The following sections describe the MAJOR safety precautions which need to be observed, but do not purport to cover every aspect of plant safety. The plant operator carries the immediate responsibility for safety and must therefore be thoroughly familiar with every aspect of the plant and its operation.

4.1.1 Burner (or Combustion System)

Observe the burner operating instructions carefully. If the burner fails to ignite promptly check for a fault condition as described in the Boiler Operation Handbook. Consistent failure to ignite promptly indicates that the burner needs servicing or that there may be a problem with the fuel (wrong type, contamination etc.).

Failure to ignite can result in an accumulation of unburnt fuel within the boiler which can subsequently ignite explosively causing damage. Do not proceed with more than TWO attempts at ignition without investigating the cause and checking to ensure that unburnt fuel has not accumulated within the boiler.

It is essential to use fuel of the correct specification. Keep the fuel clean. Do not pump fuel from the very bottom of a fuel container. Keep fuel tank closures in place except when filling. Guard against the ingress of insects or animals. Prevent water, dust, grit etc from entering the fuel.

4.1.2 Boiler (or Steam Generator)

The boiler is essentially a heat-exchanger where heat is transferred from the hot combustion gases to the water, which undergoes a change of phase to steam.

It is essential that the temperature of the boiler tubes (including the superheater tubes) remain within safe limits, and this means that they must be supplied with water at all times when the burner is in operation. If the water supply falls below a safe level the water tubes can become too hot causing distortion, weakening, or at worst, fracture or bursting under pressure. Under these conditions the saturated water temperature will exceed the set limit and the boiler will be automatically shut down.

If too much water is fed to the boiler it will be carried over into the accumulator. Take remedial action if the accumulator condensate level rises faster than is normal.

The pressure in the boiler and accumulator will increase if the heat transfer rate from the combustion gases is greater than that required to satisfy the steam demand. Pressure control is effected either by varying the steam demand or by varying the fuel flow rate. In normal operation the fuel flow rate is controlled by the boiler pressures set on the pressure switches situated on the front of the boiler. Low steam demand will result in a higher boiler pressure than will high steam demand. Consistently higher or lower boiler pressure than normal for a given steam demand is cause for investigation into the burner, or it may indicate scaling of the boiler tubes.

The boiler is equipped with two safety valves which will release steam if the pressure exceeds set levels. Do not tamper with the safety valves. They should be checked for correct operation regularly.

4.1.3 Turbine

The main feature concerning turbine safety is to guard against over-speed which can cause the turbine wheel to fracture. Although the turbine is speed regulated by a governor-controlled throttle valve and has an over-speed trip, failure or seizure of these mechanisms could lead to an over-speed condition. If such a condition occurs the turbine steam inlet valve (V12) or main steam valve (V2 or V3) must be closed as quickly as possible. Shutting down the boiler will not necessarily prevent an over-speed accident owing to the 'stored' steam within the accumulator.

Maintain the turbine governor and over-speed trip mechanisms in good condition. Refer to the Turbine Maintenance Handbook.

Keep loose clothing, long hair etc away from exposed moving parts of the turbine.

4.1.4 Dynamometer

The dynamometer must not be allowed to over-speed. The above precautions for the turbine also apply to the dynamometer.

4.1.5 Condenser and Condensate Vessel

Over-pressure of the condenser and condensate vessel must be avoided. Such a condition could occur if the cooling water supply to the condenser failed during operation of the plant. If the condenser safety valve blows or the high cooling water temperature alarm operates, shut down the plant and ascertain the cause.

The condensate vessel has a high liquid level alarm fitted. If this alarm operates check that the condensate extraction pump is operating and that the non-return valve is working properly.

4.1.6 Pumps

If the plant is not used frequently the pumps may become seized. A motor burn-out will occur if a seized pump is energised for more than a few seconds. If a pump fails to rotate switch off the electrical supply to it and ascertain the cause. Excessive noise or leakage from a pump usually indicates that maintenance is required. A noisy vacuum pump may indicate that the pump is insufficiently loaded. Try opening valve V21 slightly.

Where there are dual pumps it is good practise to use the pumps alternately in such a way as to give both pumps approximately equal use. In this way deterioration due to non use will be avoided.

4.1.7 Further General Safety Guidelines

Do not attempt to carry out maintenance or unauthorised adjustments while the plant is operating.

When opening or closing steam valves fully always back off from the stop by approximately a quarter of a turn. This helps prevent valve seizure owing to differential thermal expansion when the plant is warming up or cooling down.

Wear protective gloves or use a valve spanner to operate valves whose hand wheels are hot.

Do not knock or hit the glass fronts of pressure gauges or the glass tubes of level indicators or manometers. Glass breakage can be both dangerous and disruptive.

NOTES:

4.2 OPERATING PROCEDURE

The following procedure should be followed to enable the plant to be operated at a condition corresponding to approximately its maximum overall efficiency.

Refer to Fig. 2 and Plates 1 & 2 to identify valves and controls.

The procedure is divided into four stages:-

1. Pre-start checks.
2. Steam raising
3. Turbine operation
4. Shut down

4.2.1 Pre-start checks

1. Ensure that the control console master switch is OFF and all electrical switches on the control console and boiler control panel are in their OFF or MIN position.
2. Ensure that sufficient fuel is available to complete the run. If necessary top up the daily fuel tank by opening valve V42 and actuating the fuel hand pump. CLOSE valve V42 when the tank is full.
3. Check that all valves are CLOSED except:
 - Isolating valves fitted to all pressure gauges, pressure transducers and level gauges. These valves are not labelled since they normally remain OPEN.
 - The mains water supply valve (V31) and the mains supply valves to the cooling tower and water softener circuit to the feed tank. (V29,V32).
 - Condenser cooling water circuit valves. (V24,V25A/B,V26A/B,V27)
 - Condensate extraction pump valves V17A/B and V18A/B.
4. Remove, clean and replace the strainer in the steam main.
5. Ensure that the turbine throttle linkage can be moved by hand. Also check that the turbine-dynamometer can be rotated by hand, and that the turbine over-speed trip is set. Top up the oil in the turbine bearing housings and the governor to their correct levels.
6. Check that the condensate vessel is empty. If not energise the condensate extraction pump until the vessel is empty, then turn OFF.
7. Check that the cooling tower water reservoir and the feed tank are full.
8. Check that the water softening unit is connected and working.
9. Check that all drains are clear and unobstructed.

4.2.2 Steam raising

1. OPEN the following valves:

- All valves in the feed water supply line. (V19,V8A/B)
- Superheater inlet and outlet valves. (V3 and V4)
- Turbine by-pass valve and atmospheric exhaust valve. (V11 and V16)
- The main fuel supply valve. (V40)
- Accumulator steam trap valve. (V36)

Check that the superheater cooling water valves, V6 & V7 are fully closed.

2. Partly OPEN saturated steam by-pass valve V5.
3. Turn the control console master switch to ON. (The SUPPLY ON warning light should illuminate). This supplies power to the boiler control panel.
4. Press the (green) superheater tube high temperature warning reset button to allow power to the boiler control panel. Turn the boiler control panel master switch ON.
5. A number of warning indicators should illuminate on the boiler control panel. Reset them by pressing the RESET button on the control panel. All warning lights except the POWER ON and LOW FEED WATER FLOW warning lights should extinguish.
6. Select the feed pump whose valve was opened in Step 1, and then select feed pump ON. Check that water flows from valve V5 to drain, and that the LOW FEED WATER FLOW warning light extinguishes.
7. Select LOW BURN, then select BURNER ON.
The burner should commence its automatic purge and ignition cycle. Check for the presence of flame. If the burner malfunctions, switch OFF and rectify the fault before proceeding.
8. When steam issues from valve V5 to drain (this will take approximately 5 - 10 mins), OPEN valve V1 to allow steam to enter the accumulator, and slowly CLOSE valve V5.
9. Check that steam issues from the atmospheric vent and monitor the superheat temperature. It should not exceed 300°C.
10. Allow a few minutes for the steam to exhaust to atmosphere to clear the steam main of air and debris, then partially CLOSE the steam by-pass valve V11. DO NOT COMPLETELY CUT OFF THE STEAM FLOW. THIS WILL DEPRIVE THE SUPERHEATER TUBES OF STEAM FLOW AND COULD CAUSE THEM TO OVERHEAT.
11. Once the boiler pressure reaches approximately 4 bar select HIGH BURN. Note that the feed pump speed will automatically increase. Allow the boiler to reach its normal operating pressure.
12. The boiler will now continue to operate automatically.
If the boiler pressure exceeds the lower set limit the burner will automatically run on low burn. If the pressure exceeds the higher set limit (but below the sealed absolute safety limit) the burner will turn off. The burner will automatically reignite when the pressure falls.

4.2.3 Turbine operation (Vacuum Exhaust)

1. OPEN the turbine exhaust valve (V14) and all turbine nozzle valves.
2. OPEN vacuum valve (V20). OPEN vacuum pump mains water supply valve (V22) one turn. Turn the vacuum pump, condenser cooling water pump and cooling tower fan switches ON. Turn the condensate extraction pump switch to AUTO. Adjust the cooling water exit valve (V27) to give a flow of approximately 25 m³/h.
3. Wait until the vacuum gauge reads approximately -0.8 bar then slowly OPEN valve V13 to allow steam to the carbon ring sealing glands.
4. Turn the governor speed adjusting screw to its MINIMUM speed position if it is not already in that position.
5. Gradually OPEN the turbine steam inlet valve (V12) and allow the turbine casing to warm up slowly. Continue to open the valve and allow the turbine to rotate. The bypass valve (V11) may now be CLOSED.
6. Continue to OPEN the turbine steam inlet valve (V12) slowly until the governor assumes speed control at the low speed setting. If the governor fails to regulate the speed at the low speed setting shut down the plant and ascertain the cause.
7. Once speed control has been established and the turbine is thoroughly warmed through, OPEN the turbine steam inlet valve fully and adjust the speed setting screw to a speed of approximately 3200 RPM. The speed should fall to 3000 RPM when the turbine load is increased.
8. The turbine load may now be applied using the electrical dynamometer. Turn the field switch ON and CLOSE the armature circuit breaker. Increase the electrical load by rotating the excitation rheostat clockwise until the turbine speed falls to approximately 3000 RPM. It is recommended that the load be applied steadily so as to avoid sudden high steam demand which will cause an excessive fall in boiler pressure, but not too slowly otherwise the boiler will trip out owing to high superheat temperature.
9. At this condition the plant is operating at its maximum efficiency.

The turbine operating conditions may be varied by:
 - Changing the electrical load. NB Increasing the electrical load will control the turbine speed on load rather than by the governor.
 - Changing the speed using the speed setting screw. Do not exceed 3000 RPM.
 - Reducing the number of nozzles in use on the turbine.
 - Changing the inlet steam pressure by throttling using the turbine inlet valve (V12).
 - Changing the back pressure by throttling using the exhaust valve (V14).
10. During running monitor all pressure and temperatures and note any anomalies in the boiler operating log.

4.2.4 Shut down

1. Slowly CLOSE the turbine steam inlet valve (V12), and crack the bypass valve (V11) OPEN. Close valve V13 when the turbine ceases to rotate. (NB For a temporary shut-down CLOSE V12 only).
2. On the boiler control panel select BURNER OFF. CLOSE valve V1 and slowly OPEN valve V5. Turn the feed pump OFF when the saturated steam temperature reaches approximately 100°C.
3. CLOSE the fuel valve (V40).
4. On the control console turn the vacuum pump, condenser cooling water pump and cooling tower fan OFF. CLOSE valve V22. If the condensate vessel is not empty turn the condensate extraction pump to MANUAL and when the vessel is empty turn it OFF.
5. Turn the excitation rheostat fully anticlockwise. Turn the field switch OFF, and OPEN the armature circuit breaker.
6. Turn OFF the electrical master switches on both boiler and control console. OPEN the turbine exhaust drain valve, (V35).
7. Allow the boiler to cool to approximately ambient temperature then CLOSE all valves. If the boiler is to be left unused for a long period of time it is usual to flood it to prevent corrosion. Follow the instructions given in the Boiler Operating Handbook.

4.3 ALTERNATIVE OPERATING MODES

4.3.1 Turbine (Atmospheric exhaust)

1. Reduce the dynamometer load to zero.
2. Close turbine steam supply valve V12.
3. Turn the vacuum pump OFF, and CLOSE valve V22.
4. Slowly OPEN the atmospheric exhaust valve V15, then close the condenser exhaust valve V14.
5. Slowly re-open valve V12 and restore the dynamometer load.

Do not run for long periods in this mode to avoid excessive make-up water passing through the water softener.

Reverse the above procedure to return to vacuum exhaust running.

4.3.2 Saturated steam supply

In order to operate with saturated steam only the superheater coils must be kept cool by passing condenser cooling water through them.

DO NOT ATTEMPT TO CHANGE TO SATURATED STEAM IMMEDIATELY FROM OPERATING WITH SUPERHEATED STEAM.

The introduction of cold water to the hot superheater tubes could cause sudden steam formation and the thermal shock may damage the superheater tubes. Shut the plant down and allow the boiler to cool before restarting as directed below:-

1. Carry out the pre-start checks as directed in Section 4.2.1.
2. OPEN saturated steam supply valve V2.
3. CLOSE superheater inlet and outlet valves V3 and V4.
4. OPEN superheater cooling inlet and outlet valves V6 and V7.
5. Switch control console master switch ON, then turn the condenser cooling water pump and cooling tower fan switches ON.
6. Check that the flow indicator shows a positive water flow through the superheater tubes.
7. OPEN valves V19, V8A/B, V11 and V16.
8. OPEN accumulator steam trap valve V36 and fuel valve V40.
9. Now continue with the procedure for steam raising in Section 4.2.2 at STEP 4 and subsequent steps.

When the boiler is operating steadily saturated (or near saturated) steam will be supplied.

Operate the turbine according to the procedure given in Section 4.2.3 except that it will obviously not be necessary to switch on the cooling water pump and cooling tower fan because they will be operating already.

During operation monitor the superheater cooling water discharge temperature. If it approaches 100°C shut down the boiler and check for sufficient flow to the tubes.

4.3.3 To revert to superheated steam operation

1. Reduce the dynamometer load to zero and close valves V12 and V13 to isolate the turbine.
2. Fully OPEN the bypass valve V11. Saturated steam will now be vented to atmosphere.
3. Fully CLOSE superheater cooling inlet and outlet valves V6 and V7.
4. IMMEDIATELY OPEN valve V4.
Do not delay in doing this otherwise the water trapped in the superheater tubes could expand and fracture the superheater tubes.
5. Slowly OPEN valve V3 and CLOSE valve V2. The water in the superheater tubes will be blown through the steam main and out through the atmospheric vent. Allow sufficient time to ensure that all water has been blown clear.

The boiler is now supplying superheated steam and the turbine may be restarted as described in Section 4.2.3.

WARNING

THE STEAM AND SUPERHEATER COOLING WATER CIRCUITS MUST NEVER BE CONNECTED.
i.e. WHEN VALVES V6 AND V7 ARE OPEN, VALVES V3 AND V4 MUST BE CLOSED,
AND VICE VERSA.

SECTION 5

CALIBRATION of MEASURING INSTRUMENTS

The indication of any instrument is never absolutely accurate. Every instrument indicates a measurement which is within certain limits of the true value. These limits (or tolerance) are a measure of the instrument's accuracy. Provided the limits are within a range which is acceptable for our purposes the instrument is regarded as satisfactory.

It is recommended therefore that the accuracy of the instruments be checked at least annually.

The accuracy of instruments is typically checked in one of two ways:

- (a) By comparison with an instrument whose accuracy is at least an order of magnitude better than the instrument to be checked, or
- (b) Subjecting the instrument to a measurement known to be accurate by at least an order of magnitude better than the instrument is required to indicate.

The following procedures are recommended for the instruments provided:

5.1 PRESSURE GAUGES

Calibrate using a dead-weight tester or against a certified test pressure gauge.

If the applied or test-gauge pressure differs from the indicated pressure by more than the following amounts the gauge should be adjusted or replaced:

Gauge pressure range	Permissible error
0 to 16 bar	± 0.2 bar
-1 to 2 bar	± 0.05 bar

In addition to checking the gauge accuracy, check also that the needle moves freely and smoothly. If the needle moves in a series of stops and starts the gauge should be replaced.

5.2 TEMPERATURE GAUGES

Calibrate against a certified thermometer:-

0 - 100 °C Use a water bath and certified mercury in glass (MIG) thermometer of accuracy better than ± 0.1 °C. Temperature indication should be within ± 1 °C of the certified thermometer.

0 - 400 °C Use a suitable salt bath and certified thermocouple indicator of accuracy better than ± 0.5 °C. Temperature indication should be within ± 5 °C.

5.3 LEVEL GAUGES

No calibration check is possible since these gauges are calibrated during manufacture.

If level tubes or manometer tubes become dirty however, their readability will be impaired. If they become dirty they will need to be carefully removed, cleaned and replaced.

5.4 TACHOMETER

Check the tachometer against a suitable remote sensing electronic speed indicator of accuracy better than ± 5 RPM over the range 0 - 5000 RPM. (NB Tachometer checking will have to be accomplished during turbine operation).

The tachometer should indicate within ± 50 RPM of the test indicator.

5.5 TORQUE INDICATOR

Ensure that no residual torque is being applied to the dynamometer then set the indicator at zero using the 'zero adjust' potentiometer. Attach the weight hanger to the dynamometer and suspend the supplied calibration weight from it. Using the 'span' potentiometer, set the indicator to read the applied torque.

NB Torque arm radius = 300mm, therefore:

$$\text{Calibration weight (kgf)} * 2.94 = \text{Nm (On Torque meter)}$$

5.6 FLOW INDICATORS

No calibration is possible of the flowmeter used for measuring condenser cooling water flow or of the totalising meter for measuring feed water quantity to the boiler.

Remove, clean and refit the float gauge tube if it becomes dirty.

5.7 DIGITAL PRESSURE and TEMPERATURE INDICATORS

Calibration of the Digital Pressure and Temperature Indicators should not normally be required because of their exceptional long term stability and accuracy.

If calibration is required however, they may be checked in the same way as described above for conventional pressure and temperature indicators. Extreme care is needed to ensure that the electrical signal leads do not become damaged or broken.

5.8 SAFETY INSTRUMENTATION

The superheater water flow indicator needs no calibration.

Calibrate the superheater cooling water discharge temperature gauge if necessary as indicated in Section 5.2 above.

It is not recommended that the saturated steam temperature gauge be calibrated. Check its accuracy using steam tables when the boiler pressure is steady.

NOTES:

SECTION 6

EXPERIMENTAL PROCEDURES

For each of the experiments listed in Section 2 it is necessary to operate the plant under STEADY conditions. Therefore if a series of readings are being taken at different operating conditions ensure that sufficient time elapses between readings to restore steady state conditions.

The time required between readings can be established experimentally by taking a series of readings at regular intervals. When little or no change occurs between successive readings steady conditions can be assumed to have been achieved.

Although the boiler may be operated on its own by bypassing steam directly to atmosphere, it is recommended that the turbine also be operated even if only boiler experiments are being done. This will help to ensure that all components of the plant are kept in working order, and it will avoid passing large quantities of water through the softener.

For each of the following procedures it is assumed that the plant has been started and is being operated in accordance with the instructions given in Section 4.

A typical set of experimental measurements is shown on the Log Sheet included in Section 7 and examples of analyses can be found in the corresponding sub-sections of Section 7.

The Observations suggested are not necessary in order to do the calculations but should be noted to gain a better appreciation of the processes and changes which occur.

6.1 STEAM MASS FLOW RATE (Comparison of Methods)

Three methods of measuring steam mass flow may be used:

- (a) Orifice and Differential Pressure Gauge
- (b) Measuring the time required to fill the condensate vessel
- (c) Measuring the time required for a given change in feed water totalising meter readings.

NOTE: If steam is being bypassed (blown to atmosphere), Method '(b)' must be omitted from the comparison.

Procedure:-

- Measure:
- (1) Steam flow rate from the gauge. (Section 3.2.4)
 - (2) Time for the condensate quantity to change by 20 litres as indicated on the condensate vessel sight glass.
 - (3) Litres of water as registered by the feed water totalising meter over approximately 30 minutes.

(4) Condensate and feed water temperature.

The steam mass flow rate may be varied by changing the boiler load as described in the sub-section 6.2 below.

6.2 BOILER EFFICIENCY

Measure: (1) Fuel flow rate, (Section 3.1.1)

(2) Steam mass flow rate, (Use Method '(b)' above).

(3) Feed water temperature.

(4) Steam supply pressure and temperature.

Observe: (1) Boiler pressure and temperature.

(2) Flue gas temperature.

The boiler efficiency is typically dependent on the boiler load. The boiler load may be varied (within limits) as follows:

(a) To INCREASE the boiler load, slowly OPEN the turbine bypass valve (V11). This allows steam to escape to atmosphere and means that additional water must be supplied by the water softener. Do not therefore operate in this manner for any longer than is needed to stabilise and record the necessary readings. The maximum steam mass flow rate is approximately 450 kg/h. The boiler pressure will fall progressively if this value is exceeded.

Note that with the turbine operating as directed in Section 4.3 it may not be possible to increase the boiler load significantly.

(b) To DECREASE the boiler load reduce the dynamometer load to a minimum. To further reduce the boiler load, progressively close the turbine nozzle valves. Intermediate loads can be obtained by varying the dynamometer load.

DO NOT REGULATE THE STEAM FLOW TO THE TURBINE USING THE NOZZLE VALVES. THEY MUST BE EITHER FULLY OPEN OR FULLY CLOSED. Erosion of the valves may occur if they are used as regulators.

Minimum boiler load occurs with one nozzle open and zero dynamometer load.

Under these conditions burner operation will be intermittent and therefore relatively long time periods will be required to accomplish this test.

6.3 TURBINE ISENTROPIC EFFICIENCY

Measure: (1) Turbine shaft speed.

(2) Turbine torque.

(3) Steam mass flow rate. (Use method of para 6.1 (b))

(4) Turbine steam inlet pressure and temperature.

(5) Turbine exhaust pressure and temperature.

The turbine speed may be altered by resetting the governor speed adjusting screw. Do not exceed a turbine speed of 3200 RPM otherwise the over-speed trip may operate.

The turbine load can be varied using the dynamometer. If however, the dynamometer load is increased to the point where the governor maintains the throttle valve in the fully open position, further increasing the dynamometer load will cause the turbine speed to fall.

Each of the above strategies may be used to vary the turbine operating conditions.

Note that this test is done on the turbine/throttle combination since the turbine chest pressure is not available.

6.4 STEAM CYCLE THERMAL EFFICIENCY

Measure: (1) All steam and condensate pressures and temperatures.

(2) Turbine speed and torque.

(3) Steam mass flow rate. (Method of para 6.1 (b))

Observe: (1) Fuel flow rate

(2) Condenser cooling water flow rate, inlet and outlet temperatures.

The cycle operating conditions may be varied as described in sub-section 6.2 except that steam must not be bypassed.

6.5 OVERALL PLANT THERMAL EFFICIENCY

Measure: (1) Fuel flow rate.

(2) Turbine speed and torque.

Observe: (1) Total electrical load used by the plant (if practicable).

(2) Dynamometer Volts and Amps.

The plant operating conditions may be varied as described in sub-section 6.2.

6.6 HEAT-EXCHANGER EFFECTIVENESS

The heat-exchanger is the condenser.

Measure: (1) Condensate flow rate and temperature. (Method of para 6.1 (b))

(2) Turbine exhaust temperature.

(3) Condenser pressure.

(4) Condenser cooling water mass flow rate, inlet and outlet temperature.

The steam mass flow rate may be varied as described in sub-section 6.2.

The condenser cooling water mass flow rate may be varied by using the condenser exit valve (V27).

NOTE: If the condenser cooling water flow rate is reduced too much, insufficient heat will be removed from the turbine exhaust steam and the condenser pressure will rise. DO NOT EXCEED A CONDENSER PRESSURE OF -0.5 bar.

6.7 STEADY STATE ENERGY ANALYSES

Measure: All parameters as shown on the Log Sheet.

The plant operating conditions may be varied as described in sub-section 6.2.

6.8 INSULATION EFFECTIVENESS

Various types and sizes of insulation are supplied which may be fitted to a section of steam pipe from the superheater coil.

Procedure:

- (a) Fit the desired insulation to the pipe, and attach the outside surface temperature probe.
- (b) Monitor the steam temperature and pressure and external surface temperature of the insulant. When the readings are steady note the inside and outside surface temperatures.

SECTION 7

TYPICAL EXPERIMENTAL RESULTS & ANALYSES

The completed Log Sheet (p.43) gives a set of typical results from the plant when operating under approximately maximum overall efficiency conditions.

The following analyses use the data recorded on the Log Sheet.

The 'Points for Discussion' given in each sub-section are meant to serve as a self study and/or teaching aid.

The sub-sections of this Section correspond with the sub-sections of Section 6 and the Section 2.1.

7.1 Steam Mass Flow Rate (Comparison of Methods)

(a) Orifice and Manometer

The mass flow read from the scale was 400 kg/h
Steam density at 10.94 bar abs. and 272°C is 4.511 kg/m³
An approximate correction factor is $4.511/4.2955 = 1.050$
The corrected steam mass flow is: $400 * 1.050 = \underline{420 \text{ kg/h}}$

(b) Condensate Mass Flow Rate

20 litres of condensate collected in 180 secs.

Density of water at 39°C is 990 kg/m³

Mass flow is: $0.020 * 990 / (180 / 3600) = \underline{396 \text{ kg/h}}$

(c) Feed Water Mass Flow Rate

10.0 litres of water were pumped into the boiler in 1 min 11 sec

Density of water at 23.5°C is 998 kg/m³

Mass flow is: $0.010 * 998 / (71 / 3600) = \underline{506 \text{ kg/h}}$

Points for Discussion

1. Which mass flow rate do you consider to be the most accurate, and why?
2. Offer an explanation for the differences in the above mass flow rates.

Notes:

1. The mass flow measured by the orifice can be found by using BS 1042
The orifice diameter is 23.56 mm, the pipe diameter is 31.70 mm and the orifice has corner taps.

7.2 Boiler Efficiency

The Boiler Efficiency is defined as :

$$\eta_{\text{boiler}} = \frac{\text{Heat transfer rate to the steam}}{\text{Energy rate released by the fuel}}$$

$$= \frac{\dot{m}_s * (h_{\text{out}} - h_{\text{in}})}{\dot{m}_{\text{fu}} * \text{LCV}}$$

The feed water temperature is 23.5°C, from tables $h_{\text{in}} = 98.5$ kJ/kg

Steam temperature & pressure is 272°C & 1.094 MPa $h_{\text{out}} = 2990.0$ kJ/kg

The Lower Calorific Value of Fuel Oil is 42 MJ/kg and its Relative Density is 0.84

250 mls of fuel oil were used in 21 seconds therefore, the fuel mass flow rate is given by:

$$\dot{m}_s = 0.250 * 0.84 / 21 = 0.010 \text{ kg/s}$$

The boiler efficiency is given by:

$$\frac{(396/3600) * (2990 - 98.5)}{0.010 * 42 * 10^3} = 0.757 \quad (76\%)$$

Points for Discussion

1. How would you rate this boiler in terms of efficiency?
2. Why can boiler efficiency never be 100% ?
3. Why is the Lower Calorific Value (as opposed to the Higher Calorific Value) used in the efficiency calculation for this type of boiler?
4. What design and operating parameters affect boiler efficiency?

Notes:

1. The above calculations assume a Combustion Efficiency of 100%.

7.3 Turbine Isentropic Efficiency

The turbine isentropic efficiency is defined as:

$$\begin{aligned} \eta_{\text{turb}} &= \frac{\text{Turbine shaft power output}}{\text{Isentropic power available from the steam}} \\ &= \frac{\text{Torque} * \text{Rotational speed}}{\text{Steam mass flow} * \text{Isentropic enthalpy change}} \end{aligned}$$

The turbine steam inlet condition is 1.011 MPa & 238°C
The steam turbine exit pressure is 0.02 MPa.

Using a Mollier chart the Isentropic enthalpy change which occurs between the above conditions is 2915 - 2262 = 653 kJ/kg

The torque is 26 Nm & RPM is 3004

$$\text{Shaft power output} = 26 * 2 * \pi * 3004 / 60 = 8.179 \text{ kW}$$

The Isentropic efficiency is then given by:

$$\frac{8.179}{(396/3600) * 653} = 0.114 \quad (11 \%)$$

Points for Discussion

1. Large steam turbines operate at efficiencies in the range 80 to 90%.
Why is the efficiency of this turbine so low?
2. Under what conditions would the efficiency improve? Is it possible to operate under these conditions and if not why not?
3. How does the size of the turbine (in terms of its power output) affect its efficiency?

Notes:

1. The above-calculated efficiency is for the THROTTLE/TURBINE combination. This needs to be borne in mind when considering the above points.

7.4 Steam Cycle Thermal Efficiency

The Steam cycle thermal efficiency is defined as:

$$\eta_{\text{cycle}} = \frac{\text{Turbine shaft power output}}{\text{Heat transfer rate to the steam}}$$

From sub-section 7.3, turbine shaft power output is 8.179 kW

From sub-section 7.2, heat transfer rate to the steam is 318 kW

The Steam cycle efficiency is:

$$\frac{8.179}{318} = 0.026 \quad (2.6\%)$$

Points for Discussion

1. How does the Turbine Isentropic Efficiency affect the above result?
2. Draw the cycle on a T-s or Mollier chart.
3. How could the steam cycle efficiency be improved?
4. What is the maximum thermal efficiency of the cycle, (The Carnot Efficiency)? How does the measured thermal efficiency compare with it?
5. Explain why the measured thermal efficiency is less than the Carnot Efficiency.

Notes:

1. The feed pump power has been ignored in these calculations.

7.5 Overall Plant Thermal Efficiency

The overall plant thermal efficiency is defined as:

$$\eta_{\text{plant}} = \frac{\text{Turbine shaft power output}}{\text{Energy rate released by the fuel}}$$

From sub-section 7.3, turbine shaft power output is 8.179 kW

From sub-section 7.2, energy rate released by the fuel is 420 kW

The overall plant thermal efficiency is:

$$\frac{8.179}{420} = 0.019 \quad (2.0 \%)$$

Points for Discussion

1. Why is the overall plant thermal efficiency so low?
2. What contributes to the overall plant thermal efficiency?
3. Discuss the effect of plant size on the efficiency.

Notes:

1. Strictly, the auxiliary power used to drive the pumps, fans etc which are necessary to operate the plant, should be subtracted from the turbine power output. In large scale plant this auxiliary power is typically a small percentage of the shaft power produced by the turbine, and can be legitimately neglected. In this small scale plant subtraction of the auxiliary power would lead to a negative efficiency which would be meaningless.

7.6 Heat Exchanger Effectiveness

The Effectiveness of a heat exchanger is defined in terms of temperature:

$$E = \frac{\text{Temperature rise of the fluid with minimum thermal capacity}}{\text{Maximum temperature rise possible.}}$$

In the case of the condenser the cooling water is regarded as the minimum thermal capacity fluid, therefore:

$$E = \frac{T7 - T6}{T_{\text{sat}} - T6}$$

Where the heat transfer from a condensing vapour occurs at virtually constant temperature the effectiveness is also given by:

$$E = 1 - e^{-NTU}$$

NTU is the Number of Transfer Units defined as:

$$\begin{aligned} NTU &= \frac{\text{Overall Heat Transfer Coefficient} * \text{Heat Exchange Surface Area}}{\text{Minimum (Mass Flow} * \text{Specific Heat Capacity) of the fluids}} \\ &= \frac{U * A}{(\dot{m} * C)_{\text{min}}} \end{aligned}$$

The condenser pressure is 0.02 MPa, from tables $T_{\text{sat}} = 60.1 \text{ } ^\circ\text{C}$

$$E = \frac{39 - 30.7}{60.1 - 30.7} = 0.282$$

From the above equation : $NTU = 0.332$

The heat transfer surface area is approx. 1.4 m^2

$$U = NTU * \text{Cooling Water Mass Flow} * 4185 / A$$

$$U = 0.332 * 23000/3600 * 4185 / 1.4 = 6335 \text{ W/m}^2\text{K}$$

Points for discussion

1. Estimate the surface heat transfer coefficient on the water side.
(See Ref. 7 in Section 9)
2. Estimate the steam surface heat transfer coefficient. Is it larger than the water side coefficient? Why?
3. What effect does the presence of air have on the condensation process?
4. What effect does surface contamination have on the condensation process?

Notes:

1. Since the majority of the heat transfer occurs by condensation the saturation temperature is used in the definition for effectiveness rather than the turbine steam outlet temperature.

7.7 Steady State Energy Analysis

For any steady flow system, defined by a boundary, the First Law of Thermodynamics applies in the form of the steady flow energy equation (SFEE). The SFEE may be written:

$$\dot{Q} - \dot{W} = \dot{m}_s \Delta \left(\frac{1}{2}v^2 + gz + h \right)$$

The terms all refer to a particular fluid stream.

The SFEE may be applied to any component of the plant through which the working fluid (steam/water) passes. The example below applies the SFEE to the turbine by comparing the sum of the terms on each side of the equation.

LHS: Although the turbine is uninsulated the heat loss from it is very small i.e. $\dot{Q} = 0$ kW

From sub-section 7.2, $\dot{W} = 8.179$ kW

Therefore LHS = -8179 W

RHS: Steam velocity into and out of the turbine is given by :

$$\dot{m}_s / \text{Steam density} * \text{Flow Area}$$

For turbine entry $v_{in} = (396/3600)/(4.55 * 0.85 * 10^{-3}) = 28$ m/s

For turbine exit $v_{out} = (396/3600)/(0.2 * 5.0 * 10^{-3}) = 110$ m/s

Turbine exit and entry are virtually at the same level therefore:

$$z_{in} = z_{out}$$

From tables/chart $h_{in} = 2915$ kJ/kg

$$h_{out} = 2762$$
 kJ/kg

Therefore RHS = $396/3600 \left(\left(\frac{1}{2} * 110^2 - \frac{1}{2} * 28^2 \right) + (2762 * 10^3 - 2915 * 10^3) \right)$

$$= -17,451 \text{ W}$$

Points for Discussion

1. The Specific Kinetic and Potential Energy changes are often ignored when the SFEE is applied to devices like turbines. Why?
2. For what device inside a steam turbine is the Specific Kinetic Energy change important?
3. Why would you not normally expect to get the SFEE to exactly balance? What happens to the 'lost' energy?

Notes

1. The pipe diameters used to calculate the flow areas for the steam into and out of the turbine are : Inlet 33 mm dia.
Exit 80 mm dia.

7.8 Effectiveness of Insulation

Insulation inner surface temperature = 270°C

Insulation outer surface temperature = 28°C

Insulation size: 50 mm I.D. ; 120 mm O.D. (Fibreglass)
Thermal conductivity (λ) = 0.040 W/mK

The heat loss per unit length through a cylindrical conductor is given by:

$$\begin{aligned} \dot{q} &= \frac{2 * \pi * \lambda * \Delta T}{\ln \left(\frac{r_o}{r_i} \right)} \\ &= \frac{2 * \pi * 0.040 * (270-28)}{\ln \left(\frac{60}{25} \right)} \\ &= 69.5 \quad \text{W/m} \end{aligned}$$

The external surface heat transfer coefficient may be found from:

$$\begin{aligned} \dot{q} &= h * \pi * D * (T_o - T_{amb}) \\ h &= \frac{\dot{q}}{\pi * D * (T_o - T_{amb})} \\ &= \frac{69.5}{\pi * 0.12 * (28 - 17)} \\ &= 16.8 \quad \text{W/m}^2\text{K} \end{aligned}$$

Points for discussion:

1. If the same surface heat transfer coefficient as found above applies to the exposed pipe (i.e. uninsulated), estimate the heat loss per unit length from it.
2. How much larger is your answer from '1' than your calculated heat loss rate using the measured temperatures?
3. Compare the effectiveness of each of the types and sizes of insulation supplied.

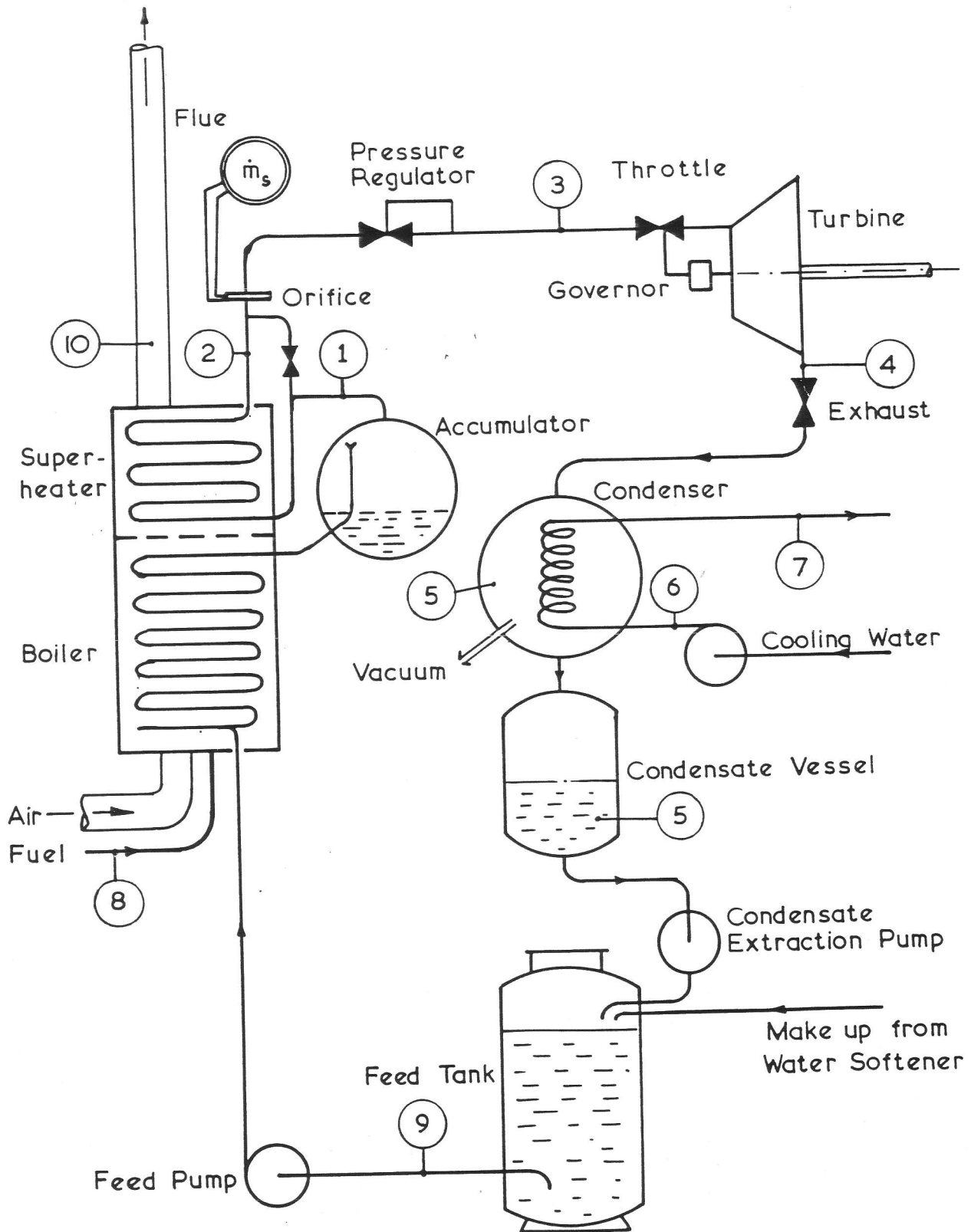
STEAM PLANT LOG SHEET		NAME: M A BELL				DATE: 18.2.87	
BAROMETRIC PRESSURE: 1000 mbar				AMBIENT TEMPERATURE: 17°C			
STATION	RUN	1		2		3	
		Temp. (°C)	Press. (bar)	Temp. (°C)	Press. (bar)	Temp. (°C)	Press. (bar)
1 Saturated Steam		176.3	9.39				
2 Superheated Steam		272	9.94				
3 Turbine Inlet		238	9.11				
4 Turbine Exhaust		141.3	-0.747				
5 Condensate		52.6	-0.808				
6 Cooling water inlet		30.7	1.22				
7 Cooling water exit		39.0	/	/	/	/	/
8 Fuel		14.9	/	/	/	/	/
9 Feed water		23.5	/	/	/	/	/
10 Flue gas		250	/	/	/	/	/
11 Lagging steam #		270					
12 Lagging surface #		28	/	/	/	/	/
FLOW MEASUREMENT	Steam: (kg/h)	400					
	Condensate: Litres	0	20				
	Time(sec)	3 min					
	Feed Water: Litres	0	10				
	Time(min)	1 min 11s					
	Cooling Water(m³/h)	23					
	Fuel: Millilitres	0	250				
TURBINE	Time(sec)	21					
	RPM	3004					
	Torque (Nm)	26					
	Field Amps/Volts	/	/				
Armature Amps/Volts	/	/					
NOTES:							
# Condensate quantity 162 g ; Elapsed time 34 mins							

SECTION 8

LOG SHEET and SYSTEM DIAGRAM

The log sheet and system diagram on the following pages may be copied and used for recording and teaching purposes.

STEAM PLANT LOG SHEET			NAME:			DATE:		
BAROMETRIC PRESSURE: mbar				AMBIENT TEMPERATURE:				
	RUN	1		2		3		
STATION		Temp. (°C)	Press. (bar)	Temp. (°C)	Press. (bar)	Temp. (°C)	Press (bar)	
1 Saturated Steam								
2 Superheated Steam								
3 Turbine Inlet								
4 Turbine Exhaust								
5 Condensate								
6 Cooling water inlet								
7 Cooling water exit		/	/	/	/	/	/	
8 Fuel		/	/	/	/	/	/	
9 Feed water		/	/	/	/	/	/	
10 Flue gas		/	/	/	/	/	/	
11 Lagging steam #								
12 Lagging surface #		/	/	/	/	/	/	
FLOW MEASUREMENT	Steam: (kg/h)							
	Condensate: Litres							
	Time(sec)							
	Feed Water: Litres							
	Time(min)							
	Cooling Water(m ³ /h)							
	Fuel: Millilitres							
	Time(sec)							
TURBINE	RPM							
	Torque (Nm)							
	Field Amps/Volts							
	Armature Amps/Volts							
NOTES:								
# Condensate quantity ; Elapsed time								



TD800 STEAM PLANT SYSTEM DIAGRAM

MAB
20.2.87

SECTION 9

BIBLIOGRAPHY

Author(s)	Title / Publisher
1 Bacon, D.H. Stephens, R.C.	Thermodynamics for Technicians (Butterworths, 1982)
2 Eastop, T.D. McConkey, A.	Applied Thermodynamics for Engineering Technologists, 3rd edition (Longman, 1978)
3 Rogers, G.F.C. Mayhew, Y.R.	Engineering Thermodynamics Work and Heat Transfer, 3rd edition (Longman, 1980)
4 Goodger, E.M.	Principles of Engineering Thermodynamics 2nd edition (MacMillan, 1984)
5 Goodall, P.M. (Ed.)	The Efficient Use of Steam (IPC Science & Technology Press, 1980)
6 BS 1042	Flow Measurement (British Standards Institute)
7 Simonson, J.R.	Engineering Heat Transfer (MacMillan, 1980)

NB All of the above references use SI units. Many older references on steam use Imperial units. Special care is required when converting from Imperial to SI units.

-21-

3. ΣΤΟΙΧΕΙΑ ΤΟΥ ΔΙΚΤΥΟΥ

3.1. ΣΩΛΗΝΕΣ

3.1.1. Διαστάσεις σωλήνων

Εφ'εξής στις εγκαταστάσεις ατμού πρέπει να χρησιμοποιούνται μόνο τυποποιημένοι σωλήνες.

Στην σημερινή τυποποίηση (ISO) χαρακτηρίζονται από την εξωτερική διάμετρο και το πάχος του τοιχώματος.

Γιά κάθε διάμετρο αντιστοιχεί ένα κανονικό πάχος. Γιά την σύνδεση των σωλήνων, εξαρτημάτων, οργάνων και λοιπών στοιχείων των σωληνώσεων έχουν τυποποιηθεί ονομαστικές διαμέτροι, που συμβολίζονται με τα γράμματα DN. Αυτές οι διαμέτροι αντιστοιχούν περίπου προς την εσωτερική διάμετρο του σωλήνα, χωρίς να αποτελούν όμως απόλυτο μέτρο.

Στον πίνακα 3.1. δίδονται όλα τα σχετικά στοιχεία. Στον πίνακα 3.2. δίδεται και ο συσχετισμός προς την αγγλοσαξωνική τυποποίηση.

ΠΙΝΑΚΑΣ 3.1. Εξωτερική διάμετροι, κανονικά πάχη και κατασκευαζόμενα λοιπά τυποποιημένα πάχη σωλήνων

DN	Εξωτερικές διαμέτροι	Σωλήνες χωρίς ραφή			Σωλήνες με ραφή		
		Κανονικό πάχος mm	Από	έως	Κανονικό πάχος mm	Από	έως
10 (12)	10,2**	1,6	1,6	2,8	1,6	1,4	2
	13,5**	1,8	1,8	3,6	1,8	1,4	2
	16 *	1,8	1,8	4	1,8	1,4	2
	17,2**	1,8	1,8	4,5	1,8	1,4	2,9
15	20 *	2	2	5	2	1,4	2,9
	21,3**	2	2	5	2	1,4	4,5
20	25 *	2	2	6,3	2	1,4	4,5
	26,9**	2,3	2,3	7,1	2	1,4	5
25	30	2,6	2,6	8	2	1,4	5
	31,8*	2,6	2,6	8	2	1,4	5
	33,7**	2,6	2,6	8,8	2	1,4	5
32	38 *	2,6	2,6	10	2,3	1,4	5
	42,4**	2,6	2,6	11	2,3	1,4	5

Συνέχεια πίνακας 3.1.

DN	Εξωτερικές διαμέτροι	Σωλήνες χωρίς ραφή		Σωλήνες με ραφή	
		Κανονικό πάχος mm	Άλλα πάχη mm	Κανονικό πάχος mm	Άλλα πάχη mm
40	44,5 48,3**	2,6 2,6	2,6 2,6	2,3 2,3	1,4 1,4
50	51 * 57 * 60,3**	2,6 2,9 2,9	2,6 2,9 2,9	2,3 2,3 2,3	1,4 1,4 1,4
65	63,5* 70 * 76,1**	2,9 2,9 2,9	2,9 2,9 2,9	2,3 2,6 2,6	1,6 1,6 1,6
80	82,5 88,9**	3,2 3,2	3,2 3,2	2,6 2,9	1,6 1,6
100	101,6* 108 114,3**	3,6 3,6 3,6	3,6 3,6 3,6	2,9 2,9 2,9	2 2 2
125	127 * 133 * 139,7**	4 4 4	4 4 4	3,2 3,6 3,6	2 2 2
150	152,4 159 168,3**	4,5 4,5 4,5	4,5 4,5 4,5	4 4 4	2 2 2
(175)	177,8 193,7	5 5,4	5 5,4	4,5 4,5	2,9 2,9
200	219,1**	5,9	5,9	4,5	3,2
250*	244,5 273 **	6,3 6,3	6,3 6,3	5 5	3,2 3,2
300*	323,9**	7,1	7,1	5,6	3,2
350*	355,6**	8	8	5,6	3,2
400*	406,4**	8,8	8,8	6,3	3,6
450	457 **	10	10	6,3	3,6
500	508 **	11	11	6,3	3,6
550	559	12,5	12,5	6,3	4,5
600	610 **	12,5	12,5	6,3	4,5
650	660 **	14,2	14,2	7,1	4,5

ΣΗΜΕΙΩΣΗ: Η αναγραφόμενη στον πίνακα 3.1. τυποποίηση με βάση την εξωτερική διάμετρο και το πάχος αφορά σε επιλογή από DIN - ISO 4200. Παρατηρητέο ότι οι εξωτερικές διαμέτροι κατατάσσονται σε τρεις κατηγορίες :

- Σειρά α (δύο αστερίσκοι) αφορά σε διαμέτρους για τις οποίες όλα τα εξαρτήματα (με φλάντζες ή για συγκόλληση) είναι τυποποιημένα.
 - Σειρά β (ένας αστερίσκος) αφορά σε διαμέτρους για τις οποίες δεν είναι όλα τα εξαρτήματα τυποποιημένα.
 - Σειρά γ (χωρίς αστερίσκο) αφορά σε διαμέτρους μόνο για ειδικούς σκοπούς για τις οποίες δεν υπάρχουν τυποποιημένα εξαρτήματα.
- Συνιστάται η χρησιμοποίηση της σειράς (α).

ΠΙΝΑΚΑΣ 3.2. Τυποποιημένες διαμέτροι σωλήνων σε mm και αντίστοιχα σε ίντσες

DN	in		in		DN		in	
	in	DN	in	DN	in	DN	in	
1		10	3/8"	100	4"	250	10"	
1,2		15	1/2"	(110)	(4 1/2")	(275)	(11")	
1,6		20	3/4"	(120)	5"	300	12"	
2		25	1"	125		(325)		
2,5		32	1 1/4"	(130)		350		
3		40	1 1/2"	(140)		(375)		
4		50	2"	150	6"	400		
5		(60)	(2 1/4")	(160)		450		
6		65	2 1/2"	(175)	7"	500		
8	1/4"	80	3"	200	8"	(550)		
		(90)	3 1/2"	(225)	(9")	600		